

# **TEST REPORT**

# **SCOPE:** EMISSIONS, EFFICIENCY AND OUTPUT

# **FUEL:** EPA TEST FUEL (CRIBS)

# TEST STANDARD: EPA

# **MODEL:** DESTINATION 2.3-I WOOD INSERT

Notice to reader: Our Destination 2.3-I wood insert was tested as part of our 2.3 Series (XTD 1.9) firebox. Therefore, the 2.3 Series (XTD 1.9) is referenced throughout the attached test report.



# REPORT NUMBER: 100456088MTL-002 REPORT DATE: March 21, 2012

# **EVALUATION CENTER**

Intertek Testing Services NA Inc. Intertek (Lachine) 1829 32<sup>nd</sup> Ave Lachine, Qc

# **RENDERED TO**

S.B.I.-Stove Builders International 250 Copenhague Street St-Augustin-de-Desmaures, QC G3A 2H3

**PRODUCT EVALUATED:** 

MODEL XTD 1.9 Wood Stove

Report of Testing Model XTD 1.9 Wood Fuel Room Heater for compliance as an "Affected Facility" with the applicable requirements of the following criteria: EPA Method 28 "Certification and Auditing of Wood Heaters" and EPA Method 5G "Determination of Particulate Matter Emissions from Wood Heaters".

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# TABLE OF CONTENTS

Ι.	INTRO I.A. I.B. I.C. I.D.	DUCTION PURPOSE OF TEST LABORATORY DESCRIPTION OF UNIT REPORT ORGANIZATION.	3 3 3
II.	SUMM II.A II.B II.C II.D	ARIZATION PRETEST INFORMATION INFORMATION LOG SUMMARY OF INFORMATION SUMMARY OF OTHER DATA	4 4 5
III.		ESS DESCRIPTION TEST SET UP DESCRIPTION AIR SUPPLY SYSTEM	8
IV.	IV.A IV.A.1 IV.B. IV.B.1	LING SYSTEM SAMPLING LOCATIONS. DILUTION TUNNEL OPERATIONAL DRAWINGS. STACK GAS SAMPLE TRAIN DILUTION TUNNEL SAMPLE SYSTEM.	8 9 10 10
V.	SAMP V.A.	LING METHODS PARTICULATE SAMPLING	12 12
VI.	VI.A. VI.A.1 VI.A.2 VI.A.3 VI.B. VI.B.1 VI.B.2	ITY ASSURANCE. INSTRUMENT CALIBRATION DRY GAS METERS. STACK SAMPLE ROTAMETER GAS ANALYZERS. TEST METHOD PROCEDURES. LEAK CHECK PROCEDURES. TUNNEL VELOCITY/FLOW MEASUREMENT PM SAMPLING PROPORTIONALITY.	12 12 13 13 13 13
VII.		CLUSION RESULTS & OBSERVATIONS	



## I. INTRODUCTION

Intertek Testing Services NA (Intertek) has witnesed testing for S.B.I.-Stove Builders International, on Wood Room Heater model XTD 1.9, to evaluate all applicable performance requirements included in EPA Method 28 "Certification and auditing of wood heaters" and Method 5G-3 "Determination of particulate matter emissions from wood heaters."

# I.A PURPOSE OF TEST

The test was conducted to determine if the unit is in accordance with U.S EPA requirements for Residential Wood Room Heaters. This evaluation was conducted August 22, 2011 – August 26, 2011.

# I.B LABORATORY

The test on Wood Room Heater model XTD 1.9 was conducted at the S.B.I's testing facility located at 250 Copenhague Street, St-Augustin-de-Desmaures, PQ G3A 2H3. The test was conducted by Florin Anghel.

# I.C DESCRIPTION OF UNIT

The model XTD 1.9 Wood Room Heater is constructed of carbon steel. The outer dimensions are 25.45 - inches deep, 30.001 - inches high, and 25.625 - inches wide.

(See product drawings.)

Proprietary drawings are on file at Intertek in Montreal.

## I.D REPORT ORGANIZATION

This report includes summaries of all data necessary to determine compliance with the regulations. Raw data, calibration records, intermediate calculations, drawings, specifications and other supporting information are contained in appendices to this report.



#### II. SUMMARIZATION

#### II.A PRETEST INFORMATION

Prior to beginning the emissions tests the unit was operated for a minimum of one hour at the burn rate corresponding to the burn rate cathegory the unit was about to be tested. The fuel used for the break-in process was Douglas Fir.

On August 22, 2011 the unit was set-up for testing.

#### II.B INFORMATION LOG

#### **TEST STANDARD**

From August 22, 2011 – August 26, 2011 the unit was tested for EPA emissions.

#### **Deviation from Standard Method**

No deviations from the standards were performed, however, only the applicable sections from each standard were used during all testing.



# **II.C SUMMARY OF TEST RESULTS**

RUN #1 (August 22, 2011) Burn time was 330 minutes with a category 2 burn rate of 0.96 Kg/hr and an emission rate of 4.82 g/hr. The fuel was loaded by 50 seconds and the door was closed at 90 seconds. The air control was fully opened for 5 minutes and then set to it's fully closed position at 5.0 minutes. The blower was off for the first 30 minutes and on-low for the reminder of the test.

RUN #2 (August 23, 2011) Burn time was 290 minutes with a category 2 burn rate of 1.09 and an emission rate of 4.07 g/hr. The fuel was loaded in 45 seconds and the door was left ajar (1/4") for 90 seconds. The air control was opened for the first 5 minutes and then abruptly set to 3/16" inch open at 5 minutes. The blower was off for the first 30 minutes and on-low for the reminder of the test.

RUN #3 (August 24, 2011) Burn time was 170 minutes with a category 3 burn rate of 1.84 kg/hr and an emission rate of 3.10 g/hr. The fuel was loaded in 45 seconds and the door was ajar (1/4") for 90 seconds. The air control was opened for 5 minutes and then abruptly set to 3/4 inch open for the reminder of the test. The blower was off for the first 30 minutes and on-low for the reminder of the test.

RUN #4 (August 25, 2011-Fan Confirmation) Burn time was 290 minutes with a category 2 burn rate of 1.09 kg/hr and an emission rate of 4.55 g/hr. The fuel was loaded in 50 seconds and the door was ajar at ¼" for 90 seconds. The air control was opened for 5 minutes and then set to 3/16 inch open from fully closed. Blower was off for the whole duration of the preburn and of the run.

RUN #5 (August 26, 2011) Burn time was 120 minutes with a category 4 burn rate of 2.67 Kg/hr. and an emission rate 2.86 g/hr. The fuel was loaded by 35 seconds and the door was left ajar at ¼" for 60 seconds. The air control was opened for 5 minutes and then set to it's fully open position. The blower was off for the first 30 minutes and on-low for the reminder of the test.



# **II.D SUMMARY OF OTHER DATA**

Run Number	Test Date	Burn Rate (kg/hr)	Emission Rate (g/hr)	Adjusted Emission Rate (g/hr)	Heating Efficiency (% LHV)
1	09/22/2011	0.96	3.23	4.82	74.7
2	09/23/2011	1.09	2.64	4.07	77.2
3	09/24/2011	1.84	1.93	3.15	75.2
4	09/25/2011 Fan Conf.	1.09	3.03	4.56	75.9
5	09/26/2011	2.67	1.73	2.87	67.4

#### **EMISSIONS**

# WEIGHTED AVERAGE CALCULATION

Test No.	Burn Rate	(E) Average Emission Rate g/hr	Heat Output (Btu/hr)	Probability	(K) Weighting Factor	(KxE)				
1	0.96	4.82	11575.87	0.3384	0.4494	2.1161				
2	1.09	4.07	13143.44	0.4494	0.5422	2.2068				
3	1.84	3.15	22187.09	0.8806	0.5264	1.6582				
5	2.67	2.87	32195.39	0.9758	0.1194	0.3427				
	Totals: 1.6374 6.3737									
	Weighted average emission rate: 3.8926									

### **TEST FACILITY CONDITIONS**

	Room	Room	Baro.	Baro.	R.H.	R.H.	Air	Air
Run	Temp.	Temp	Pres.	Pres.	%	%	Vel.	Vel.
Run	°F	°F	In. Hg	In. Hg	<sup>70</sup> before	After	Ft/min	Ft/min
	before	after	before	after	Delote	Allei	before	after
1	81.7	81.6	29.54	29.5	24	22	0	0
2	82.5	86.1	29.91	29.92	22	22	0	0
3	79.9	80.1	29.95	29.95	24	23	0	0
4	79.8	88.2	29.7	29.7	25	24	0	0
5	78.8	83.9	29.97	29.7	23	23	0	0



_	G-3)	TONNEL						
Run	Burn Time	Velocity	Volumetric Flow Rate	Total Temp.		ume nple		culate 1 (mg)
No.	(min)	(ft/sec)	(dscf/min)	(°R)	1	2	1	2
1	330	7.62	142.76	559.078	29.609	33.084	11.7	11.9
2	290	7.802	146.54	564.923	29.622	29.750	8.6	9.2
3	170	7.707	138.22	592.318	17.133	17.172	4.1	3.9
4	290	7.81	147.18	559.113	29.239	29.138	9.8	10.2
5	120	8.514	149.12	604.156	12.140	12.107	2.4	2.3

# DILUTION TUNNEL FLOW RATE MEASUREMENTS AND SAMPLING DATA

# **DILUTION TUNNEL DUAL TRAIN PRECISION**

	Sample	Ratios	Total Emi	ssions (g)	%	% Deviation
Run No.	Train 1	Train 2	Train 1	Train 2	Deviation	of 7.5% of
						7.5 grams*
1	1591.1	1423.9	18.62	16.94	3.90	5.01
2	1434.6	1428.4	12.34	13.14	2.62	2.84
3	1371.5	1368.4	5.62	5.34	2.17	1.82
4	1459.8	1464.9	14.31	14.94	1.80	2.19
5	1474.0	1478.1	3.54	3.40	1.65	1.27

\*= As described in Method 5G-3 section 16.2.5

## **GENERAL SUMMARY OF RESULTS**

Run No.	Burn Rate (kg/hr)	Change In Surface Temp (°F)	Initial Draft (in/H <sub>2</sub> O) *	Run Time (min)	Average Draft (in/H <sub>2</sub> O) *
1	0.96	-120.3	N/A	330	N/A
2	1.09	-122.6	N/A	290	N/A
3	1.84	-19.16	N/A	170	N/A
4	1.09	-126 **	N/A	290	N/A
5	2.67	-41.68	N/A	120	N/A

\* The Initial draft was not recorded on all the test runs

\*\*We noticed that the Delta-T obtained in the Fan Confirmation Test one degree over the allowed limit. Nevertheless, we ask for it to be taken into consideration as a limit exception, given that this test does not get into the calculation of the overall weighed average and that it's purpose is solely to demonstrate that the the wood heater may be considered to have the same average emission rate with or without the blower operating



# III. PROCESS DESCRIPTION

#### **III.A TEST SET-UP DESCRIPTON**

A standard 8" diameter single wall pipe and insulated chimney system was installed to 15' above the scale level. The unit controls were set to the lowest setting during the test.

# IV. SAMPLING SYSTEMS

## **IV.A. SAMPLING LOCATIONS**

Particulate samples are collected from the dilution tunnel at a point 20 feet from the tunnel entrance. The tunnel has two elbows and two mixing baffles in the system ahead of the sampling section. (See Figure 3) The sampling section is a continuous 13 foot section of 6 inch diameter pipe straight over its entire length. Tunnel velocity pressure is determined by a standard Pitot tube located 60 inches from the beginning of the sampling section. The dry bulb thermocouple is located six inches downstream from the Pitot tube. Tunnel samplers are located 60 inches downstream of the Pitot tube and 36 inches upstream from the end of this section. (See Figure 1)

Stack gas samples are collected from the steel chimney section 8 feet  $\pm$  6 inches above the scale platform. (See Figure 2)



#### IV.A.(1) **DILUTION TUNNEL**

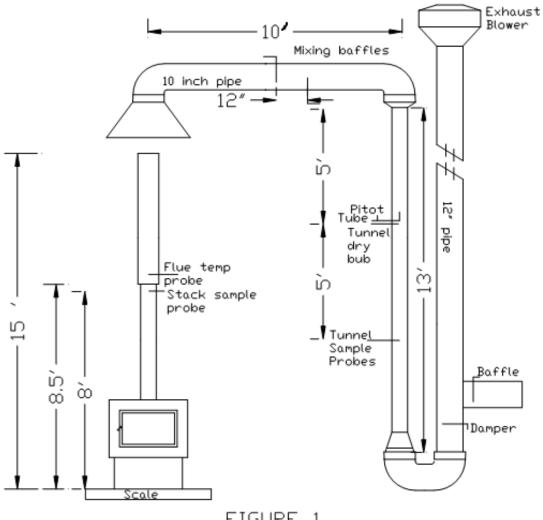


FIGURE 1



# **IV.B.OPERATIONAL DRAWINGS**

# IV.B.(1) STACK GAS SAMPLE TRAIN

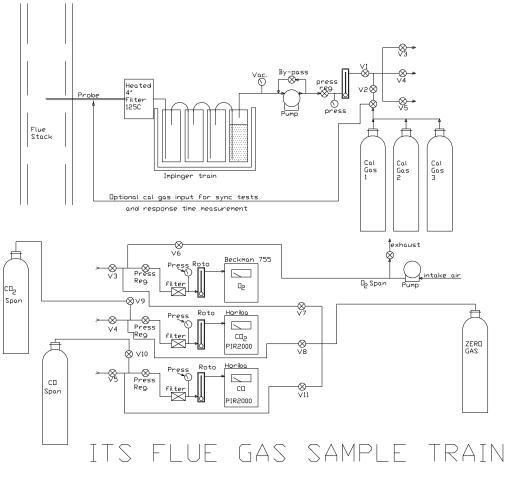


FIGURE 2



# IV.B.(2). DILUTION TUNNEL SAMPLE SYSTEMS

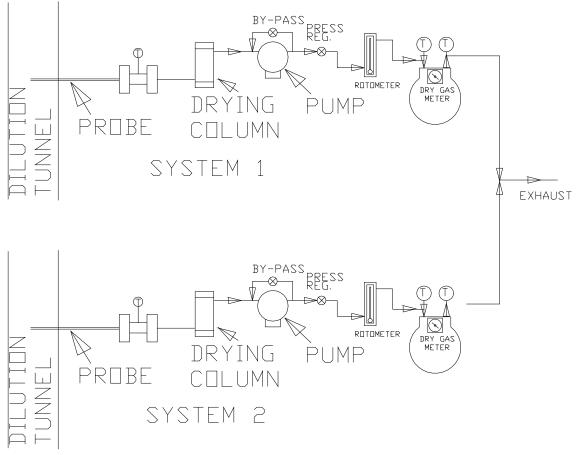


Figure 3



# V. SAMPLING METHODS

### V.A. PARTICULATE SAMPLING

Particulates were sampled in strict accordance with EPA Method 5G-3. This method uses two identical sampling systems 47-mm diameter filters. The dryers used in the sample systems are filled with "Drierite" before each test run.

### **VI. QUALITY ASSURANCE**

#### **VI.A. INSTRUMENT CALIBRATION**

## VI.A. (1). DRY GAS METERS

At the conclusion of each test program the dry gas meters are checked against our standard dry gas meter. Three runs are made on each dry gas meter used during the test program. The average calibration factors obtained are then compared with the six-month calibration factor and, if within 5%, the six-month factor is used to calculate standard volumes. Results of this calibration are contained in Appendix D.

An integral part of the post test calibration procedure is a leak check of the pressure side by plugging the system exhaust and pressurizing the system to 10" W.C. The system is judged to be leak free if it retains the pressure for at least 10 minutes.

The standard dry gas meter is calibrated annually by an accredited laboratory certified ISO 17025. The process involves sampling the train operation for 1 cubic foot of volume. With readings made to .001 ft<sup>3</sup>, the resolution is .1%, giving an accuracy higher than the  $\pm 2\%$  required by the standard.

#### VI.A.(2). STACK SAMPLE ROTAMETER

The stack sample rotometer is checked by running three tests at each flow rate used during the test program. The flow rate is checked by running the rotometer in series with one of the dry gas meters for 10 minutes with the rotometer at a constant setting. The dry gas meter volume measured is then corrected to standard temperature and pressure conditions. The flow rate determined is then used to calculate actual sampled volumes.



# VI.A.(3). GAS ANALYZERS

The continuous analyzers are zeroed and spanned before each test with appropriate gases. A mid-scale multi-component calibration gas is then analyzed (values are recorded). At the conclusion of a test, the instruments are checked again with zero, span and calibration gases (values are recorded only). The drift in each meter is then calculated and must not exceed 5% of the scale used for the test.

At the conclusion of each unit test program, a five-point calibration check is made. This calibration check must meet accuracy requirements of the applicable standards. Consistent deviations between analyzer readings and calibration gas concentrations are used to correct data before computer processing. Data is also corrected for interferences as prescribed by the instrument manufacturer's instructions.

# VI.B. TEST METHOD PROCEDURES

# VI.B.(1). LEAK CHECK PROCEDURES

Before and after each test, each sample train is tested for leaks. Leakage rates are measured and must not exceed 0.02 CFM or 4% of the sampling rate. Leak checks are performed checking the entire sampling train, not just the dry gas meters. Pre-test and post-test leak checks are conducted with a vacuum of 10 inches of mercury. Vacuum is monitored during each test and the highest vacuum reached is then used for the post test vacuum value. If leakage limits are not met, the test run is rejected. During, these tests the vacuum was typically less than 2 inches of mercury. Thus, leakage rates reported are expected to be much higher than actual leakage during the tests.

# VI.B.(2). TUNNEL VELOCITY/FLOW MEASUREMENT

The tunnel velocity is calculated from a center point Pitot tube signal multiplied by an adjustment factor. This factor is determined by a traverse of the tunnel as prescribed in EPA Method 1. Final tunnel velocities and flow rates are calculated from EPA Method 2, Equation 6.9 and 6.10. (Tunnel cross sectional area is the average from both lines of traverse.)

Pitot tubes are cleaned before each test and leak checks are conducted after each test.

## VI.B.(3). PM SAMPLING PROPORTIONALITY (5G-3)

Proportionality was calculated in accordance with EPA Method 5G-3. The data and results are included in Appendix C.



#### VII. CONCLUSION

These tests demonstrate that this unit is an affected facility under the definition given in the regulation. The weighted average emission rate of 3.89 g/hr meets the EPA requirements.

## VII.A RESULTS AND OBSERVATIONS

The Model XTD 1.9 Wood Room Heater has been found to be in compliance with the applicable performance and construction requirements of the following criteria: EPA Method 28 "Certification and auditing of wood heaters" and Method 5G-3 Determination of particulate matter emissions for pellet stoves."

#### INTERTEK TESTING SERVICES NA

Reported by:

Florin Anghel Testing Engineer

Reviewed by: 75-

Bruce S. Davis, Project Engineer



# Appendix C

С. G.

# Sample Analysis



CLIENT: SBI	MODEL: XTD 1	.9 <b>PROJECT #:</b> G100456088
DATE: 8/22/2011	RUN #:	<u>    1                                </u>
SAMPLE TRAIN: A	SAMPLE ID #:	MTL1108221414-001
INTERTEK EQUIPMENT #'s:		SBI 206

		FILTER # OR		WEIGHTS	(mg)
SAMPLE COMPONENT	REAGENT	PROBE #	FINAL	TARE	PARTICULATE
FRONT FILTER CATCH	FILTER	1	133.6	122.6	
REAR FILTER CATCH	FILTER	2	122.8	122.3	
TOTAL TARE			256.4000	244.9000	11.50
PROBE & FILTER HOLDER	PROBE	17	139749.6	139749.4	0.20
				TOTAL:	11.70

ENGINEER:



 CLIENT: SBI
 MODEL: XTD 1.9
 PROJECT #: G100456088

 DATE: 8/22/2011
 RUN #: 1

 SAMPLE TRAIN: B
 SAMPLE ID #: MTL1108221414-001

 INTERTEK EQUIPMENT #'s:
 SBI 206

		FILTER # OR		WEIGHTS (mg)			
SAMPLE COMPONENT	REAGENT	PROBE #	FINAL	TARE	PARTICULATE		
FRONT FILTER CATCH	FILTER	3	133	122.8			
REAR FILTER CATCH	FILTER	4	123.1	122.3			
TOTAL TARE			256.10	245.10	11.00		
PROBE & FILTER HOLDER	PROBE	19	140123.3	140122.4	0.90		
				TOTAL:	11.90		

ENGINEER:



CLIENT: SBI	MODEL: XTD	1.9	PROJECT #: G100456088
DATE: 8/23/2011	RUN #:	2	
	SAMPLE ID #:	MTL11	08221414-001
INTERTEK EQUIPMENT #'s:		SBI 206	

		FILTER # OR		WEIGHTS	(mg)
SAMPLE COMPONENT	REAGENT	PROBE #	FINAL	TARE	PARTICULATE
FRONT FILTER CATCH	FILTER	5	128.9	121.7	
REAR FILTER CATCH	FILTER	6	122.9	122.4	
TOTAL TARE			251.80	244.10	7.70
PROBE & FILTER HOLDER	PROBE	20	139069	139068.1	0.90
				TOTAL:	8.60

Intertek

CLIENT: SBI	MODEL: XTD 1.9	PROJECT #: G100456088
DATE: 8/23/2011	RUN #:	2
SAMPLE TRAIN: B	SAMPLE ID #:	MTL1108221414-001

INTERTEK EQUIPMENT #'s: SBI 206

		FILTER # OR	WEIGHTS (mg)		
SAMPLE COMPONENT	REAGENT	PROBE #	FINAL	TARE	PARTICULATE
FRONT FILTER CATCH	FILTER	7	133	122.7	
REAR FILTER CATCH	FILTER	8	123.1	122	
TOTAL TARE			253.20	244.70	8.50
PROBE & FILTER HOLDER	PROBE	21	139249.4	139248.7	0.70
				TOTAL:	9.20

ENGINEER:

DATE: \_\_\_\_\_11/8/2011



CLIENT: SBI	MODEL: XTD	1.9 <b>PROJECT #</b> : <u>G100456088</u>
DATE: 8/24/2011	RUN #:	3
SAMPLE TRAIN: A	SAMPLE ID #:	MTL1108221414-001
INTERTEK EQUIPMENT #'s:		SBI 206

	FILTER # OR			WEIGHTS	(mg)
SAMPLE COMPONENT	REAGENT	PROBE #	FINAL	TARE	PARTICULATE
FRONT FILTER CATCH	FILTER	9	124.7	121.6	
REAR FILTER CATCH	FILTER	10	122.4	121.8	
TOTAL TARE			247.10	243.40	3.70
PROBE & FILTER HOLDER	PROBE	23	136189	136188.6	0.40
				TOTAL:	4.10

ENGINEER:

 $\bigcirc$ 

Intertek

CLIENT: SBI	MODEL: XTD 1.9	PROJECT #: <u>G100456088</u>
DATE: 8/24/2011	RUN #:3	}
SAMPLE TRAIN: B	SAMPLE ID #:	MTL1108221414-001

	1	FILTER # OR			(mg)
SAMPLE COMPONENT	REAGENT	PROBE #	FINAL	TARE	PARTICULATE
FRONT FILTER CATCH	FILTER	11	123.7	120.6	
REAR FILTER CATCH	FILTER	12	123.3	123	
TOTAL TARE			247.00	243.60	3.40
PROBE & FILTER HOLDER	PROBE	24	136041.3	136040.8	0.50
				TOTAL:	3.90

INTERTEK EQUIPMENT #'s: SBI 206

ENGINEER:

Intertek

CLIENT: SBI	MODEL: XTD	1.9	<b>PROJECT #</b> : <u>G100456088</u>
DATE: 8/25/2011	RUN #:	4	
SAMPLE TRAIN: A	SAMPLE ID #:	MTL1	108221414-001
INTERTEK EQUIPMENT #'s:		SBI 206	

		FILTER # OR	WEIGHTS (mg)		
SAMPLE COMPONENT	REAGENT	PROBE #	FINAL	TARE	PARTICULATE
FRONT FILTER CATCH	FILTER	13	130.6	122	
REAR FILTER CATCH	FILTER	14	123.1	122.4	
TOTAL TARE			253.70	244.40	9.30
PROBE & FILTER HOLDER	PROBE	25	136833.6	136833.1	0.50
				TOTAL:	9.80

ENGINEER:

DATE: \_\_\_\_\_11/8/2011

Intertek

CLIENT: SBI	MODEL: XTD	1.9	PROJECT #: G100456088
DATE: 8/25/2011	RUN #:	4	
SAMPLE TRAIN: B	SAMPLE ID #:	MTL110	8221414-001
INTERTEK EQUIPMENT #'s:		SBI 206	

		FILTER # OR		WEIGHTS (mg)		
SAMPLE COMPONENT	REAGENT	PROBE #	FINAL	TARE	PARTICULATE	
FRONT FILTER CATCH	FILTER	15	132.2	123.3		
REAR FILTER CATCH	FILTER	16	123.8	122.9		
TOTAL TARE			256.00	246.20	9.80	
PROBE & FILTER HOLDER	PROBE	26	139829.3	139828.9	0.40	
				TOTAL:	10.20	

( )

DATE: \_\_\_\_\_11/8/2011\_\_\_\_

Intertek

CLIENT: SBI	MODEL: XTD	) 1.9 PR	OJECT #: G100456088
DATE: 8/26/2011	RUN #:	5	
SAMPLE TRAIN: A	SAMPLE ID #:	MTL11082214	414-001
INTERTEK EQUIPMENT #'s:		SBI 206	

	1	FILTER # OR	WEIGHTS (mg)		
SAMPLE COMPONENT	REAGENT	PROBE #	FINAL	TARE	PARTICULATE
FRONT FILTER CATCH	FILTER	17	124.6	123	
REAR FILTER CATCH	FILTER	18	122.5	122.3	
TOTAL TARE			247.10	245.30	1.80
PROBE & FILTER HOLDER	PROBE	27	136902.6	136902	0.60
				TOTAL:	2.40

ENGINEER:

Intertek

CLIENT: SBI	MODEL: XTD	1.9	PROJECT #: G100456088
DATE: 8/26/2011	RUN #:	5	
SAMPLE TRAIN: B	SAMPLE ID #:	MTL110	08221414-001
INTERTEK EQUIPMENT #'s:		SBI 206	

		FILTER # OR		WEIGHTS	(mg)
SAMPLE COMPONENT	REAGENT	PROBE #	FINAL	TARE	PARTICULATE
FRONT FILTER CATCH	FILTER	19	124	122.2	
REAR FILTER CATCH	FILTER	20	117.6	117.5	
TOTAL TARE			241.60	239.70	1.90
PROBE & FILTER HOLDER	PROBE	28	136224.2	136223.8	0.40
				TOTAL:	2.30

ENGINEER:

101236 201323 501324 501324 501324 601324 601329 601329 501330 501320 50120 5005 5005	Date 2011 05 Date 0.12.24 0.12.24 0.12.17 0.12.16 0.12.17 0.12.16 0.12.19 0.12.25 0.12.19 0.12.26 0.12.19 0.12.26 0.12.19 0.12.26 0.12.19 0.12.26 0.12.19 0.12.26 0.12.15 0.12.26 0.12.25 0.12.26 0.12.25 0.12.26 0.12.25 0.12.26	Date 01226 01226 01227 01228 01228 01220 01220 01220 01220 01220	late     Date     Date     Date $a12.26$ $013.21$ $013.24$ $013.26$ $013.26$ $a12.24$ $013.21$ $012.26$ $013.26$ $013.26$ $a12.24$ $012.27$ $012.27$ $012.26$ $012.26$ $a12.24$ $012.27$ $012.27$ $012.26$ $012.26$ $a12.24$ $012.27$ $012.27$ $012.26$ $012.26$ $a12.26$ $012.26$ $012.26$ $012.26$ $012.26$ $a12.20$ $012.26$ $012.26$ $012.23$ $0122.23$ $a12.20$ $012.23$ $012.23$ $012.23$ $012.23$ $a12.20$ $012.23$ $012.23$ $012.23$ $012.23$ $a12.20$ $012.23$ $012.23$ <td< th=""><th>Date 0.12.26 0.12.26 0.12.28 0.12.23 0.12.24 0.12.20 0.12.20 0.12.20 0.12.20 0.12.20</th><th>Date         Date         Date         Date           01326         01226         0.1226         0.7226           01326         01226         0.1228         0.7226           01227         01227         0.7226         0.7226           01227         01227         0.7226         0.7226           01227         01227         0.1228         0.1228           01227         01227         0.1227         0.1228           01237         01237         0.1229         0.1228           01237         01237         0.1223         0.1223           01237         01237         0.1223         0.1223           01237         01233         01233         0.1233           01233         01233         01233         01233</th><th>Date 0. 1340 0.1230 0.1233 0.1233</th><th>Date     Date       Date     0       0     0       0     0       0     0       0     0       0     0       0     0       0     0       0     0       0     0       0     0       0     0       0     0       0     0       0     0       0     1224       0     0       0     1223       0     1230       0     1230</th><th>te A335 A335 A335 A335 A335 A335 A335 A33</th><th>Date 0.12.00 0.12.00 0.12.00 0.12.00 0.12.20 0.12.20</th></td<>	Date 0.12.26 0.12.26 0.12.28 0.12.23 0.12.24 0.12.20 0.12.20 0.12.20 0.12.20 0.12.20	Date         Date         Date         Date           01326         01226         0.1226         0.7226           01326         01226         0.1228         0.7226           01227         01227         0.7226         0.7226           01227         01227         0.7226         0.7226           01227         01227         0.1228         0.1228           01227         01227         0.1227         0.1228           01237         01237         0.1229         0.1228           01237         01237         0.1223         0.1223           01237         01237         0.1223         0.1223           01237         01233         01233         0.1233           01233         01233         01233         01233	Date 0. 1340 0.1230 0.1233 0.1233	Date     Date       Date     0       0     0       0     0       0     0       0     0       0     0       0     0       0     0       0     0       0     0       0     0       0     0       0     0       0     0       0     0       0     1224       0     0       0     1223       0     1230       0     1230	te A335 A335 A335 A335 A335 A335 A335 A33	Date 0.12.00 0.12.00 0.12.00 0.12.00 0.12.20 0.12.20
0, 1235	0,1234	01233	01234	01235					6221.0
17 6 1330 18 0 1323 19 7 1222	01222	0.1230	01223	01230					
1 - 13 :	01175	0112		01176					
23 0 11 95	0.184	0 184	0.1184	0 1227					

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		20-107	12-20-1102	201-08-102 20-107-10-102	2 40-1102 76-Co-192 92-20-1102	71-00-10	2 +60-1102			
ld. Filtres	Date	Date	Date	Date	Date	Date	Date	Date	Date	Date
	1 0.1336	0.1336								
	20.1228									
	30.1330	0.1330								
4	40.1231									
	50.1287	0.1283								
	6 O. 1229	0.1225								
	70.1302	5130								
~	80.1228	0.1228								
	6	0.1248		0.1247						
10	0	0.1222		0 1224						
11	-	0.1238		0.12 Ma						
12	2	0.1233		0.1233						
13	~	01211			0.1308	0.1306				
14	1	0.1232			0.12.31	0.1231				
15	2	0.1325			0.1322	0.1322				
16	10	0.1236			0.1237	0.1238				
17	C221.0 1		0.1230	54210		4421.0				
18	18 0.1224		01223	0.1227		0.1226				
15	19 0.1223		0.1222	0.1239		0.1240				
2(	FP11.002		Stw 0	0.1179		54110	5t10			
21	21 0.1224									
22	22 0.1228									
23	SO.1185									
24	0120									

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		2011-08-11	201-08-12 2011-	2011-08-17	ł	2011-08-14 2011-08-22 2011-08-22 201-08-23	22-80-1107	201-08-23	201-08-23 201-08-24	2011-08-24	2011-08-24
ld. Probes		Date	Date	Date	Date	Date	Date	Date	Date	Date	Date
Kun 41	17	139-7483	139 7429	134 74 78	139 74 89	ちたいこ	1842 021		Scife Cel		
	12	18 147 3409	147.8910	147 0904	0197 8910	0108 241	++08'0+1	1-1-821-1		1268.541	
Run +1	61	140 12 19	140 1230	140 12 14	1401219	140,1224 140,1224	140,1224		140,1230		
	20	139.0680	1390682	134 0678	139 0684	133,0686 133,0681		139,0681	139,0681		
	21	139 2484	1392494	1392482	1392486	1242,251	133,2489	+842, CE1 F842, CE1 F842, CE1	4842, CEV		
	22	1395793	1395793	134 5789	1395798		125,5732	2645, 621		8845 621	
CA-WA H	23	136 1879	1361882	156 1880	136 1883	136,1888	1981 130,1884	136,1884		136,1886	136,1281
li unti 5	24	136 0406	136 0405	136.0402	1360404	136,0408 136,0405	136,0405	136,0405		8040951	136,043
Kunty .	25	25 136.8325	1368325	136 8323	136.2325	136,8333	136,8329 136,8327	136,8327		136,8329	
Kunty	26	139 9286	1398235	139 8283	139 92 96	125,8231	139,4288 139,8288	133,8288		139,8288	
	27	136,9013	136 9013	136 9009	136,9017	136, 3019 136,3015 136,3015	136,9615	136,3015		136,3017	
	28	136 22332	136,3332	1362230	1362235	136,2240 56,2232 36,2232	56,2222	136,2232		136,2238	
	29		135 18 30	135 1826	135 1832	135,1836 435,435 135,1833	425,435	135,18 33			
	30		135,9029	135,4025	135 9031	2505,201	1500/521 1500/551	1200551			
	31		137 0 499	137 0493	1370499	137,1003 137,0398		8000 451			
	32		136 044	136 0157	1360195	136,0138	156,0136	136,0196			
	33		135. 9949	135 4942	135 9944	135,3352	4955'SEN 6466'SEN	135,3547			
	34		108 4113	108 411 0	108 4113	101,4117 108,444		1114,801			
	35		107 8381	1078374	1078382	107,8385	107,8380 107,8380	107,8380			
	36		108 5030	103 5026	108 5030	108,5035	108,5030 108,5030	0205 801			
	37		108 3837		109 3937	A08,3840	NESS-SO1	7282,801			
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	Date																							
	Date																							
	Date																							
	Date											HTT T												
201-00-12	Date									136,8336	135 8293	136,30277	136.2240											
2011-01-20	Date									136.8340	123,8238													
201-08-26 2011-08-26 2011-09-12	Date			1521,041	0530, 621	4642.001		136,1830	136,0412				36,2238											
08-20	Date			2	-	-			7			136, 30,20 136, 3023	136,2238 136,2238											
22-80-	Date				1530,651	39, 2495		136, 1891	136,0420	8331 136, 8335		V												
72-80	Date	17 133,7436	18 Atta 8017	19140,1233	20 133,0688 135,0631	21 139 ,2495 139	22 (39,57-35				26 139, 8289	27 136,3017	28 436,2235											
1	ld. Probes 0	17 4	18 A	191	20 1	21 A	22 V	23	24	25/36	26 1	27 V	28 4	29	30	31	32	33	34	35	36	37	38	

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# **DILUTION TUNNEL WORKSHEET - METHOD 5G3**

					000			
Client: SBI N								
Project #: Gloo4								
Date: 08-22-11 E								
Balance Equipme	nt #: 581-206 Th	ermo/Hygro mel	ter Equipment #	SB1-212				
Audit weight Equi	pment #: 180-110	(Balance audit n	nfr. std: 500 ± 0	.72 mg)				
Front Filter #	1	Tare:	0.1226	Preliminary	Wt:	¢	0. 1340	
Rear Filter #	2_	Tare:	0.1223	Preliminary	Wt:	0	1230	
Seal Set #		Tare:		Preliminary	Wt:			
Date/Time in de	essicator:	08-22-11	17:40	Preliminary	Wt:	0.	257-	
Date	Time	R/H %	Temp. (F)	Weight (grams)	(gra	udit ams)	Initials	
08-23-11	17:00	15%	69.9	0.2569	0.2 0,20		AF	
08-25-11	8:30	17%	68.2	0.2564	0.2		Æ	
08-25-M	18:30	17%	69.0	0.2564	0.2 0.20		Æ	FIHAL STABILIZ WEIGHT
								-
Probe #:	17	Tare:	139,7494	Preliminary \	l Nt:	139	),7484	-
Date/Time in de	ssicator:	08-22-11	/17:40					
Date	Time	R/H %	Temp. (F)	Weight (grams)	Au (gra	idit ims)	Initials	
08-23-11	17:00	15%	69.9	139,7496	200.0	.0 = 202	A	
08-25-11	8:30	17%	68.5	139,7496	200	.0=	A	FINAL STABILIZI WEIGHT
		<u> </u>			_			_

Date: 11-08-11

# **DILUTION TUNNEL WORKSHEET - METHOD 5G3**

Client: SBi N			ORRSHEET		363		
Project #: GA004			27 141 4-00	A			
Date:08-22-11E	ngineer HOR	H ANGHEL P		- amolo Troin #:	R		
Balance Equipme	nt #: SB1-206TI	hermo/Hyaro me	ter Equinment #	SB1-212			
Audit weight Equi	pment #: 180-43	Balance audit r	mfr. std: $500 \pm 0$	.72 ma)			
Front Filter #	3	Tare:	0. 1228	Preliminary	Wt: 🗸	0.1334	
Rear Filter #	4	Tare:	0.1223	Preliminary	Wt: C	2.1233	-
Seal Set #		Tare:		Preliminary			-
Date/Time in de	essicator:	08-22-11	17:40	Preliminary	Wt: O	.2577	
Date	Time	R/H %	Temp. (F)	Weight (grams)	Audit (grams)	Initials	
08-23-11	17:00	15%	63.3	0.2566	0.2 =	AF	
08-25-11	8:30	17%	68.5	0.2561	0.2 =	AF	
08-25-11	18:30	17%	69.0	0.2561	0.2= 0.2000	AF	FIHAL STABILIZE WEIGHT
Probe #:	19	Tare:	140,1224	Preliminary \	Nt: Nho	1,1224	7
Date/Time in de	ssicator:	08-22-11	17:40				
Date	Time	R/H %	Temp. (F)	Weight (grams)	Audit (grams)	Initials	1
08-23-21	17:00	15%	63.3	140,1230	200.002	- <del>A</del> -	
08-25-11	8:30	17%	68.5	140,1233	2	AF	FIHAL STABILIZ WEIGHT

Date: 11-08-11

# **DILUTION TUNNEL WORKSHEET - METHOD 5G3**

Client: SBI N					000			
Project #: Glook			8221414-	001				
Date: 08-23-41 E					A			
Balance Equipme	ent #: 581-206 Th	ermo/Hvaro met	er Equipment #	SB1-212				
Audit weight Equi	180-195 pment #: 1 <u>80-11</u> 0	(Balance audit m	nfr. std: 500 ± 0	.72 mg)				
Front Filter #	5	Tare:	0.1217	Preliminary	Wt:	0	.12.88	
Rear Filter #	G	Tare:	0.1224	Preliminary	Wt:	0.	1230	
Seal Set #		Tare:		Preliminary	Wt:			
Date/Time in de	essicator:	8-23-11/	17:00	Preliminary	Wt:	0	.251	
Date	Time	R/H %	Temp. (F)	Weight (grams)		udit ams)	Initials	
8-25-11	8:30	17%	68.5	0.2516	0.2		AF	
8-25-11	18:30	17%	63.0	0.2518	0.2 0.2		- <del>M</del>	1
						-	0	
Probe #:	20	Tare: A	39,0681	Preliminary V	Nt:	139	0681	
Date/Time in de	essicator:	8-23-11/	17:00					
Date	Time	R/H %	Temp. (F)	Weight (grams)	I .	idit ms)	Initials	
8-25-11	8:30	イナ	68.5	133,0688	200.0		AT	
8-25-M	18:30	17-	69.0	139,0691	2.00 200,0		AF	]~
8-26-11	12:15	17	69.0	139,0630	200,0	),0= CO2	AF	
								1
			the second s					

Date: 11-08-11

# **DILUTION TUNNEL WORKSHEET - METHOD 5G3**

Client: <u>SBi</u> Model: <u>XTL</u> 1.9 Project #: <u>GN004</u>56088 Sample ID #: <u>HTL</u> 1108221414-001 Date: <u>8-23-11</u> Engineer: <u>FLORIN ANGHELRun #: 2</u> Sample Train #: <u>B</u> Balance Equipment #: <u>SBi 206</u> Thermo/Hygro meter Equipment #: <u>SBI - 212</u> Audit weight Equipment #: <u>180-195</u> (Balance audit mfr. std: 500 ± 0.72 mg)

7	Tare:	0.1227	Preliminary \	Nt:	0.1301	
8	Tare:	0.1220	Preliminary \	Nt:	0.1227	
	Tare:		Preliminary \	Nt:		
essicator:	8-23-11	17:00	Preliminary \	/Vt:	0.2528	
Time	R/H %	Temp. (F)	Weight (grams)			
8:30	17%	68.5	0.2530	0.2=		
18:30	17	69.0	0,2532	-		-
		1				
21	Tare:	139,2487	Preliminary V	Vt: 13	59,2484	
essicator:	8-23-14	14:00				
Time	R/H %	Temp. (F)	Weight (grams)			
8:30	17	68.5	139,2493	200.0: 200.002	<del>A</del>	
18:30	17	63.0	139,2495			]~
12:15	17	69.0	139,2494			
						1
	$\begin{array}{c c} \hline \\ \hline $	7Tare:8Tare:rare:Tare: $8$ Tare:essicator: $8-23-44$ 8:30 $17$ 18:30 $17$ 21Tare:essicator: $8-23-44$ 8:30 $17$ 18:30 $17$	7       Tare: $0. A227$ 8       Tare: $0. A220$ Time $R/H %$ 8:30 $A7%$ 68.5 $48:30$ 24       Tare:         A39,2487         essicator: $8-23-AA / A7:00$ Time $R/H %$ Temp. (F) $8:30$ A7 $68.5$ $48:30$ $A7$ $68.5$ $48.5$ $48:30$ $A7$	8Tare: $\bigcirc$ . $\land$ $220$ Preliminary $\land$ Tare:Tare:Preliminary $\land$ essicator: $\$$ -2 $\Im$ - $\land$ / $\land$ $12:00$ Preliminary $\land$ Time $\aleph$ /H %Temp. (F)Weight (grams) $\$:30$ $\land$ $12\%$ $6\$.5$ $0.2\$30$ $18:30$ $\land$ $12\%$ $6\$.5$ $0.2\$30$ $18:30$ $\land$ $12\%$ $6\$.0$ $0.2\$32$ $18:30$ $\land$ $12\%$ $139,24\$$ Preliminary $\checkmark$ essicator: $\$$ - $25$ - $\land$ $\land$ $\land$ $129,24\$$ Preliminary $\checkmark$ essicator: $\$$ - $25$ - $\land$ $\land$ $\land$ $129,24\$$ Preliminary $\checkmark$ essicator: $\$$ - $25$ - $\land$ $\land$ $\land$ $129,24\$$ Preliminary $\checkmark$ essicator: $\$$ - $25$ - $\land$ $\land$ $\land$ $129,24\$$ Preliminary $\checkmark$ essicator: $\$$ - $25$ - $\land$ $\land$ $\land$ $129,24\$$ Preliminary $\checkmark$ essicator: $\$$ - $25$ - $\land$ $\land$ $\land$ $129,24\$$ Preliminary $\checkmark$ essicator: $\$$ - $25$ - $\land$ $\land$ $\land$ $129,24\$$ Preliminary $\checkmark$ essicator: $\$$ - $25$ - $\land$ $\land$ $\land$ $129,24\$$ Preliminary $\checkmark$ essicator: $\$$ - $25$ - $\land$ $\land$ $\land$ $139,24\$$ Preliminary $\checkmark$ essicator: $\$$ - $25$ - $\land$ $\land$ $139,24\$$ Preliminary $\checkmark$ $\$$ $130$ $17$ $6\$$ $139,24$ $18:30$ $17$ $6\$$ $139,24$ $18:30$ $17$ $6\$$ $139,24$ $18:30$ $17$ $6\$$ $139,24$	$7$ Tare: $0. \ A2.2.7$ Preliminary Wt:         8       Tare: $0. \ A2.20$ Preliminary Wt:         8       Tare: $0. \ A2.20$ Preliminary Wt:         1       Tare: $0. \ A2.20$ Preliminary Wt:         essicator: $8-23-44$ $17:00$ Preliminary Wt:         Time $R/H \%$ Temp. (F)       Weight (grams)       Audit (grams) $8:30$ $A7\%$ $68.5$ $0.2530$ $0.2 = 0.2000$ $18:30$ $A7$ $69.0$ $0.2532$ $0.2 = 0.2000$ $18:30$ $A7$ $69.0$ $0.2532$ $0.2 = 0.2000$ $18:30$ $A7$ $69.0$ $0.2532$ $0.2 = 0.2000$ $2.4$ Tare: $139,2487$ Preliminary Wt: $139,2000$ $2.5 - A1 / A7$ $68.5$ $139,2493$ $200.002$ $8:30$ $17$ $68.5$ $139,2493$ $200.002$ $18:30$ $A7$ $69.0$ $139,2495$ $200.002$	7Tare: $0. A223$ Preliminary Wt: $0. A30A$ 8Tare: $0. A220$ Preliminary Wt: $0. A223$ 8Tare: $0. A220$ Preliminary Wt: $0. A223$ 1Tare:Preliminary Wt: $0. 2528$ 1 $8 - 23 - AA$ $A12300$ Preliminary Wt: $0.2528$ 1R/H %Temp. (F)Weight (grams)Audit (grams)Initials $8:30$ $A7/2$ $68.5$ $0.2530$ $0.2 = 0.2000$ $7A$ $18:30$ $A7$ $69.0$ $0.2532$ $0.2 = 0.2000$ $7A$ $18:30$ $A7$ $68.5$ $139,2487$ Preliminary Wt: $139,2484$ $8:30$ $A7$ $68.5$ $133,2493$ $200.02$ $7A$ $18:30$ $A7$ $68.5$ $139,2495$ $200.02$ $7A$ $18:30$ $A7$ $69.0$ $139,2495$ $200.02$ $7A$

Date: 11-08-11

Page 1 of 1

# **DILUTION TUNNEL WORKSHEET - METHOD 5G3**

			IONNONLLI		963			
Client: SBI	Model: XTL 1.	С.						
Project #.G.1004	Co88 Sample ID	#: HT 1109	8221414-	100				
Date: 08-24-11	Engineer: FLORit	A ANGHEL RI	un #: <u>3</u> Si	ample Train #:	A			
Balance Equipme	ent #: SBI 206 Th	nermo/Hygro met	ter Equipment #	SB1-212	-			
Audit weight Equ	ipment #:180-19	(Balance audit n	nfr. std: 500 ± 0	.72 mg)				
Front Filter #	2	Tare:	0.1216	Preliminary	Wt:	0	. 1248	
Rear Filter #	10	Tare:	0.12.18	Preliminary	Wt:	0.	1225	
Seal Set #		Tare:		Preliminary	Wt:			
Date/Time in d	essicator:	8-24-11/	18:00	Preliminary	Wt:	0.	2473	
Date	Time	R/H %	Temp. (F)	Weight (grams)	(gra	udit ams)	Initials	
8-25-11	18:30	17	63.0	0.2470	0,1 0.2.	2 =	A	ļ
8-26-11	12:15	17	63.0	0.2471	0.2	2 = 000	<del>AF</del>	],
Probe #:	23	Tare:	136,1886	Preliminary \	Nt:	13	6,1881	
Date/Time in de	essicator:	8-24-11	18:00					
Date	Time	R/H %	Temp. (F)	Weight (grams)		udit ams)	Initials	
8-25-11	18:30	17	63.0	136,1891	200.0	0.0 <i>=</i> 202	AF	
8-26-11	12:15	17	63.00	136,1830	200 200.0	0 = x02	<del>-</del>	٦
								_

Date: 11-08-11

# **DILUTION TUNNEL WORKSHEET - METHOD 5G3**

	Nodel: <u>XTN</u>	1.3					
Project #: G1004							
Date: 8-24-11 E	ingineer: FLORI	H ANGHOLR	un #: <u>3</u> Si	ample Train #:	B		
Balance Equipme	ent #: 58126 Th	ermo/Hygro me	eter Equipment #	<u>SB1-212</u>	-		
Audit weight Equi	pment #: 180-110	(Balance audit	mfr. std: 500 ± 0	.72 mg)			
Front Filter #	۸۸ Tare:		0. 1206	Preliminary Wt:		. 1237	
Rear Filter #	12_ Tare:		0.1230	Preliminary Wt: 😋		1235	
Seal Set #		Tare:		Preliminary V	Vt:		
Date/Time in dessicator:		8-24-11/18:00		Preliminary Wt:		.2472	
Date	Time	R/H %	Temp. (F)	Weight (grams)	Audit (grams)	Initials	
8-25-11	18:30	17	63.0	0.2471	0,2 = 0,2000	++-	
8-26-11	12:15	17	69.0	0.2470	0.2 = 0.2000	<del>AF</del>	
Probe #:	24	Tare:	136,0408	Preliminary Wt: 13(		5,0413	
Date/Time in de	essicator:	8-24-11	18:00				
Date	Time	R/H %	Temp. (F)	Weight (grams)	Audit (grams)	Initials	
8-25-11	18:30	イナ	69.0	136,0420		A	
8-26-11	12:15	17	63.0	136,0412			
9-12-11	18:00	16	69.9	136,0413	200.0 F 200.002	AF	L
						-	

Date: <u><u>M</u>-98-M Engineer signature: \_</u>

Page 1 of 1

## **DILUTION TUNNEL WORKSHEET - METHOD 5G3**

Client: SBI N		3		METHOD				
Project #: Gloo			221414-0	100				
Date: 8-25-11 E	ingineer: FLORI	A ANGHEL RU	in #: <u>4</u> Sa	ample Train #:	A			
Balance Equipme	nt #: SB1206 Th	ermo/Hvaro met						
Audit weight Equi	180-195 pment #:180-110	(Balance audit m	nfr. std: 500 ± 0	.72 mg)				
Front Filter #	13	Tare:	0.1220	Preliminary	Wt:	•	0. 1311	
Rear Filter #	(4	Tare:	0.1224	Preliminary	Wt:	C	D. 1232	
Seal Set #		Tare:		Preliminary	Wt:			
Date/Time in de	essicator:	8-25-NK/	18:30	Preliminary	Wt:	C	0.2543	
Date	Time	R/H %	Temp. (F)	Weight (grams)	Au (gra		Initials	
8-26-11	19:00	17	69.6	0.2539	0.2		AT	
9-12-11	17:00	16	70.0	0.2537	0,2 0,200		AF	]~
								-
								-
Probe #:	25	Tare:	136,8331	Preliminary \	Nt:	130	,8335	
Date/Time in de	essicator:	8-25-11	18:30					
Date	Time	R/H %	Temp. (F)	Weight (grams)	Au (grai		Initials	
8-25-11	19:00	7	69.6	136,8340	200.0	0,0= 002	A	
9-12-11	N7:00	16	70.0	136,8336	200 200.0		A	] -
								and the second

Date: \_\_\_\_\_ 0 8- 11

Engineer signature:

## **DILUTION TUNNEL WORKSHEET - METHOD 5G3**

Client: SBI	Model: XTD1.	9						
Project #: G1004	56088 Sample I	#: MTL MOS	8221414-	100				
Date: 8-25-11	Engineer: FLORIN	A ANGHEL RI	un #: 4 S	ample Train #:	B			
Balance Equipme	Date: 8-25-11 Engineer: FLORIN ANGHEL Run #: 4 Sample Train #: B Balance Equipment #: 581206 Thermo/Hygro meter Equipment # : 581212							
Audit weight Equ	ipment #280-195	(Balance audit n	nfr. std: 500 ± 0	).72 mg)				
Front Filter #	15	Tare:	0.1233	Preliminary	Wt:	c	0.1325	٦
Rear Filter #	16	Tare:	0.1229	Preliminary	Wt:		0.1236	
Seal Set #		Tare:		Preliminary	Wt:			
Date/Time in d	essicator:	8-25-11/	18:30	Preliminary	Wt:	C	.2561	1
Date	Time	R/H %	Temp. (F)	Weight (grams)	Au (gra		Initials	-
8-26-11	19:00	17	69.6	0.2559	0.20	2 ≠ ∞	<del>\\</del>	
9-12-11	17:00	16	70.0	0.2560	0.20	2=	TA	1
								1
Probe #:	26	Tare:	139,828.9	Preliminary \	A/+-			-
						1 22	,829.8	1
Date/Time in de	essicator:	8-25-11	18:30					
Date	Time	R/H %	Temp. (F)	Weight (grams)	Auc (gran	ns)	Initials	
8-26-11	19:00	17	69.6	139,829.8	200.0	02	<del>AF</del>	
9-12-11	17:00	16	70.0	139,829.3	200	20-	Ŧ	1.
								]
								1
								1

Date: <u>\\-</u>08-\\

Engineer signature:

## **DILUTION TUNNEL WORKSHEET - METHOD 5G3**

Olivert CRI					/v c	JKKSHEEI	- WEIHUD	563			
					8-	22 Aleale					
Project #: Call	Project #: <u>G10045088</u> Sample ID #: <u>MTL</u> 1108221414 - 001										
Date: 8-26-11 Engineer: <u>FLOPIH ANGHEL Run #: 5</u> Sample Train #: <u>A</u> Balance Equipment #: <u>SB1-26</u> Thermo/Hygro meter Equipment # : <u>SB1-212</u>											
	oment	nent #: <u>\80-130</u>	ermo/	Hygro me	ete	r Equipment #	281-212				
			(Balar		mt						-
Front Filter	#	17		Tare:		0.1230	Preliminary	Wt:	6	0.1245	
Rear Filter #	¥	18		Tare:		0.1223	Preliminary	Wt:	٩	2.12.27	
Seal Set #				Tare:			Preliminary V	Wt:			
Date/Time in	n des	sicator:	8-2	-6-41/	1	12:15	Preliminary	Nt:	C	0.2472	
Date		Time	I	R/H %		Temp. (F)	Weight (grams)	(gra	udit ams)	Initials	
9-12-11		17:00		YC		0.0F	0.2473	0.20	2 =	TA	
10-20-1		9:30		6		୍ଟେ.୨	1246/.1225 0.2471	0.2	2. ≘ 000	<del>\\</del>	١.
Probe #:		27		Tare:	13	36,9020	Preliminary V	Vt:	136	5,9023	1
Date/Time in	n dess	sicator:	8-:	26-11	/	12:15					
Date		Time	F	VH %		Temp. (F)	Weight (grams)		udit ams)	Initials	
9-12-11	X	A:00	٨	6		0.0f	136,3027	200 200	0.0 = .002	AF	
10-20-11		9:30	٦	6		63.5	136,9026	200	2.0.6	AF	$\mathbf{F}$
10-21-11		9:00	٨	6		70.0	136,9024	200.0	.0= 002	Ŧ	
											1
	_										

Date: <u>11-08-11</u>

Engineer signature:

			ORKSHEET	- METHOD	5G3			
	Client: $\underline{SBI}$ Model: $\underline{\times TD}$ 1.3							
Project #: 4004	CO88 Sample ID	#: HTLANO	8221414-0	$\infty \gamma$				
Date: 8-26-11 E					B			
Balance Equipme Audit weight Equi	180-191							
Front Filter #	49	Tare:	0.1222	Preliminary	Wt:	0	1239	1
Rear Filter #	20	Tare:	0. 1175	Preliminary	Wt:	0	CFJI.	
Seal Set #		Tare:		Preliminary	Wt:			
Date/Time in de	essicator:	8-26-11	12:15	Preliminary V	Wt:	O,	.2418	
Date	Time	R/H %	Temp. (F)	Weight (grams)	Au Au		Initials	
9-12-11	17:00	λς	70.0	0.245	0.20	- 0	ĀF	]
10-20-11	9:30	16	63.5	·124 /.1176 0.2416	0.2	2 = 000	-74-	-
								1
								1
Probe #:	28	Tare:	136,2238	Preliminary V	/Vt:	136	,2238	
Date/Time in de	ssicator:	8-26-M/	12:15					]
Date	Time	R/H %	Temp. (F)	Weight (grams)	Aud (grai		Initials	
9-12-11	17:00	46	70.0	136,2240	200. 200. c		ŦÆ	]
10-20-11	9:30	16	63.5	136,2242	200.0	202	¥	]~
10-21-11	9:00	16	70.0	136,2240	200.0 200.0	0 =		]

Date:  $\frac{11-08-11}{1000}$ 

Engineer signature:

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Appendix D

Calibrations

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No du rapport d'étalonnag CA0003-088-032111 Mettler Toledo Service Business Unit Industrial 1900 Polaris Parkway Columbus, Ohio 43240 1-800-METTLER

# **METTLER TOLEDO**

ISO 9001 Registered ANSI/NCSL Z540 Accrédité



Accrédité par l'American Association of Laboratory Accreditation (A2LA) CERT.CALIBRATION #1902.02

## Certificat d'étalonnage

#### Client

Société :	SBI Fabricant de poêles International	inc.	
Adresse :	250, rue Copenhague		
Ville :	St-Augustin	État/Province :	Québec
Code postal :	G3A 2V1	Astea Customer ID:	C037589001001
Instrument			
Constructeur :	Rice Lake	Modèle de terminal :	IND560
Modèle :	Roughdeck	No de série du termin	00927396KL
No de série :	B00927396KL	No, Série Impr.	N/A
Capacité :	625 kg	Service/Pièce :	Lab
Résolution :	0.02 kg	Nbre de Divisions	31250
Classe :	111	Procédure utilisée :	Canadien
Numéro/ID d'actif du clie	SBI-013		
Procédure:	Le présent certificat est émis conform l'A2LA, en vertu de la norme ISO/IEC laboratoire et la traçabilité des normes	17025, A2LA a évalué la	certification accordées par capacité de mesure du
Date de calibrage :	21-mars-2011	Le prochain Cal Date	31-mars-2012
Signataire autorisé (A2LA) :	Dany Careau	Signature:	ELECTRONIC SIGNATURE
Signature du client			

## Étalons de travail

raçabilité	Les poids de test utilisés se réfèrent au National Institute of Standards and Technology.						
Jeu de poids no :	Traçabilité NIST No.:	Classe ASTM/OIML	Date d'étalonnage :	Date proch. étalonnage			
42268	M10-0278	M1	5-août-2010	5-août-2011			
MTP1	MT0015626	F1	17-sept2010	17-sept2011			
Kit S	1356103	M1	5-oct2010	5-oct2011			

No du rapport d'étalonnag CA0003-088-032111

## **METTLER TOLEDO**

## Résultats de mesure

La température :

70 °F

Les conditions ambiantes ont été vérifiées afin d'assurer l'exactitude de l'étalonnage.

## Test de variation



n -		Avant Réglage	Après Réglage
Les poids Appliqués	Position	Valeur lue	Valeur lue
1: 125 kg	Position 1	125.02 kg	124.98 kg
2: 125 kg	Position 2	125.16 kg	125,02 kg
3: 125 kg	Position 3	125.16 kg	125.02 kg
4: 125 kg	Position 4	125.26 kg	125.00 kg
Erreur maximum :		0.26 kg	0.04 kg
Max Erreur Admissible		0.10 kg	0.1 kg

#### Linéarité

		Avant réglage						
	Les poids Appliqués	Valeur lue	Erre	eur	Erreur admissible	Dans la Tolérance		
Zero 1	0.00 kg	0.00 kg	0.00 kg	0 d	1 d	OUI		
2	20.00 kg	20.02 kg	0.02 kg	1 d	2 d	OUI		
3	40.00 kg	40.04 kg	0.04 kg	2 d	2 d	OUI		
4	100.00 kg	100.12 kg	0.12 kg	6 d	5 d	NON		
Max 5	200.00 kg	200.24 kg	0,24 kg	12 d	5 d	NON		
6	100.00 kg	100.12 kg	0.12 kg	6 d	5 d	NON		
7	40.00 kg	40.04 kg	0.04 kg	2 d	2 d	OUI		
8	20.00 kg	20.02 kg	0.02 kg	1 d	2 d	OUI		
Zero 9	0,00 kg	0.00 kg	0.00 kg	0 d	1 d	OUI		

Méthode de substitution utilisée

Version Logiciel : 4.3.0.7

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#### No du rapport d'étalonnag CA0003-088-032111

## **METTLER TOLEDO**

			Après régla	ge		
	Les poids Appliqués	Valeur lue	Erre	eur	Erreur admissible	Dans la Tolérance
Zero 1	0.00 kg	0.00 kg	0.00 kg	0 d	1 d	OUI
2	20.00 kg	20.00 kg	0,00 kg	0 d	2 d	OUI
3	40,00 kg	40.00 kg	0.00 kg	0 d	2 d	OUI
4	100.00 kg	100.02 kg	0.02 kg	1 d	5 d	OUI
Max 5	200.00 kg	200.02 kg	0.02 kg	1 d	5 d	OUI
6	100.00 kg	100.02 kg	0.02 kg	1 d	5 d	OUI
7	40.00 kg	40.00 kg	0.00 kg	0 d	2 d	OUI
8	20.00 kg	20.00 kg	0.00 kg	0 d	2 d	OUI
Zero 9	0.00 kg	0.00 kg	0,00 kg	0 d	1 d	OUI

Méthode de substitution utilisée

Un réglage de la balance a été requis

Si NON, les résultats relatifs à l'état du système avant la prestation de service correspondent à l'état de

🗹 oui

#### Répétabilité

Poid	s appliqués : 100.00 kg		
	Chargé	Vide	Différence
1	100.00 kg	0.00 kg	100 kg
2	100.02 kg	0.00 kg	100.02 kg
3	100.02 kg	0.00 kg	100.02 kg
	Erreur maximale :	0.02 kg	1.0 d
	Tolérance :	0.10 kg	5 d

NON

#### Incertitude

Mesure de l'incertitude = \_\_\_\_0.022 kg

Les meilleures incertitudes représentent les incertitudes étendues selon un facteur de sécurité K=2 générant un niveau de confiance approximatif de 95 %. Des dispositions doivent être prises en matière d'environnement au lieu d'étalonnage, d'incertitude induite par l'article en étalonnage et d'effets indésirables causés par le transport du matériel d'étalonnage. Ces facteurs pourraient entraîner une incertitude plus grande que le BMC.

#### Remarques

Aucune

Version Logiciel : 4.3.0.7

Page 3 sur 3 © METTLER TOLEDO

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No du rapport d'étalonnag CA0003-086-032111 **Mettler Toledo** Service Business Unit Industrial 1900 Polaris Parkway Columbus, Ohio 43240 1-800-METTLER

# **METTLER TOLEDO**

ISO 9001 Registered ANSI/NCSL Z540 Accrédité



Accrédité par l'American Association of Laboratory Accreditation (A2LA) CERT.CALIBRATION #1902.02

## Certificat d'étalonnage

#### Client

Société :	SBI Fabricant de poêles International	inc.	
Adresse :	250, rue Copenhague		
Ville :	St-Augustin	État/Province :	Québec
Code postal :	G3A 2V1	Astea Customer ID:	C037589001001
Instrument			
Constructeur :	Weightronix	Modèle de terminal :	IND560
Modèle :	DSL-6060	No de série du termin	00927386KL
No de série :	B00927386KL	No. Série Impr.	N/A
Capacité :	500 kg	Service/Pièce :	LAB
Résolution :	0.02 kg	Nbre de Divisions	25000
Classe :	III	Procédure utilisée :	Canadien
Numéro/ID d'actif du clie	SBI-014		
Procédure:	Le présent certificat est émis conform l'A2LA, en vertu de la norme ISO/IEC laboratoire et la traçabilité des normes	17025. A2LA a évalué la	
Date de calibrage :	21-mars-2011	Le prochain Cal Date	31-mars-2012
Signataire autorisé (A2LA) :	Dany Careau	Signature	ELECTRONIC SIGNATURE
Signature du client			

## Étalons de travail

açabilité	Les poids de test utilisés se réfèrent au National Institute of Standards and Technology.						
Jeu de poids no :	Traçabilité NIST No.:	Classe ASTM/OIML	Date d'étalonnage :	Date proch, étalonnage			
42268	M10-0278	M1	5-août-2010	5-août-2011			
MTP1	MT0015626	F1	17-sept2010	17-sept-2011			
Kit S	1356103	M1	5-oct2010	5-oct2011			

No du rapport d'étalonnag CA0003-086-032111

70 °F

## **METTLER TOLEDO**

## Résultats de mesure

La température :

Les conditions ambiantes ont été vérifiées afin d'assurer l'exactitude de l'étalonnage.

#### **Test de variation**



Υ.		Avant Réglage	Après Réglage
Les poids Appliqués	Position	Valeur lue	Valeur lue
1: 125.00 kg	Position 1	125.00 kg	125.00 kg
2: 125.00 kg	Position 2	125.04 kg	125.00 kg
3: 125:00 kg	Position 3	125.00 kg	125.00 kg
4: 125.00 kg	Position 4	124.96 kg	125.00 kg
Erreur maximum :		0.08 kg	0.00 kg
Max Erreur Admissible		0.10 kg	0.1 kg

#### Linéarité

	Avant réglage								
	Les poids Appliqués	Valeur lue	Erre	eur	Erreur admissible	Dans la Tolérance			
Zero 1	0.00 kg	0.00 kg	0,00 kg	0 d	1 d	OUI			
2	20.00 kg	20.00 kg	0.00 kg	0 d	2 d	OUI			
3	40.00 kg	40.00 kg	0.00 kg	0 d	2 d	OUI			
4	100.00 kg	100.02 kg	0.02 kg	1 d	5 d	OUI			
Max 5	200.00 kg	200.04 kg	0.04 kg	2 d	5 d	OUI			
6	100.00 kg	100.02 kg	0.02 kg	1 d	5 d	OUI			
7	40.00 kg	40.00 kg	0.00 kg	0 d	2 d	OUI			
8	20.00 kg	20.00 kg	0.00 kg	0 d	2 d	OUI			
Zero 9	0.00 kg	0.00 kg	0.00 kg	0 d	1 d	OUI			

Méthode de substitution utilisée

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No du rapport d'étalonnag CA0003-086-032111

## **METTLER TOLEDO**

	Après réglage								
	Les poids Appliqués	Valeur lue	Erre	əur	Erreur admissible	Dans la Tolérance			
Zero 1	0.00 kg	0.00 kg	0.00 kg	0 d	1 d	oui			
2	20.00 kg	20.00 kg	0.00 kg	0 d	2 d	OUI			
3	40.00 kg	40.00 kg	0,00 kg	0 d	2 d	OUI			
4	100.00 kg	100.00 kg	0.00 kg	0 d	5 d	OUI			
Max 5	200.00 kg	200.00 kg	0.00 kg	0 d	5 d	oui			
6	100.00 kg	100.00 kg	0.00 kg	0 d	5 d	OUI			
7	40.00 kg	40.00 kg	0.00 kg	0 d	2 d	OUI			
8	20.00 kg	20.00 kg	0.00 kg	0 d	2 d	OUI			
Zero 9	0.00 kg	0.00 kg	0.00 kg	0 d	1 d	OUI			

Méthode de substitution utilisée

Un réglage de la balance a été requis

Si NON, les résultats relatifs à l'état du système avant la prestation de service correspondent à l'état de

🗹 oui

#### Répétabilité

Poid	s appliqués : 100.00 kg	L	
	Chargé	Vide	Différence
1	100.00 kg	0.00 kg	100 kg
2	100.02 kg	0.00 kg	100.02 kg
3	100.00 kg	0.00 kg	100 kg
	Erreur maximale :	0.02 kg	1.0 d
	Tolérance :	0.10 kg	5 d

NON

#### Incertitude

Mesure de l'incertitude = 0.022 kg

Les meilleures incertitudes représentent les incertitudes étendues selon un facteur de sécurité K=2 générant un niveau de confiance approximatif de 95 %. Des dispositions doivent être prises en matière d'environnement au lieu d'étalonnage, d'incertitude induite par l'article en étalonnage et d'effets indésirables causés par le transport du matériel d'étalonnage. Ces facteurs pourraient entraîner une incertitude plus grande que le BMC.

#### Remarques

Aucune

Version Logiciel : 4.3.0.7

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No du rapport d'étalonnag CA0003-090-032111 Mettler Toledo Service Business Unit Industrial 1900 Polaris Parkway Columbus, Ohio 43240 1-800-METTLER

# **METTLER TOLEDO**

ISO 9001 Registered ANSI/NCSL Z540 Accrédité



Accrédité par l'American Association of Laboratory Accreditation (A2LA) CERT.CALIBRATION #1902.02

## Certificat d'étalonnage

## Client

Société :	SBI Fabricant de poêles Int		
Adresse :	250, rue Copenhague		
Ville :	St-Augustin	État/Province :	Québec
Code postal :	G3A 2V1	Astea Customer ID:	C037589001001
nstrument			-
Constructeur :	Mettler Toledo	Modèle de terminal :	IND560
Modèle :	2256 kg	No de série du termin	00927336KL
No de série :	B00927336KL	No. Série Impr.	N/A
Capacité :	625 kg	Service/Pièce :	Lab
Résolution :	0.02 kg	Nbre de Divisions	31250
Classe :	ш	Procédure utilisée :	Canadien
Numéro/ID d'actif du clie	SBI-186		
Procédure:	l'A2LA, en vertu de la norme	s conformément aux conditions de c e ISO/IEC 17025. A2LA a évalué la les normes nationales reconnues.	
Date de calibrage :	21-mars-2011	Le prochain Cal Date	31-mars-2012
Signataire autorisé (A2LA) :	Dany Careau	Signature:	ELECTRONIC SIGNATURE
Signature du client			

## Etalons de travail

Traçabilité Les poids de test utilisés se réfèrent au National Institute of Standards and Technology,							
Jeu de poids no :	Traçabilité NIST No.	Classe ASTM/OIML	Date d'étalonnage :	Date proch. étalonnage			
42268	M10-0278	M1	5-août-2010	5-août-2011			
MTP1	MT0015626	F1	17-sept2010	17-sept2011			
Kit S	1356103	M1	5-oct2010	5-oct2011			



Version Logiciel : 4.3.0.7 No du rapport d'étalonnag CA0003-090-032111

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## **METTLER TOLEDO**

## Résultats de mesure

La température :

Les conditions ambiantes ont été vérifiées afin d'assurer l'exactitude de l'étalonnage.

## Test de variation



		Avant Réglage
Les poids Appliqués	Position	Valeur lue
1: 125 kg	Position 1	124,98 kg
2: 125 kg	Position 2	124.98 kg
3: 125 kg	Position 3	125.02 kg
4: 125 kg	Position 4	125,00 kg
Erreur maximum :		0.04 kg
Max Erreur Admissible :		0.10 kg

#### Linéarité

	Avant réglage								
	Les poids Appliqués	Valeur lue	Erre	əur	Erreur admissible	Dans la Tolérance			
Zero 1	0.00 kg	0.00 kg	0.00 kg	0 d	1 d	OUI			
2	20.00 kg	20.00 kg	0,00 kg	0 d	2 d	OUI			
3	40.00 kg	40.00 kg	0.00 kg	0 d	2 d	OUI			
4	100.00 kg	100.00 kg	0.00 kg	0 di	5 d	OUI			
Max 5	200.00 kg	200.00 kg	0.00 kg	0 d	5 d	OUI			
6	100.00 kg	100.00 kg	0.00 kg	0 d	5 d	OUI			
7	40.00 kg	40.00 kg	0.00 kg	0 d	2 d	OUI			
8	20.00 kg	20.00 kg	0.00 kg	0 d	2 d	OUI			
Zero 9	0,00 kg	0.00 kg	0.00 kg	0 d	1 d	OUI			

Méthode de substitution utilisée

Un réglage de la balance a été requis

Si NON, les résultats relatifs à l'état du système avant la prestation de service correspondent à l'état de

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Version Logiciel : 4.3.0.7 No du rapport d'étalonnag CA0003-090-032111

## **METTLER TOLEDO**

#### Répétabilité

Poids appliqués : 100.00 kg

	Chargé	Vide	Différence
1	100.00 kg	0.00 kg	100 kg
2	100.00 kg	0.00 kg	100 kg
3	100.00 kg	0.00 kg	100 kg
	Erreur maximale :	0.00 kg	0.0 d
	Tolérance :	0.10 kg	5 d

#### Incertitude

Mesure de l'incertitude = 0.012 kg

Les meilleures incertitudes représentent les incertitudes étendues selon un facteur de sécurité K=2 générant un niveau de confiance approximatif de 95 %. Des dispositions doivent être prises en matière d'environnement au lieu d'étalonnage, d'incertitude induite par l'article en étalonnage et d'effets indésirables causés par le transport du matériel d'étalonnage. Ces facteurs pourraient entraîner une incertitude plus grande que le BMC.

#### Remarques

Aucune.



## Certificat d'Étalonnage

Groupe de service des instruments 1-800-267-6633			# 724396	- 01*		
Client: SBI Stove Builder Inte	rnational		Local: Metrolog	gie		
St-Augustin de Desma	ures		Modèle : TE21	4S		
Balance			# Série : 25851066			
Liste des Vérification	codes		Spécifica	tions : Fabricant: 🛛	Client:	
Câble d'alimentation	ОК	Capacité : 210 g		Tolérance : 0.2 m	a	
Sélecteurs, clavier, commandes	ОК	Résolution : 0.1 mg	g			
Circuits imprimés	ок				Charge Maximale	
Mécanisme de pesée	ок		Relevées d	des vérifications		
Poids d'étalonnage interne	N/A		Référence	Tel que trouvé	Tel que laissé	
Horizontalité	ок	⊠ g □ mg	0.0500	0.0500	0.0500	
Plateau et support de plateau	ОК	🖾 g 🗆 mg	5.0000	5.0056	5.0000	
Boîtier et housse	ОК	⊠g □ mg	50.0000	50.0564	50.0001	
Vitres	ОК	⊠g □ mg	200.0000	200.2254	200.0000	
Fonction de tarage Fonction Auto-Calibration Hysteresis		Répond aux spécificat Répond aux spécificat	-			
Charges excentrées Tolérance : ±		4 1 2	1 2 4 3 P	Charges excentré Poids d'essai: 100 ⊠		
Commentaires :			Tel que laissé :			
		Centre: <u>0.0000</u>	Centre: 0.0000			
		1: 0.0000	1: 0.0000		ond aux spécifications :	
		2: 0.0000 3: 0.0000	2: 0.0000 3: 0.0000	Tel que trouvé : [  Tel que laissé : [		
			4: 0.0000	1 di que iaisse . L		
Codes : OK = , vérifié , étal		N/A = non applicab		gé Déf = défectueux R	Remp = Remplacer	
Étalons certifiés		Représentant de	e service :	Daniel Toulouse Doniel -	Digitally signed by Daniel Toulouse Tanon Qate: 2010.11.15	
Jeu de poids QUE014		Date d'étalonna	ige :	15 Novembre 2010	14:41:43 -05:00	
		Prochaine date	d'étalonnage :	30 Novembre 2011		
		Approbation du	client :	-		
		Date:				

## Thermal Metering System Calibration Y factor for Method 5G sampling

Manufacturer:	American Meter Company
Model:	DTM-200A
Serial Number:	90R054300
	Average Gas Meter y Factor 1,000
Calibration Date:	04-28-11
Calibrated by:	Claude Paré
Calibration Frequency:	6-month
Next Calibration Due:	10-27-11
Instrument Range:	1,000 cfm
Standard Temp.:	67 oF
Standard Press.:	29,92 "Hg
Barometric Press,:	29,66 "Hg
Signature/Date:	Clarka 2011-04-28

#### **Previous Calibration Comparision**

Date	N/A	Acceptable	
		Deviation (5%)	Deviation
y Factor	1,003	5	0,003
Acceptance	Acc		

ut Calibration
ition 0,020
ion 0,003
Acceptable

	Reference	: Standard *	
Standard	Model	Standard Test	Meter
Calibrator	S/N	07J264834	
	Calib. Date	21-mars-11	
	Calib. Value	0,9930	y factor (ref)

Calibration Parameters	Run I	Run 2	Run 3
Vacuum ("Hg)	0,00	0,00	0,00
dH ("H2O)	0,00	0,00	0,00
Initial Reference Meter	543,9	549,1	554,5
Final Reference Meter	548,9	554,3	559,8
Initial DGM	462,625	467,778	473,129
Final DGM	467,581	472,933	478,407
Temp. Ref. Meter (°F), Tr	67,0	67,0	68,0
Temperature DGM (°F), Td	67,0	67,0	68,0
Time (Minutes)	45,5	48,0	50,0
Net Volume Ref. Meter, Vr	5,000	5,200	5,300
Net Volume DGM, Vd	4,956	5,155	5,278
Gas Meter y Ractor =	1,002	1,002	0,997
Gas Meter y Factor Deviation (from avg.)	0,002	0,001	0,003
Orifice dH@	0,00	0,00	0,00
Orifice dH@ Deviation (from avg.)	0,000	0,000	0,000

where:

0,108923077

L. Deviation = [Average value for all runs - current run value]

2. y = [Vr x (y factor (ref)) x (Pb) x (Td + 460) / [Vd x (Pb + (dH / 13.6)) x (Tr + 460]]

3. dH@ = 0.0317 x dH / (Pb (Td + 460)) x { (Tr + 460) x time) / Vr }^2

\* Reference calibration is traceable to NIST through NIST Test # 40674, Kimble ASTM E1272

## Thermal Metering System Calibration Y factor for Method 5G sampling

Manufacturer:	American Meter Con	npany
Model:	DTM-200A	
Serial Number:	98Z33	2226
		Average Gas Meter y Factor 0,996
Calibration Date:	04-28	.11
Calibrated by:	Claude Paré	
Calibration Frequency:	6-mo	ath
Next Calibration Due:	10-27-11	
Instrument Range:	1,000	cfm
Standard Temp.;	71	oF
Standard Press.:	29,92	"Hg
Barometric Press.:	29,49	"Hg
Signature/Date;	Vala	2011-04-28

#### **Previous Calibration Comparision**

Date	N/A	Acceptable	
		Deviation (5%)	Deviation
y Factor	0,996	5	0,000
Acceptance	Acc	ceptable	

# Current Calibration Acceptable y Deviation 0,020 Maximum y Deviation 0,001 Acceptance Acceptable

	Reference	Standard *	
Standard	Model	Standard Test	Meter
Calibrator	S/N	07J264834	
	Calib. Date	21-mars-11	
	Calib. Value	0,9930	y factor (ref)

Calibration Parameters	Run 1	Run 2	Run 3
Vacuum ("Hg)	0,00	0,00	0,00
dH ("112O)	0,00	0,00	0,00
Initial Reference Meter	560,3	565,5	\$73
Final Reference Meter	565,3	572,8	578
Initial DGM	552,783	557,957	565,424
Final DGM	557,76	565,228	570,396
Temp. Ref. Meter (°F), Tr	70,5	71,0	71,0
Temperature DGM (°F), Td	70,0	70,0	70,0
Time (Minutes)	50,5	72,0	48,5
Net Volume Ref. Meter, Vr	5,000	7,300	5,000
Net Volume DGM, Vd	4,977	7,271	4,972
Gas Meter y Factor =	0,997	0,995	0,997
Gas Meter y Factor Deviation (from avg.)	0,001	0,001	0,001
Orifice dil@	0,00	0,00	0,00
Orifice dH@ Deviation (from avg.)	0,000	0,000	0,000

where:

0,098554455

I. Deviation = [Average value for all runs - current run value]

2. y = [Vr x (y factor (ref)) x (Pb) x (Td + 460) / [Vd x (Pb + (dH / 13.6)) x (Tr + 460]]

3.  $dH@ = 0.0317 \text{ x } dH / (Pb (Td + 460)) \text{ x } [ (Tr + 460) \text{ x time}) / Vr ]^2$ 

\* Reference calibration is traceable to NIST through NIST Test # 40674, Kimble ASTM E1272

## CERTIFICATE OF NIST TRACEABLE CALIBRATION

## Calibration Certificate No: 24648

Customer Information

Customer: SBI St-Augustin

Address : 250, De Copenhague Doors 11-12

Customer PO #: 23966 St-Augustin-de-Desmaures

## **Calibration Procedure Information**

Procedure ID: GTP FLOW\_INDI

Graftel ID

Revision #: 3

Colliburation Standard, I. C.

Revision Date: 7/21/2008

CAL Due

	Canbration Standar	as Information
Manufacturer	Model #	Description

10159	LIODO	1112 011	Tender in the second	CALIDA
101.22	НОВО	U12-011	Environment Monitor System	6/22/2011
60030	Paroscientific	760-100A	Pressure, 100 psia	8/24/2011
10128	Furness	FCO352	Diff Pressure	8/24/2011
		100004	2.11 ( 1030010	0/24/2011
10062	Graftel	9202	5-Channel Temperature Sensor	8/28/2012
10075	Meriam	50MJ10-9	Laminar Flowmeter	6/23/2011
610 un				
51202	Paroscientific	760-100A	Pressure, 100 Psia	2/24/2012

	Sensor Information	
Manufacturer: American Meter	Description: Gas Meter	Method Used: Laminar
Model #: DTM-200A	Rated Accuracy: ± 1 % of Reading	Accuracy Specified By: American Met.
Instrument ID#: SBI-103	Range: 0 to 250 soft	Condition: Functional
Serial #: 07J264834		Cononton: Parictional

Comments: Calibration Date: 03-21-2011

The instruments(s) listed on this certificate have been calibrated against standards traceable to the National Institue of Standards and Technology (NIST) or compared to nationally or Internationally recognized consensus standards. The reported calibration uncertainty has a confidence level of 95% (K=2). A calibration uncertainty ratio of 4:1 was maintained unless required uncertainty support by analysis Graftel, Inc. Quality Assurance System complies with applicable requirements of ISO/IEC-17025-2005, ANSI/NCSL Z540-1-1994 and ISO 9002. 1994(E). All results contained within this certification relate only to item(s) calibrated. This certificate shall not be reproduced except in full and with the written consent of Graftel, Inc.

Performed By:

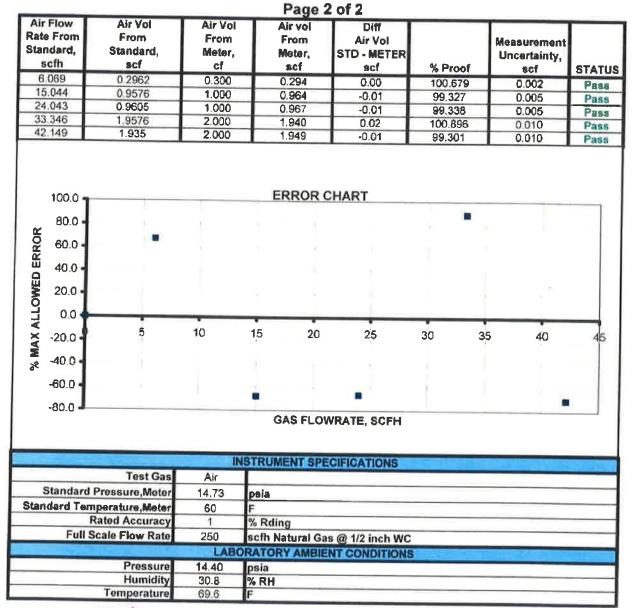
M. Rodriguez Calibration Technician

Date: 3/21/11

Page 1 of 2



## ATTACHMENT TO CALIBRATION CERTIFICATE 24648 AS FOUND DATA



Flow - Humidity - Temperature - Pressure - Design - Consulting - Engineering NIST Traceable Calibration Data Sheet Graftel, LLC, #70 Cambridge Drive, Els Grave Village, 12,80007 P. 847-384-2000 F. 847-384-2000

Date: 12/7/2010

Equipment: SBI-134 (T1) Accuracy: 0.2 Reference: SBI-096

Temperature: 71 F R.H.: 41%

 S.D.
 0.00
 %

 R.M.U.
 0.29
 %

 D.M.U
 0.60
 %

 D.M.U
 0.60
 %

 D.M.U
 0.60
 %

 Standard
 Reading
 A.D.

 TO.0
 70.0
 0.00
 %

 TO.0
 70.0
 69.8
 0.29

 TO.0
 70.0
 0.00
 0.00

A.D. 0.05 0.04
-------------------

Technician: Claude Paré

 $\bigcirc$ 

 S.D.
 0.00
 %

 R.M.U.
 0.10
 %

 **O.M.U 0.45** %

 Ave A.D.
 0.20
 %

 Standard
 Reading
 A.D.

 200.0
 199.6
 0.20

 200.0
 199.6
 0.20

 200.0
 199.6
 0.20

 200.0
 199.6
 0.20

	0.04	1399.4	1400.0
	0.04	1399.4	1400.0
	0.04	1399.4	1400.0
	A.D.	Reading	Standard
%	0.04	Ave A.D.	
	%	0.09	0.M.U
	%	0.01	R.M.U.
	%	0.00	S.D.

S.D.	0.00	%	
R.M.U.	0.03	%	
0.M.U	0.21	%	
	Ave A.D.	0.10	%
Standard	Reading	A.D.	
600.0	599.4	0.10	
600.0	599.4	0.10	
600.0	599.4	0.10	

Date: 12/7/2010

Equipment: SBI-134 (T2) Accuracy: 0.2 Reference: SBI-096 Température: R.H.:

R.M.U. S.D. 0.02 0,29 **2.36** Ave A.D. Reading 1.14 %

Standard

A.D.

%

70.0 70.0 70.0

70.8 70.8 70.8

1.14 1.14 1.14

S.D.	0.00	%	
R.M.U.	0.02	%	
0.M.U	0.09	%	
	Ave A.D.	0.04	%
Standard	Reading	A.D.	
1000.0	1000.4	0.04	
1000.0	1000.4	0.04	
1000.0	1000.4	0.04	

Technician: Claude Paré

0

71 F 41%

S.D.	0.00	%	
R.M.U.	0.10	%	
0.M.U	0.45	%	
	Ave A.D.	0.20	%
Standard	Reading	A.D.	
200.0	200.4	0.20	
200.0	200,4	0.20	
200.0	200.4	0.20	

S.D.	0.00	%	
R.M.U.	0.01	%	
0.M.U	0.03	%	
	Ave A.D.	0.01	%
standard	Reading	A.D.	
1400.0	1400.2	0.01	
1400.0	1400.2	0.01	
1400.0	1400.0	222	

0.03	600.2	600.0
0.03	600.2	600.0
0.03	600.2	600.0
A.D.	Reading	Standard
0.03	Ave A.D.	
%	0.09	0.M.U
%	0.03	R.M.U.
%	0.00	S.D.



Ulrich Métrologie inc. **Uirich Metrology Inc.** 9912, Côle-de-Liesse Moniréal (Québec) H8T 1A1

Tél. (514) 631-6653 Fax (614) 631-6122 info@ulrich.ca www.uirich.ca

## CALIBRATION CERTIFICATE

Certificate no.: 228051 Identification: SBI-096 **Description:** CALIBRATOR, OMEGA CL23A Size: TC K/J/T Manufacturer: OMEGA Model no.: CL23A Serial no.: T-256137

SBI

Calibration date	August 09, 2010
Certificate issued	August 09, 2010
Interval:	12 months
Due date;	August 9, 2011
Procedure no.:	MET/CAL
Environment:	CLAS Type 2 Laboratory
Temperature:	23 ± 2°C
Humidity:	35 - 55% RH
Metrologist:	NFS

#### Property of:

250 RUE DE COPENHAGUE ST-AUGUSTIN-DE-DESMAURES, QC G3A 2H3

Approved by:

Nuccio Mercuri, Lab Manager

This calibration certificate is issued in accordance with the applicable requirements of ISO/IEC 1702S and QM-98. Measurement results provided are traveable to either the National Research Council Canada (NRC), the National Institute of Standards and Technology (NIST), a national Informatory of another exontry signatory to the CTPM Mutual Recognition Arrangement (MRA), or a culturation laboratory accessived by an accrediting body with which Canada has an equivalence agreement.

#### CALIBRATION STANDARDS

See notes below.

#### MEASUREMENT UNCERTAINTY

The above listed instrument meets or exceeds all specifications as stated in the reference procedure, unless noted otherwise. For measurement results associated with the conformance to a tolerance, the uncertainty in the measurement system did not exceed 25% (4:1 test uncertainty ratio) of the acceptable tolerance for each characteristic calibrated, unless otherwise noted in the report

#### CALIBRATION DATA

See next page for measurement results.

Notes:

9V battery replaced.



Ulrich Métrologie Inc. - Utrich Metrology Inc. 9912, Côte-de-Liesse Tél. 1514) 631-6653

Lachine, QC H8T1A1

www.ulrich.ca

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## CALIBRATION DATA

Certificate No.228051

Instrument ID;	SBI-096	Res
Туре:	CALIBRATOR THERMOMETER	Con
Serial no.:	T-256137	001
Procedure:	Omega CL23A: 5520A-M	

Result: PASS Condition: FOUND-LEFT

Standard ID	Туре	Manufacture	ŕ	Model no.	Cal. Date	Due Date
7870009	CALIBRATOR	FLUKE		5520A	2010/04/23	2011/04/2:
MEASUREMENT	RESULTS (Per MET/CAL)					
PARAMETER	TRUE	TEST	ACCEPTANCE	LIMITS	PASS/	
FARADITER	VALUE	RESULT	LOW	RIGH	FAIL	TUR
DISPLAY CALIB	RATION					
Did all segmen	ats of the display illuminate?					
Result of Open	rator Evaluation				PASS	
HERMOMETER CA	C TREAMING				endu	
(Type Thermod						
-200,0deqF	oubre					
60,0deqF		-200.8	-201.0	-199.0	PASS	1.7
40.0degF		-60.6	-61.0	-59.0	PASS	3.1
32.0degF		-40.5	-40.5	-39.5	PASS	1.5
1240.0degF		31.6	31.5	32.5	PASS	1.7
1240.00egF		1239.6	1239.5	1240.5	PASS	1.1
2500.0degF		1259.6	1259.5	1260.5	PASS	1.1
Type Thermor	1	2499.5	2499.0	2501.0	PASS	1,4
200.0degF	oupre					
60.0degF		-200.6	-201,0	-199.0	PASS	2.1
40.0degF		-60.4	-61.0	-59.0	PASS	3.5
32.0degF		-40.4	-40.5	-39,5	PASS	1.7
1240.0degF		31.6	31.5	32.5	PASS	2.0
1240.0deg#		1239.5	1239.5	1240.5	PASS	1,6
1400.0degF		1259.5	1259.5	1260.5	PASS	1.6
Type Thermoc		1399.5	1399.4	1400.6	PASS	1.8
200.0degF	puble					
50.0deqF		-200.3	-201.0	-199.0	PASS	2.3
10.0degF		-6D,O	-61.0	-59.0	PASS	2.3
12.0degF		-40.1	-40.5	-39.5	PASS	1.2
750.0degP		31.6	31.5	32.5	PASS	1.7
1997 Udegr		749.8	749.5	750.5	PASS	2.0
LIBRATOR CALL	BRATION					
Type Thermoco	aple					
00.0degr		-199.3	~201.0	-199.0	-	
0.0degF		-59.7	-61,0	-199.0	PASS	1.7
0.DdegF		-39,7	-40.5	-39.5	PASS	3.1
2.0degF		32,2	31.5	39.5	PASS	1.5
					£ 494313	±. (
bration Data for Certificate	this					



Rirsh01



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9912, Côte-de-Liesse Tél. (514) 631-6653 Lachine, OC H8T1A1 Fax (514) 631-6122 www.ulrich.ca info@ulrich.ca

	TRUE	TEST	ACCEPTANCE	LIMITS	PASS/	
PARAMETER	VALUE	RESULT	LOW	HIGH	FAIL	TUR
1240.0degF		1239,6	1239.5	1240.5	PASS	1.1
1260.0degF		1259.6	1259.5	1260.5	PASS	1.1
2500.0degP		2499.3	2499.0	2501.0	PASS	1.4
J Type Thermocouple						4 . 4
-200.0degF		-199.9	-201.0	-199.0	PASS	2.1
- 60. OdegF		-60.1	-61,0	-59.0	PASS	3.5
-40.0degF		-39,9	-40,5	-39.5	PASS	1.7
32.0degF		31.9	31.5	32.5	PASS	2.0
1240.0degF		1239.5	1239.5	1240.5	PASS	1.6
1260.0degF		1259.6	1259.5	1260.5	PASS	1.6
1400.0degF		1399.3	1399.4	1400.6	FAIL	1.8
1400.0degF		1399.5	1399.4	1400.6	PASS	1.8
Type Thermocouple						1.0
200, OdegF		-199.8	-201.0	.199.0	PASS	2.3
60.0degF		-60.0	-61,0	-59.0	PASS	2.3
40.0degF		-39.0	-40.5	-39,5	PASS	1,2
32.0degF		31.9	31.5	32.5	PASS	1.7
750.0degP		749.6	749.5	750.5	PASS	2.0

End of Test Data





 4850, bd Gouin est
 Tèl. (514) 328-2550

 Montréal-Nord, Qc
 1800 522-1226

 Canada
 F11 G 1A2
 Fax (514) 327-0604

 www.chevrierinstruments.com
 Info@chevrierinstruments.com

 Indramanis de measure et de régulation pour les procédés indestriels et laboratoire d'étaioneage

## Certificat d'étalonnage

#### Numéro du certificat: CE1640

PJB

4850 GOUIN E MONTREAL, QO	/RIER INSTRUMENTS INC. ST C, CANADA H1G 1A2	Pour : 3424 SBI INC 250, RUE DE COP ST-AUGUSTIN-DE	ENHAGUE -DESMAURES, QC G3A 2H3
Informations si			
Description:	MANOMETRE DIFFERENTIEL ANALOGIQUE		
Manufacturier:	DWYER	Date d'étalonnage	2011-02-10
Modèle:	2000-00	Échéance ;	2012-02-10
Plage	0/0.25 POH2O		
Précision:	±4%P.E.		
Numéro de série	3	Résultat de l'étaion	nage: Conforme
1.D.:	SBI-101	Conditions ambiant	
Etat de l'instrum	ent: BON	Technicien :	Pierre Junior Berlus PITB
Commentaire :			

POINTS D'ÉTALONNAGE	的相关或和自己	
		20 YO M REPORT OF BUILDING TO POSTA

A second states and	Valeur Appliquée	Tolérance -	Lectures	Tolérance +	Verdict
Ascendant	0.0000 poH2O	-0.0100	0		
Ascendant	0.0500 poH20	0.0400	0.045	0.0100	OK
Ascendant	0.1000 poH20	0.0900		0.0600	OK
Ascendant	0.1500 poH2O	and the second se	0.10	0.1100	OK
Ascendant	0.2000 poH2O	0.1400	0.15	0.1600	OK
Ascendant	0.2500 poH20	0.1900	0.20	0.2100	OK
noochdam	and the second	0.2400	0.25	0.2600	OK
CHINE AND	Valeur Appliquée	Tolérance -	Lectures	Tolérance +	Verdict
Descendant	0.2500 poH2O	0.2400	0.25	0.2600	OK
Descendant	0.2000 poH2O	0.1900	0.20	0.2100	
Descendant	0.1500 poH2O	0.1400	0.15	0.1600	OK
Descendant	0.1000 poH2O	and the second			
	0.1000 poH2O 0.0500 poH2O	0.0900	0.10	0.1100	OK
Descendant Descendant Descendant	0.1000 poH2O 0.0500 poH2O 0.0000 poH2O	and the second			

## Certificat d'étalonnage

Numéro du certificat: CE1640

## Étalons utilisés traçable au C.N.R.C / N.I.S.T

	and a series of the second	Echéance
DE PRESSION DH PPC4	2010-03-17	2011-03-17
70		
	ge	5010-02-11

3PR500-01-CHE ÉTALONNAGE DE MANOMÈTRE



 4850, bd Gouin est
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 Canada
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 info@chevrierinstruments.com

 Instruments de missure et de régulation peur les procédés industriels et informations d'étaionnage

## Certificat d'Étalonnage

#### Numéro du certificat: CE509

C.O

AE

C.Q

DC

#### Étaionnage effectué par :

LA CIE J. CHEVRIER INSTRUMENTS INC. 4850 GOUIN EST MONTREAL, QC, CANADA H1G 1A2

#### Informations sur l'instrument

Description.TUBE DE PITOT EN SManufacturierDWYERModèle:160S-24Numéro de sérieI.D.I.D.SBI-203État de l'Instrument:BON

Commentaire :

## Pour : 3424

SBLINC. 250, RUE DE COPENHAGUE ST-AUGUSTIN-DE-DESMAURES, QC G3A 2H3

Dâte d'étalonnage :	2010-12-15
Échéance :	2011-12-15
Résultat de l'étalonn	age: Conforme
Conditions ambiante	s: 21:1 "C / 39 %hr
Technicien	Abdennour Hocini A.H

#### Points d'étalonnage

. atten m admiditten R.			
Valeur Appliquée pi/min	Pitot standard "Ce	Pitot Uut "Ce	ratio
298 pi-min	0.0055 poH2O	0.0074 poH2O	0.86
499 pi-min	0.0154 poH2O	0.0231 poH2O	0.82
802 pi-min	0 0398 poH2O	0.0577 paH2O	0.83
1002 pi-min	0.0622 poH2O	0_0920 poH2O	0.82
2004 pi-min	0.2485 poH2O	0 3614 poH2O	0.83
3008 pi-min	0.5592 poH2O	0.8208 poH2O	0.83
4014 pi-min	0.9940 poH2O	1.4596 poH2O	0.83
5022 pi-min	1.5535 poH2O	2.2827 poH2O	0.82



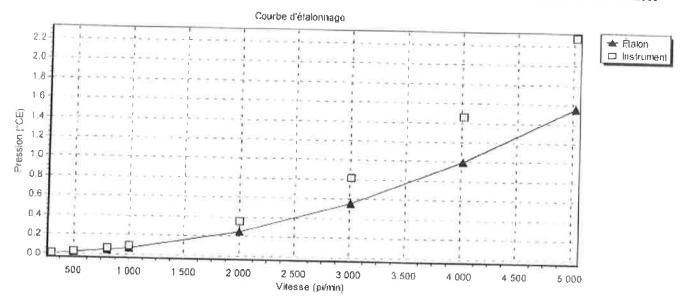
4850, bd Gouin est Montréal-Nord, Qc Canada H1G1A2 www.chevrierinstruments.com info@ Instruments de monera et de régulation sour les precédés indus

Tél. (514) 328-2550 1 800 522-1226 Fax (514) 327-0604 info@chevrierinstruments.com recélés Indusirials et interpolates d'étalements

Instrumente de menera el de régulation pour les procédés industrials et inhormoire d'étaloneage

# Certificat d'Étalonnage

#### Numéro du certificat: CE509



## Fait conformément à l'Échelle International de Température EIT90.

	ulisés traçable au C.N.F	die Frithert		
I.D.	Certificat No	Description	Étalonné le	Échéance
CHEV029	091210-960294	MANOMETRE NUMERIQUE FURMESS PPC500		
CHEV031	CHEV121-100830	TUYÉRE AIRFLOW DEVELOPMENTS	2009-12-16	2010 12-16
			2010-08-30	2011-02-28
Procedure	es utilisées dans cet ét	alonnage		
Procédure			D	
3PR500-2		NNAGE TUBE DE PITOT	Date de	revision

Verdict \star = Point noa conforme

Enregistré par le BNQ selon ISO 8001:2008

## 11/24/2010 SBI-113

## Post test calibration

	Calibration gas	Reading
СО	20.10%	20.14%
CO2	19.80%	19.85%
02	20.90%	20.95%

	Nitrogen	Reading
CO	0.00%	0.00%
CO2	0.00%	0.00%
02	0.00%	0.00%

Date: ID: Appendix E

Sample Calculations

## Equations and Sample Calculations - Method 5G

Equations used to calculate the parameters listed below are described in this appendix. Sample calculations are provided for each equation. The raw data and printout results from a sample run are also provided for comparison to the sample calculations.

- BR Dry burn rate, kg/hr
- m<sub>n</sub> Total particulate matter collected, mg
- $V_{m(std)}$  Volume of gas sampled corrected to standard conditions, dscf
- v<sub>s</sub> Average dilution tunnel gas velocity, ft/sec
- C<sub>s</sub> Particulate concentration, g/dscf
- Q<sub>sd</sub> Average dilution tunnel gas flow rate, dscf/min
- E Particulate emission rate, lbs/hr
- PR Proportional rate variation, %

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## Dry Burn Rate

Using equation 28-3:

$$BR = \frac{60 \times W_{wd}}{\Theta} \times \frac{100 - \% M_{w}}{100}$$

Where,

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\_) T

BR	Ħ	Dry burn rate, 1b/hr
$W_{wd}$	=	Mass of wood burned (wet basis) during tost run, ib
θ	=	Total time of test run, minutes
%M <sub>w</sub>	#	Average moisture content of test fuel charge, wet basis percent

Sample Calculation:

Dry basis moisture of fuel = 20.03%

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Using the equation 28-2 for converting dry basis moisture to wet basis moisture,

$$\%M_{W} = \frac{20.03 \times 100}{20.03 + 100}$$

 $\%M_{\mu} = 16.69\%$ 

The wet weight of the fuel charge was 7.8 pounds. Converting pounds to kilograms yields a weight of 3.538 kg. The run time for this run was 180 minutes. Therefore, the burn rate equation appears thus:

$$BR = \frac{60 \times 3.538 \times (100 - 16.69)}{180 \times 100}$$

$$BR = 0.98 \ kg/hr = 2.17 \ lb/hr$$

## Volume of Gas Sampled Corrected to Dry Standard Conditions

Using equation 5-1:

$$V_{m(std)} = V_m \times Y \times (\frac{T_{std}}{P_{std}}) \times \frac{(P_b + \frac{\Delta H}{13.6})}{T_m}$$

Where:

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 $\bigcirc$  2

K	=	17.64 °R/in. Hg
T <sub>std</sub>	E	528 °R
$\mathbf{P}_{std}$	14	29.92 in. Hg
۷ <sub>m</sub>	=	Volume of gas sample measured at the dry gas meter, dcf
Y	11	Dry gas meter calibration factor, dimensionless
$\mathbf{P}_{b}$	2	Barometric pressure at the testing site, in. Hg
ΔH	11	Average pressure differential across the orifice meter, in, $H_2O$
T <sub>m</sub>	=	Absolute average dry gas meter temperature, °R

Sample Calculation:

$$V_{m(std)} = 98.434 \times 1.01 \times (\frac{528}{29.92}) \times \frac{30.03 + \frac{0.7}{13.6}}{532.5}$$

$$V_{m(std)} = 99.116 \ ft^3$$

## Dilution Tunnel Gas Velocity

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Using equations 2-7 and 2-6, calculated at each recorded interval:

		$v_s = k_p \times C_p \times \sqrt{\Delta P} \times \sqrt{\frac{T_{s(avg)}}{P_s \times M_s}}$ $M_s = M_d \times (1 - B_{vs}) + 18.0 \times B_{vs}$
Where:		
Vs	-	Average dilution tunnel gas velocity, fl/sec
k <sub>p</sub>		Pitot tube constant: $85.49 \frac{ft}{sec} \left[ \frac{(lb/lb-mole) \times (inches Hg)}{(^{\circ}R) \times (inches H_2O)} \right]^{\frac{1}{2}}$
$C_p$	3	Pitot tube coefficient (0.99 for standard pitot tube; 0.84 may be used for
		S-type pitot tubes constructed according to Method 2 procedures), unitless
Δp		$\Delta P$ measured during the pre-test flow traverse of the dilution tunnel; the
		square root of the $\Delta P$ values are averaged for this calculation, in. $H_2O$
$\mathbf{P}_{\mathbf{b}}$	=	Barometric pressure at test site, in. Hg
$P_{g}$	-	Static Pressure of tunnel, in. Hg
$\mathbb{P}_{s}$	Ħ	Absolute tunnel pressure, = $P_b + P_g$

t

 $M_s = Molecular$  weight of tunnel gas; assume  $M_d = 29$  lb/lb-mole (per method 5G)

B<sub>ws</sub> = Moisture content of dilution tunnel gas, ratio; assume 4% (per method 50)

 $T_s$  = Dilution tunnel temperature, °R; (°R = °F + 460)

Sample calculation:

$$M_s = 29 \times (1 - 0.04) + 18.0 \times 0.04 = 28.56$$

$$v_s = 85.49 \times 0.99 \times \sqrt{0.0351} \times \sqrt{\frac{(548)}{(30.03 + \frac{-0.45}{13.6})} \times (28.56)}$$
  
 $v_s = 12.69 \frac{ft}{sec}$ 

## Particulate Concentration

Using equation 5G-2:

$$C_s = 0.001 \frac{g}{mg} \times \frac{m_n}{V_{m(s(d))}}$$

Where:

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C<sub>s</sub> Concentration of particulate matter in stack gas, dry basis, corrected to standard conditions, g/dscf

 $m_n = Total mass of particulate matter collected in the sampling train, mg <math>V_{m(stb)} = V$ olume of gas sampled corrected to dry standard conditions, dscf

Sample calculation:

$$C_s = \frac{0.001 \times 16.2}{99.116}$$

 $C_{s} = 0.000163 \ g/dscf$ 

## Average Dilution Tunnel Gas Flow Rate

Using equation 2-8, calculated at each recorded interval:

$$Q_{sd} = 3600 \times (1 - B_{ws}) \times v_s \times A \times \frac{T_{std}}{T_{s(avg)}} \times \frac{P_s}{P_{std}}$$

Where:

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$Q_{sd}$	1:2	Gas flow rate corrected to dry, standard conditions, dscf/hr
3600	Π	Conversion from seconds to hours
$\mathbf{B}_{ws}$	=	Moisture content of dilution tunnel gas, ratio; assume 4% (per method 5G)
$V_{\mathfrak{g}}$	=	Average dilution tunnel gas velocity, ft/sec
А	8	Cross sectional area of dilution tunnel, ft <sup>2</sup>
$\mathbf{T}_{\mathrm{std}}$	1	Standard absolute temperature, 538°R
$T_{s(avg)}$	11	Average absolute dilution tunnel temperature, °R, (°R = °F + 460)
P <sub>b</sub>	12	Barometric pressure at test site, in. Hg
P <sub>g</sub>	п	Dilution tunnel static pressure, in. Hg
P,	-	Absolute dilution tunnel gas pressure, in Hg, $(Hg = P_b + P_g)$
$\mathbf{P}_{\mathrm{std}}$	=	Standard absolute pressure, 29.92 in Hg

Sample calculation:

 $Q_{sd} = 3600 \times (1 - 0.04) \times 12.69 \times \frac{(\pi \times 3^2)}{144} \times \frac{528}{548} \times \frac{30.03 + \frac{-0.45}{13.6}}{29.92}$ 

 $Q_{sd}$  = 8313.36 dscflhr = 138.56 dscflmin

#### Particulate Emission Rate

Using equation 5G-3 and 5G-4:

$$E = C_s \times Q_{sd}$$

$$E_{adj} = K_3 \times E^{0.83}$$

Where:

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Ε	=	Particulate emission rate, g/hr
$\mathbf{E}_{\text{adj}}$	=	Particulate emission rate, adjusted, g/hr
$C_s$	1	Concentration of particulate matter in the stack, corrected to dry, standard
	condit	ions, g/dscf

 $K_3 = Constant, 1.82$  for metric units, 0.643 for English units

Sample calculation:

 $E = 0.000163 \times 8313.36$ 

 $E = 1.36 \, g/hr$ 

 $E_{adj} = 1.82 \times 1.36^{0.83}$ 

 $E = 2.35 \, g/hr$ 

# **Proportional Rate Variation**

Using equation 5H-9, calculated at each recorded interval:

$$PR = \frac{\theta \times (V_{mf} \times V_s \times T_m \times T_{sf})}{10 \times (V_m \times V_{sf} \times T_s \times T_m)} \times 100$$

Where:

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PR	=	Percent proportional rate
θ	=	Time of test, min
$\mathbf{S}_{\mathbf{I}}$	Ĩ	Measured tracer gas concentration for the "ite" interval, in this case, the
		inverse of the calculated flow in the stack based on CO <sub>2</sub> concentrations in
		the stack and in the dilution tunnel
V <sub>ml(std)</sub>	) =	Volume of gas sample measured by the dry gas meter during the "ith" 10
		minute interval, dscf
V <sub>m</sub>		Volume of gas sample as measured by dry gas meter, dscf
$V_{\rm sf}$		Average gas velocity in the dilution tunnel during each 10 minute interval, i,
		of the test run, m/sec
V,	==	Average gas velocity in the dilution tunnel, m/sec
T <sub>mi</sub>	-	Absolute average dry gas meter temperature during each 10 minute interval, i,
		of the test run, °R
T <sub>m</sub>	=	Absolute average dry gas meter temperature, °R
T <sub>st</sub>	=	Absolute average gas temperature in the dilution tunnel during each 10
		minute interval, i, of the test run, °R
T,	#	Absolute average gas temperature in the dilution tunnel, °R

Sample calculation (for the reading at 50 minutes into test run 1):

 $PR = \frac{180 \times 5.6 \times 12.69 \times 533 \times 552}{10 \times 98.434 \times 12.63 \times 548 \times 532} \times 100$ 

PR = 103.8%

Appendix F

Test Data

#### **EPA NSPS WEIGHTED AVERAGE CALCULATION** V 1.1

Sort data from lowest to highest burn rate and enter below.

Type of Stove: Weighted Average 1=cat 2=noncat 3=pellet

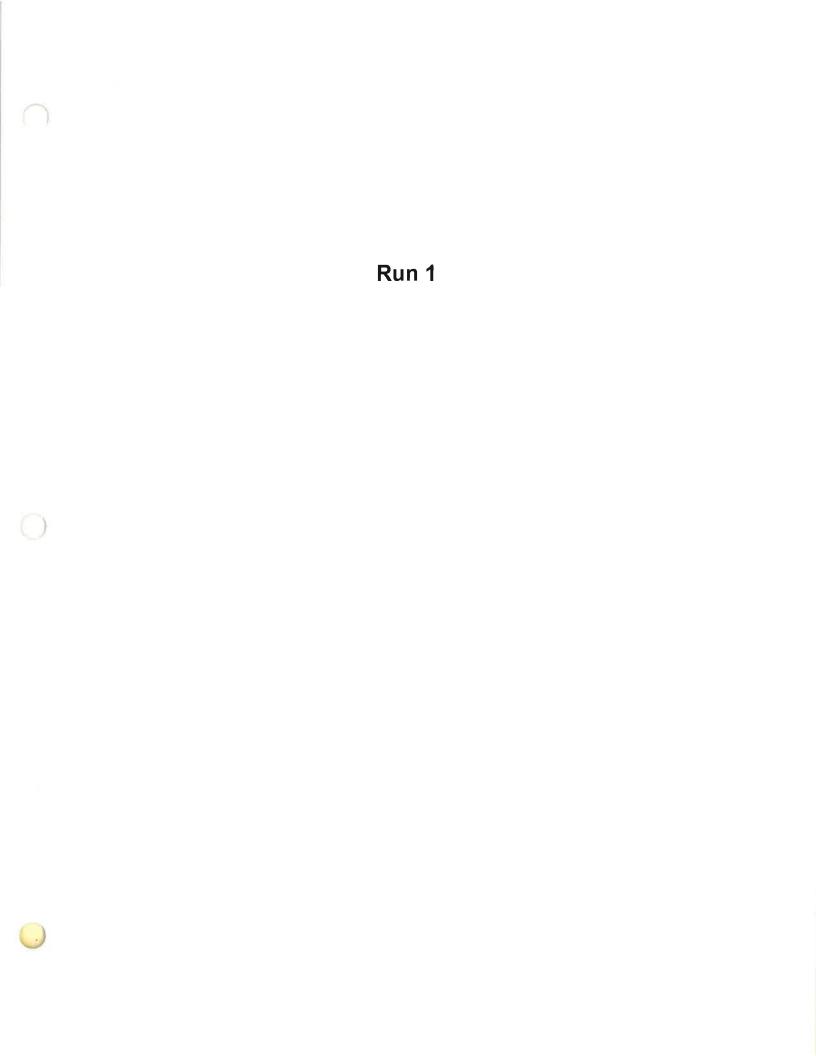
2

		(E)						
		Ave.		Heat		(K)		
Test	Burn	Emission		Output		Weighting		
No.	Rate	Rate g/hr	(OHE)	(BTU/HR)	Prob.	Factor	(KxE)	KxOHE
1	0.96	4.82		11575.87	0.3384	0.4494	2.1661	0.00
2	1.09	4.07		13143.44	0.4494	0.5422	2.2068	0.00
3	1.84	3.15		22187.09	0.8806	0.5264	1.6582	0.00
5	2.67	2.87		32195.39	0.9758	0.1194	0.3427	0.00
				0.00	1.0000	0.0000	0.0000	0.00
				0.00	1.0000	0.0000	0.0000	0.00
				0.00	1.0000	0.0000	0.0000	0.00
				0.00	1.0000	0.0000	0.0000	0.00
				0.00	1.0000	0.0000	0.0000	0.00
						0.0000	0.0000	0.00

Totals: 1.6374 6.3737 0.00

Weighted average emissions rate:	3.8926
Weighted Average OHE:	0.00

03/20/2012





( )

#### Run Notes EPA Methods 28 and 5G-3

PROJECT / TES	T INFORMATION		Appliance Info	ormation
Project Number:	G100456088			1 - Catalytic
Manufacturer:	SBI	Appliance	e 2	2 - Non - Catalytic
Model:	XTD 1.9	Type:	-	3 - Pellet
Sample ID Number:	MTL1108221414-001			4 - Hydronic
Test Date:	22-Aug-11	SBI Nation XTD 11 RUN+1 22/08/2011 ft <sup>3</sup> :	2.14	N/A for pellet type
Test Run Number:	1	Convection	on	1 - No Fan
Date tunnel cleaned:	8/18/2011	Blower	1 2	2 - Fan Optional
Purpose of Test	Cat 1	Blower		3 - Fan Standard
		Contraction of the second		

Contraction of the local distance

		Test Settings	
	Primary Air:	Fully closed	
Sec	condary Air:	Fixed	
Co	ntrol Board:	N/A	
1	Blower/Fan:	Off the first 30 minutes and turned On-Low after 30 minutes for the reminder of the test	
		Pre- Burn Activities	
Time	Activity		
(min.)	Closed the	primary air when the scale indicated 8.00 pounds	
45	Stirred the	Coad Bed	
100	Leveled the	e Coal Bed for 50 seconds	
	-	Start-Up Procedure	
oading of	f fuel. sec. :	Start-Up Procedure	
-		Loaded by 50 seconds	
Fuel-loa	ading door :		
Fuel-loa	ading door :	Loaded by 50 seconds Left ajar for 90 seconds Fully open the first 5 minutes. Abruptly closed at 5 minutes.	
Fuel-loa Sec	ading door : Primary air:	Loaded by 50 seconds Left ajar for 90 seconds Fully open the first 5 minutes. Abruptly closed at 5 minutes. Fixed	
Fuel-loa Sea Co	ading door : Primary air: condary air: ntrol board:	Loaded by 50 seconds Left ajar for 90 seconds Fully open the first 5 minutes. Abruptly closed at 5 minutes. Fixed	
Fuel-loa Sea Co	ading door : Primary air: condary air: ntrol board:	Loaded by 50 seconds Left ajar for 90 seconds Fully open the first 5 minutes, Abruptly closed at 5 minutes. Fixed N/A	

- Hugher 03/26/12

				VERSION 1.	2	2/5/2010			1			
Manufacturer:	SBI	1										
Model:	XTD 1.9											
Date	22-08-2011											
	1	· · · · · · · · · · · · · · · · · · ·										
	G100456088	Para										
Test Duration:		i										
Test Duration.	330	Start	End									
	Barometer (in.Hg):	29.54	29.5	1							1	
	barometer (mang).	20.04	20.0									
	Dry Bulb (F):	82	82	· · · · · · · · · · · · · · · · · · ·								
		24	22									
	Humidity (%):	24	22	·								
Blower turned on at 30 min - lo												
	THE REPORT OF A DESCRIPTION OF A DESCRIP	40.5700							-			
Moisture content of				10.00	000 75	04.00	00.00	000.40	440.00	000.00	400.00	329
	Average	1.32	4.51	15.77	222.75	84.38	99.08	388.10	410 33	386.36	420.06	329
2	141-1-64		τ.		<b>5</b> 1	Deces	Tunnel	Unit	Unit	Unit	Unit	Unit
Elapsed	Weight	00	001	03	Flue	Room	Tunnel Dev Bullo	Unit	Back	R.Side	L.Side	Botto
Time	Remaining	CO	CO2	02 19.07	Gas 264.06	Temp 81.68	Dry Bulb 110,11	Top 376.03	488.82	433.31	474.67	408
		0.65	1.97							398.73	474.07	406
10		0.69	3.42		236,03	92.63	97,66	382.31	464_11			
20		0.95	4.07		224.55	84.40	98,69	360 97	429.37	363.69	423.05 407.93	397 382
30		0.72	9.12		226,30	83,92	98.04	368,27	402.09	351.77		
40		0.70	10.32		267.51	80,80	101.06	434.50	399.52	347.01	398.85	360
50		0.57	9,83		305 72	89.53	105,04	533.45	418.80	362 82	412.32	343
60	8.47	0.88	10.69		323,50	83.53	111,34	583.70	277.12	379.99	434_74	331
70		0.96	8.75		331.86	92.24	108.67	612.47	297.39	399.68	453.81	324
80	6.21	0.98	8.27		313 43	89.68	109,75	592.06	314_81	419_83	474.81	321
90	5.27	0.81	8.12	11.94	302.83	84 39	112 11	558,89	328.00	438.22	486.06	318
100	4.45	0.60	7.18	13.47	293.92	83.12	110.60	542 25	339 29	447 21	492 56	316
110	3,80	1.03	5,57	14.85	276,99	82.31	109 10	522.92	359.76	451:31	499.55	316
120	3.35	0.97	5.46	14.32	251.45	82,90	105,75	485.10	408 81	455.39	496 10	316
130	2.91	1.11	4.62	15.2B	244 29	81,50	105,15	455.33	506 74	458 82	487.86	317
140	2.62	1.00	4.58	15.58	230.41	79.22	102.78	434 16	528 58	461.66	482.36	317
150	2.42	1.27	4.15	15.83	220 39	79.40	101,75	410,23	514.94	449 20	475.50	318
160	2.22	1.51	3.31	16 72	214.12	78.46	100.32	390,84	505.08	431.31	466 23	318
170	2.07	1.67	3.40	16.51	209,55	77 71	99.01	372.79	494 16	412.28	456 24	320
180	1.92	1.52	3.12	16.72	201.83	85.81	96.15	357.47	480.73	393.25	443_24	321
190	1.73	1.81	3,03	16.66	196 09	86.15	96,63	344.24	467.38	380,69	430.71	322
200	1.55	1.87	2.96		191.56	84.50	95.60	332.62	453.95	375 73	418.53	323
210	1.41	2,27	2.51	17-16	167.99	83.42	95.18	324.72	442.70	364 12	408_40	322
220	1.29	1.76	2.81	17.37	185,14	84.16	93,30	316,35	432.57	358.93	400.20	321
230	1.18	1.85	2.72		182.43	86.36	93,37	309.29	421.99	356.56	391.25	320
240	1.04	2.02	2.48		179.70	85.18	92.97	304.02	410.81	347.66	384 62	318
250	0.90	1.88	2.59		178.06	84.52	92.55	299.06	401 65	341.23	378.63	316
260	0.75	1.98	2.03		175.76	84.96	92.49	292.58	395 71	336.78	370.42	314
270	0.62	1.81	2.16		172 57	82.91	92,08	286.65	390.07	335.34	361.37	312
280	0.48	1.67	2.10		169.44	82.71	92,15	279.59	381 27	341 17	352 29	312
280	0.38	1.34	2.89		166.11	87.51	90,06	273.75	372.08	346.71	344.31	312
			2.89		163,92	88.72	88.31	268.25	363 55	352.94	344.51	312
300	0.25	1.41							357.81	355 02	332 93	312
310	0.16	1.46	2.06		163.46	86 84	89.79	266.89			332 93	310
320	0.06	1.41	2.18		162.04	86.03	90.49	263 78	353 50	347-14		
330	0.00	1.60	1.94	18.19	160.34	81.61	90.61	259.95	347.98	340.87	323.06	307

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- Hughel 03/26/12

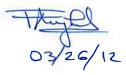


	da al con	001											
Manu	facturer:			1									_
		XTD 1.9										+++++++++++++++++++++++++++++++++++++++	
	ALC: NAME OF TAXABLE PARTY.	22-08-20	)11						į				
	Run:		E										
C	Control #:	G100456	6088									li	
												i	
3		1								111		h	
348.76	79.54	79.51	81.82	388,01	79,58	79.50	82.74	0.02	0.000	0.00	<ul> <li>Providencial and Algorithm</li> </ul>		
	9.81	in the second								Visual	A real of the second	Change in	- <u>k</u>
DGM 1	DGM 1	DGM 1	Filter 1	DGM 2	DGM 2	DGM 2	Filter 2		Chimney	Smoke	Stove	Surface	Elapsed
Reading	Inlet T	Outlet T	Temp	Reading	Inlet T	Outlet T	Temp	Velocity	Draft	Observed	Temp	Temp.	Tim
333,439	78.26	78.19	79.42		78.26	78.12	79.09	0.021			436.2 420.8	-15.402	10
334.379 335,300	78.40	78.32	81.00		78.34	78,24	81.09	0.021			394.8	-41.34	20
336,232	78.44	78.38	81.23 81.22	372.745 373.812	78.40	78.31	81.57	0.021	111-0		382.6	-53.591	30
337,163	78.59 78.79	78.48 78.65	81.44	373.812	78.49 78.65	78.44 78.65	81.92 82.22	0.021			388.1	-48.102	4(
338.090	78.75	78.55	81.59	375.958	78.05	78.65	82.40	0.021			414.2	-21.978	50
339.012	78.83	78.76	81.85		78.78	78,08	82.99	0.021			401.4	-34.768	60
339.938	79.05	78.90	82.41	378.038	78.95	78.91	83.78	0.021			417.5	-18.699	70
340.866	79.11	79.00	82.42	379.064	79.05	78.99	83.96	0.021			424.6	-11.593	80
341.792	79.29	79.15	82.83		79.20	79.16	84.40	0.021			425.9	-10.285	90
342.726	79.39	79.24	82.95		79.31	79.27	84.52	0.021			427.6	-8.5597	100
343.657	79.51	79,35	82.95	382.265	79.42	79.38	84.57	0.021			430.0	-6.1501	110
344.580	79.51	79.37	82.85	383.313	79.51	79.40	84.38	0.021			432.5	-3.7093	120
345.513	79.55	79,44	82.73	384,363	79,56	79.43	84.19	0.021			445.1	8.9736	130
346.441	79.58	79.46	82.56	385,406	79,59	79.47	84.04	0.021			444.9	8.7391	140
347.382	79.66	79.55	82.43	386.468	79.68	79.55	83.80	0.021	¢111		433.7	-2.4874	150
348.305	79.65	79.57	82.30	387.495	79.69	79.57	83.51	0.021			422.5	-13.719	160
349.232	79.69	79,61	82.21	388,549	79.72	79.61	83.24	0.021			411.1	-25.078	170
350.261	79. <b>72</b>	79.70	82.12	389,695	79.81	79.70	83.10	0.021			399.3	-36.919	180
351.088	79.64	79.70	82.09	390.842	79.82	79.68	82.96	0.021			389.2	-47	190
352.011	79.76	79.80	81.92	391.694	79.86	79,79	82.78	0.021			380.9	-55.314	200
352.928	79,80	79.84	81.79	392.736	79.91	79.82	82.63	0.021			372.5	-63.626	210
353.843	79.89	79,91	81.63	393,788	80.01	79.97	82.44	0.021			365.9	-70.237	220
354.768	79.93	79.98	81.46	394.824	80.05	80,01	82.33	0.021			359.9	-76.247	230
355,698	79.97	80.04	81.60	395.862	80.07	80.03	82.38	0.021			353.2	-83.007	240
356.615	79.97	80.06	81.55	396,909	80.07	80.00	82.46	0.021			347.5	-88.682	250
357,549	80,04	80.12	81.70	397.945	80.14	80,08	82.51	0.021				-94.113	260
358,495	80.04	80.14	81.61	398.990	80.16	80,09	82.37	0.021			337.3	-98.913	270
359.422	80.19	80.25	81.49	400.035	80.31	80.28	82.19	0.021			333.3	-102.89	280
360.359	80.24	80,30	81.57	401.070	80,39	80,33	82.21	0.021			329.8	-106.36	290
361.381	80.21	80.29	81.23	402.118	80.41	80.28	81.84	0.021			327.1	-109.05	300
362.224	80.27	80.35	81.21		80,46	80,32	81.79	0.021				-111.45	310
363,160	80,28	80,33	81.22		80,49	80,35	81.80	0.021			320.7	-115.46	320
364.104	80,33	80.35	81.28	405.238	80.46	80,34	81.82	0.021			315.8	-120.33 -120	.33 330

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	Manu	facturer:		SBI				
		Model:		XTD 1.9				
		Date:		22-08-2011				
		Run:		1				
	Projec	1#:	1 1 1 1 1	G100456088				
	Test Dura	· · · · · · · · · · · · · · · · · · ·		330			(	
Total Gas \				29.595	Pit	ot Factor	0.82	
	Total Gas Volume (DGM 2):			33.068			0.99 standar	
Average Barometric Pressure:			1	29.52			al. Factor fo	
		lar Weig	ht:	28.56				
		orrection		0.9151				
Calibration Fa				1.0000				
Calibration Fa				0.9960			P+	
	ALL		(1) VS:	0.0276				
			(2) VS:	0.0247			Filter	Filter
			A. A. 1973				Face	Face
DGM 1	DGM 1	DGM 1	DGM 2	DGM 2	DGM 2	Tunnel	Velocity	Velocity
Reading	Inlet T	Outlet T	Reading	Inlet T		Dry Bulb	DGM 1	DGM 2
333.439	78.3		370.835	78.3	78.1	110.1		
334.379	78.4	78.3	371.795	78.3	78.2	97.7	7.84	7.9
335.300	78.4	78.4	372.745	78.4	78.3	98.7	7.68	7.8
336.232	78.6	78.5	373.812	78.5	78.4	98.0	7.77	8.86
337.163	78.8	78.6	374.925	78.7	78.7	101.1	7.76	9.24
338.090	78.8	78.7	375.958	78.7	78.7	105.0	7.72	8.57
339.012	78.8	78.8	376.962	78.8	78.8	111.3	7.68	8.3
339.938	79.0	78.9	378.038	79.0	78.9	108.7	7.71	8.93
340.866	79.1	79.0	379.064	79.1	79.0		7.73	8.5
341.792	79.3	79.2	380.131	79.2	79.2	112.1	7.71	8.8
342.726	79.4		381.218	79.3	79.3	110.6	7.77	9.0
343.657	79.5	79.3	382.265	79.4	79.4	109.1	7.75	8.68
344.580	79.5	79.4	383.313	79.5	79.4	105.8	7.68	8.69
345.513	79.5	79.4	384.363	79.6	79.4	105.2	7.76	8.70
346.441	79.6		385.406	79.6	79.5	102.8	7.72	8.64
347.382	79.7		386.468	79.7	79.6	101.7	7.83	8.80
348.305	79.6		387.495	79.7	79.6	100.3	7.68	8.5
349.232	79.7		388.549	79.7	79.6	99.0	7.71	8.73
350.261	79.7	79.7	389.695	79.8	79.7	96.1	8.56	9.49
351.088	79.6	79.7		79.8	79.7	96.6	6.88	7.84
352.011	79.8		391.694	79.9	79.8	95.6	7.68	8.7
352.926	79.8		392.736	79.9	79.8	and the second second second second	7.61	8.6
353.843	79.9		393.788	80.0	80.0	93.3	7.62	8.7
354.768	79.9	80.0	394.824	80.0	80.0	93.4	7.69	8.58
355.698	80.0		395.862	80.1	80.0	93.0	7.73	8.59
356.615	80.0		396.909	80.1	80.0	92.6	7.62	8.67
357.549	80.0	80.1	397.945	80.1	80.1	92.5	7.76	8.58
358.495	80.0	1	398.990	80.2	80.1	92.1	7.86	8.6
359.422	80.2		400.035	80.3	80.3	92.2	7.70	8.6
360.359	80.2	1.000000000	401.070	80.4	80.3	90.1	7.79	8.56
361.381	80.2		402.118	80.4	80.3		8.49	8.6
362.224	80.3		403.153	80.5	80.3		7.00	8.56
363,160	80.3		404.191	80.5	80.3		7.78	8.59
364.104	80.3	CONTRACTOR NO.	405.238	80.5	80.3		7.84	8.66

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Thyll 03/26/12

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1 1 1 4 4 4 1 1 1 1 1 1 1	Stack are	ea (ft2):	0.3491		Mar	ufacturer:	SBI			
Wood	moisture		16.579				XTD 1.9	1		
	Veight (lb		13.95			Date:	22-08-2011			
	tate (Dry I		0.960			Run:				
- inal Ter	mperature	e (DGM #1	) Degree	s Rankin	539.524					
		(DGM #2			539.540					
		nperature			559.078					
		ocity (feet			7.623023					
		d Tunnel f			142.76					
		Average	Average							
	eh mimihm	Inlet +	Inlet +							
		Outlet	Outlet	99,96	99,97	#1	#2			
Tunnel	Tunnel	Temp.	Temp.	00,00	00,01	dDGM	dDGM			
Velocity	5	Meter 1	Meter 2			Vol.Std.	Vol.Std.			
Delta-P	F1/Sec	Deg. R	Deg. R	PR1	PR2	(ft3)	(ft3)	Time		
0.021	7.698	538.2	538.2					0		
0.021	7.614	538.4	538.3	101.25	92.19	0.909	0.925	10		
0.021	7.621	538.4	538.4	99.29	91.30	0.891	0.915	20		
0.021	7.616	538.5	538.5	100.39	102.46	0.901	1.028	30		
0.021	7.637	538.7	538.7	100.52	107.13	0.900	1.072	40		
0.021	7.664	538.7	538.7	100.44	99.78	0.896	0.995	50		
0.021	7.706	538.8	538.8	100.44	97.50	0.891	0.967	60		
0.021	7.688	539.0	538.9	100.61	104.22	0.895	1.036	70		
0.021	7.696	539.1	539.0	100.91	99.45	0.896	0.987	80		
0.021	7.712	539.2	539.2	100.87	103.61	0.894	1.026	90		
0.021	7.701	539.3	539.3	101.59	105.39	0.902	1.045	100		
0.021	7.691	539.4	539.4	101.11	101.36	0.899	1.007	110		
0.021	7.669	539.4	539.5	99.94	101.15	0.891	1.008	120		
0.021	7.664	539.5	539.5	100.96	101.28	0.901	1.009	130		
0.021	7.648	539.5	539.5	100.20	100.38	0.896	1.003	140		
0.021	7.641	539.6	539.6	101.50	102.10	0.908	1.021	150		
0.021	7.632	539.6	539.6	99.43	98.61	0.891	0.987	160		
0.021	7.623	539.7	539.7	99.73	101.08	0.895	1.013	170		
0.021	7.603	539.7	539.8	110.41	109.60	0.993	1.101	180		
0.021	7.606	539.7	539.8	88.78	90.61	0.798	0.910	190		
0.021	7.599	539.8	539.8	98.98	100.55	0.890	1.011	200		
0.021	7.597	539.8	539.9	98.07	99.55	0.883	1.001	210		
0.021	7.584	539.9	540.0	98.11	100.31	0.884	1.010	220		
0.021	7.584	540.0	540.0	98.96	98.78	0.892	0.995	230		
0.021	7.581	540.0	540.0 540.0	99.45	98.93	0.897	0.997	240 250		
0.021		540.0		98.02	99.76	0.884	0.995			
0.021	7.578	540.1	540.1	99.82	98.69	0.901		260 270		
0.021	7.575	540.1	540.1	101.06	99.51 99.48	0.912	1.003	280		
0.021	7.576	540.2	540.3 540.4	99.02	99.48 98.33	0.894		280		
0.021	7.561	540.3	540.4	99.89	98.33	0.903	0.993	300		
0.021	7.549	540.3		108.78	99.41	0.985	0.993	310		
0.021	7.560	540.3 540.3	540.4 540.4	89.84 99.81	98.64	0.902	0.993	320		
0.021	7.565	540.3	540.4	100.67	98.64 99.51	0.902	1.005	320		

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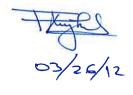
- Hypel 03/26/12

		Intertek Testing Service	es					
		SFBA EPA ADJUSTED	EMISSION	RESULT	s			
	100000000	of DALLA ADJOUTED	Linicolory	INE OUL I	Č			
Manufacturer		SBI				RESULT	S	
	Model:	XTD 1.9						
1	Date:	22-08-2011		P	verage Ad	justed Emis	sions Rate:	4.8
	Run:	1		A	verage Una	adjusted Em	ission Rate	3.2
	Project #:	G100456088				Burn Rate	(Dry kg/hr):	0.9
Test Duration		330						
Test Duration	n (Hours):	5.50						
1				BARO	METRIC	PRESSU	RE	
							Average:	29.5
TEMPERA	ATURE FAC						Start:	29.5
4		DGM #1:	0.9786				End:	29
		DGM #2:	0.9786			1		
				DRY GA	S METER		i	
VOLUM	ES SAMP	exercise and a service of the set				DGM #1		364.10
	F	DGM #1:	29.609				Initial:	333.43
		DGM #2:	33.084			DGM #2	Final	105.0
TOTAL		VOLUME (scf):	47110				Final: Initial:	405.23
TOTAL	IONNEL	VOLUME (SCI).	47110				n nuar.	3/0.0.
SAMPLE	RATIOS			TEMP	FRATUR	ES (DEG	RANKIN	)
	the stand of side process where	e Train 1:	1591.1				DGM #1:	539.52
		e Train 2:	1423.9				DGM #2:	539.54
		R INSTRUCTION	Linter Procession					
TOTAL	EMISSION	NS		CALIB	RATION	FACTOR	S	
San	ple Train	1 (g):	18.62			1	DGM #1:	1.00
San	ple Train	2 (g):	16.94				DGM #2:	0.99
		Ave:	17.78					
the last state of the second state of the	ON RATES			TUNN	AT THE REPORT OF A PARTY	V RATE:		142.8
	le Train 1		3.38		PART		CATCH (	mg)
Samp	le Train 2	A DATE OF A DOMESTIC AND A DOMESTIC ADDRESS OF A DOMESTICA ADDRESS OF ADDRE	3.08			/ / / = ===== + + + + + + + + + + + + +	e Train 1:	
		Ave:	3.23				Filters	11
		SION RATES					Probe	0
	le Train 1		5.01			and the second second second	Total	11
Samp	le Train 2	ADDU & WHEN WAR AND ADDU ADDU ADDU ADDU ADDU ADDU ADDU	4.63			Sample	Train 2:	-
	DE	Ave: /IATION:	4.82				Filters Probe	1 0.
	DEV		3.90%				Total	11.
الحمام الم	on in arrest	ter than 7.5% due to lov	u porticulata	oatab				
		rates shall not differ by		catch			110-0-0	
		erage emission rate lim		) (5g-3)				
Use the	following:							
ove the								
Catalytic			9.17%					
7.5% of								
Non cata	lytic units		5.01%					
	7.5 g/hr						(*************************************	

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	Before 82	After 82	Before 29.54	After 29.50	Before 24	After 22	Before	After
		Temp	Bar Pressure		Relative H		Air Velo	
						1		
	Water C							
		DGM 2:	79.54				[]	
		DGM 1:	79.52				[ · · · · · ]	
		nnel:	99.08					
	Filte	And the second shifts a	82.74					
	Filte		81.82		1			
		alion:	3.90%					
		em 2:	4.631		fan se			
Aujuste		em 1:	5.007					
Adjusto	d Emissio	the first state of the second state of the sec	4.819		-			
	Burn F	lator	0,960				1	
					1			
Chang	e in stov	e temp:	-120.3276534		1		1	
							[]	
Ave	age Roo	m Temp:	84.38				1	
		meter:	29.52					
Stack	Stack Static (neg):		-0.0925		1			
	Moisture (		19.87333333					
		Model:	XTD 1.9		[		1	
		Project:	G100456088					
		Date:	22-08-2011					
		Run:	1					
		Client:	SBI					
	REPORT	DATA			3			

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77-5/12 03/26/12

Manufacturer: SBI Model XTD 1.9 Project G100456088

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- t	roject G IU	1400000							c
	Flue	Room	Tunnel	Unit	Unit	Unit	Unit	Unit	Scale
	Gas	Temp	Dry Bulb	Тор	Back	R.Side	L.Side	Bottom	weight
	609.46	85.92	174.76	688.52	456.68	589.43	565.00	469.30	10.28
	408.59	86.69	134.54	725.69	427.78	590.33	583.80	477.08	8.21
	358.29	85.57	122.60	634.08	438.83	556.52	574.42	474.02	7.03
	349.50	85.88	118.39	640.54	435.22	544.92	572.45	462.07	5.80
	353.02	86.41	4170.61	665.84	562.98	533.03	581.82	450.51	4.45
	300.31	85.93	115.50	613.82	462.44	533.08	581.70	435.28	3.84
	278.02	84.96	112.68	541.96	538.80	517.69	564.85	428.07	3.50
	249.51	83.73	107.79	479.79	456.58	483.90	538.29	423.05	3.33
	236.55	83.28	105.03	436.09	519.03	463.18	514.35	417.99	3.16
	224.35	80.10	100.76	408.85	514.06	445.53	495.61	415.07	3.00
	216.43	79.39	99.26	389.31	495.91	428.23	480.52	410.20	2.81

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1/26/12

VERSION 1.2

2/5/2010

### E&E Tunnel Traverse Worksheet

		TUNNEL	SQUARE
	VELOCITY	TEMP	ROOT
A CENTER	0.023	119	0.1500
<b>B CENTER</b>	0.020	118	0.1414
A1	0.018	117	0.1323
A2	0.020	118	0.1414
A3	0.018	118	0.1323
A4	0.018	108	0.1323
B1	0.018	118	0.1323
B2	0.020	119	0.1414
B3	0.018	119	0.1323
B4	0.015	113	0.1225
AVERAGE	0.0185	116.86	0.1333

Static Pressure:

PITOT CONSTANT 0.9151

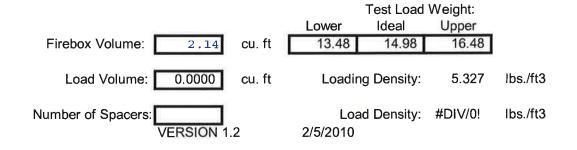
Tunnel Diameter (in): Tunnel Area (ft2) Tunnel Static Pressure 8 0.349066 0.0925

03/26/12

120

120

### **E&E FUEL LOAD DATA SHEET**



		Piece S	ize:		Weight	М	Meter Moisture Conte			
Thick	Х	Wide	Х	Length	lbs		Dry Uncorrect			
	2		4	12	1.2	20.4	19	19		
	2		4	12	1.3	20	19.7	21		
	2		4	12	1.1	20.5	20.1	21		
	2		4	12	1.2	21.2	21	21.4		
	2		4	16	1.55	21	20.5	21		
	2		4	16	1.75	19.00	19.50	20.90		
	2		4	16	1.70	20.50	21.20	20.90		
	2		4	16	1.60	20.10	19.90	19.90		
	I		I							

Test Load Weig	<b>h</b> 11.40 lbs.	Dry We	igh 4.28	8 kg.
Dry: 20.21	Average Pretest M two pin: (dry)		<b>nt: %</b> Wet:	17.29

03/26/12



VERSION 1.2

2/5/2010

## **E&E FUEL LOAD DATA SHEET**

		Test Load V	Neight:	
		Lower Ideal	Upper	
Firebox Volume: 2.14	cu. ft	13.48 14.98	16.48	
Load Volume: 0.0651	cu. ft	Loading Density:	6.519	lbs./ft3
Number of Spacers: 20		Load Density:	214.272	lbs./ft3

	Piece Size:		Weight	Meter Moisture Content			
Thick x	Wide x	Length	lbs	Dry Uncorrected %			
2	4	15.75	2.10	21.40	21.40	21.10	
2	4	15.75	1.85	19.50	19.80	19.70	
2	4	15.75	1.75	19.90	19.70	19.00	
4	4	15.75	4.10	19.50	18.90	19.50	
4	4	15.75	4.15	20.00	19.20	19.50	

Test Load Weigh 13.95 Ibs.	Dry Weig	h 5.28	kg.
Average Moist	ure Content: %	Wet:	16.58
Pre-test moist	ure content: %	Wet:	16.81
Coal Bed Range: 2.8 Ibs.	to 3.4 lbs.	20% to 25%	of test load
- Jagt 03/20	es estr		

Run 2

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#### Run Notes EPA Methods 28 and 5G-3

PROJECT / TES	T INFORMATION		Appl	iance	Information
Project Number:	G100456088				1 - Catalytic
Manufacturer:	SBI		Appliance	2	2 - Non - Catalytic
	XTD 1.9		Туре:	-	3 - Pellet
Sample ID Number:	MTL1108221414-001	CO.			4 - Hydronic
Test Date:	23-Aug-11	SBI NODEL XTD 1.1 RUN#2 23/09/2011	Firebox Volume, ft <sup>3</sup> :	2.14	N/A for pellet type
Test Run Number:	2	A second	Convection		1 - No Fan
Date tunnel cleaned:	8/18/2011		Blower	2	2 - Fan Optional
Purpose of Test	Cat 2		Diowel		3 - Fan Standard
	A				

1.1712

		Test Settings
	Primary Air	Opened at 3/16"
	condary Air:	
	ntrol Board:	
		Off the first 30 minutes and turned On-Low after 30 minutes for the reminder of the test
	Biowenn an.	Pre- Burn Activities
Time	Activity	
(min.)		primary air at 3/16" when the scale indicated 8.750 pounds
45	Stirred the	
100		e Coal Bed and activate (door was left ajar 1/4" open) for 30 seconds.
100		ulation lasted 55 seconds
	*	
		Start-Up Procedure
Loading o	f fuel, sec. :	Loaded by 45 seconds
Fuel-lo	ading door :	Left ajar at 1/4" for 90 seconds
		Fully open the first 5 minutes. Abruptly closed (3/16") at 5 minutes.
Se	condary air:	Fixed
	ontrol board:	
E	Blower / fan:	Off the first 30 minutes and turned On-Low after 30 minutes for the reminder of the test
		Other Notes
Coal Bed	range: 2.8-3	.4 lb

- Hegy 03/2 5/12

SBI		3	VERSION	1.4	2/5/2010	1					
JDI						-					
XTD 1.9											
23-08-2011											É.
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2		- m - 3									ł.
											i i i i i i i i i i i i i i i i i i i
290											
											İ.
arometer (in Hg):	29,91	29.92									
Dry Bulb (F):	87	87									
Humidity (%):	22	22									
Contraction of the Contraction o											
position.										i i i	
wood (wet basis):	16.523										
and the second s		4.95	15,77	261.95	81,53	104.92	424,55	433.95	424.81	456.18	345.8
	•		*			•				•	
Weight				Flue	Room	Tunnel	Unit	Unit	Unit	Unit	Unit
	CO	CO2	02	Gas		Dry Bulb	Тор	Back	R.Side	L.Side	Bottom
							403 35	441.36	453.78	491.76	413.7
A							397.81	464.45	418.12	467.94	412.3
											403.3
											387.7
											366.6
											351.5
											342.8
							- N-				336.8
											332.6
				276							330 3
											329 5
				7.5.5			1.25				329_1
											328 7
2.39	0_88	4.77									327.9
2,09	0,90	4.62	15.81	254 16	80,80						328.0
1,90	0_99	4.59	15 87	246_44	78 24	104.71	414.56	518 98	471.09	502_41	328.6
1.69	1.05	4.37	16.02	240 42	76 77	102.97	400.48	515_03	468_19	492.54	330.6
1,46	0,94	3,88	16,5	238.41	74,94	103 28	389 73	506 52	464.72	484.67	333 2
1.24	1,31	3,53	16,8	233.64	75,19	102.42	383,24	497_99	464.84	477,98	335 6
1,09	1.20	3,16	17,11	226,66	81,90	98.87	373,11	491_28	448 57	470.02	340.1
0,91	1.27	3,36	17.39	222,50	80,94	99,62	361,49	481,35	432,06	458 36	343 6
0.77	1.31	2.95	17.38	218.66	85.86	99,19	349 84	467.55	417.48	445.07	345,6
0.60		1.59		213 27	81.82	98.86	341.53	455 31	411,05	431,88	347
							330.68	443.26	393.69	419.08	348.6
					78.92	96.57	316.29	426.02	377.96	403.25	344.9
			1.00		- 20						339.6
											334
											330.8
											326.5
											320 3
3	G100456088 290 Barometer (in.Hg): Dry Bulb (F): Humidity (%): v position. wood (wet basis): Average * Welght Remaining 13.85 12.99 12.33 11.13 9.80 8.59 7.34 6.18 5.19 4.34 8.66 3.10 2.65 2.39 2.09 1.90 1.69 1.46 1.24 1.09 0.91 0.77	G100456088         Start           290         Start           barometer (in.Hg):         29.91           Dry Bulb (F):         87           Humidity (%):         22           r position.         16.523           wood (wet basis):         16.523           Average         0.95           *         *           Weight         CO           11.13         0.35           9.80         0.45           8.59         0.48           7.34         0.49           6.18         0.41           5.19         0.56           4.34         0.66           3.66         0.50           3.10         0.63           2.65         0.78           2.39         0.88           2.09         0.90           1.90         0.99           1.69         1.05           1.46         0.94           1.24         1.31           0.09         1.90           0.91         1.27           0.77         1.31           0.60         1.61           0.51         1.52           0.41	G100456088         Starl         End           290         29.91         29.92           Dry Bulb (F):         87         87           Humidity (%):         22         22           r position.         0.95         4.95           wood (wet basis):         16.523	G100456088         Starl         End           290         29.91         29.92           Dry Bulb (F):         87         87           Humidity (%):         22         22           r position.         0.95         4.95         15.77           wood (wet basis):         16.523         *           Average         0.95         4.95         15.77           *         *         *         *           Weight         0.57         2.75         19.09           12.99         0.57         4.78         17.27           12.33         0.46         9.99         10.81           11.13         0.35         10.36         10.74           9.80         0.45         10.25         10.68           8.59         0.48         10.65         13.32           11.13         0.35         10.36         10.74           9.80         0.45         10.25         10.68           8.59         0.48         10.65         13.32           11.13         0.35         10.86         12.49           1.41         0.66         7.48         13.41           3.66         0.50         7.	G100456088         Starl         End           290         29.91         29.92           Dry Bulb (F):         87         87           Humidity (%):         22         22           r position.         0.95         4.95         15.77           Average         0.95         4.95         16.72           13.85         0.55         2.58         19.09         300.22           12.99         0.57         4.78         17.27         261.16           12.33         0.46         9.99         10.81         253.60           11.13         0.35         10.36         10.74         329.92           9.80         0.45         10.25         10.66         357.00           8.59         0.48         10.65         13.32         363.85           7.34         0.49         9.79         11.1         370.73           6.18         0.41         9.09	G100456088         Start         End           290         Start         End           Sarometer (in Hg)         29 91         29.92           Dry Bulb (F)         87         87           Humidity (%)         22         22           Position.         16.523         Flue           Average         0.95         4.95         15.77           Weight         16.523         Flue         Room           Remaining         CO         CO2         02         Gas           11.13         0.35         2.25         19.09         300.22         82.45           12.33         0.46         9.99         10.81         258.60         78.90           11.13         0.35         10.36         10.74         32.92         77.49           9.80         0.45         10.25         10.86         357.00         82.81           6.18         0.41         9.09         11.8         30.46         87.93           5.19         0.56         8.36         12.69         350.22         82.44           4.34         0.66         7.48         13.41         30.84         83.08           6.59         0.48 <t< td=""><td>G100456088         Start         End         Image: Start         End         Image: Start         End           290         29.91         29.92         Image: Start         End         Image: Start         Image: Start         End         Image: Start         Image: S</td><td>G100456088         Start         End         <t< td=""><td>G100456088         Start         End         <t< td=""><td>C100456088         Composition         Start         End         C         <thc< th="">         C</thc<></td></t<><td>G100456088         Image: Start         End         Image: Start         Image: Start</td></td></t<></td></t<>	G100456088         Start         End         Image: Start         End         Image: Start         End           290         29.91         29.92         Image: Start         End         Image: Start         Image: Start         End         Image: Start         Image: S	G100456088         Start         End         End <t< td=""><td>G100456088         Start         End         <t< td=""><td>C100456088         Composition         Start         End         C         <thc< th="">         C</thc<></td></t<><td>G100456088         Image: Start         End         Image: Start         Image: Start</td></td></t<>	G100456088         Start         End         End <t< td=""><td>C100456088         Composition         Start         End         C         <thc< th="">         C</thc<></td></t<> <td>G100456088         Image: Start         End         Image: Start         Image: Start</td>	C100456088         Composition         Start         End         C <thc< th="">         C</thc<>	G100456088         Image: Start         End         Image: Start         Image: Start

7/26/12 03/26/12

	Manu	afacturer:	SBI								-			
			XTD 1.9											
		Date:	23-08-20	11										
		Run:	2											
	0	Control #:	G100456	088										
						-1								
												I		
379.14	80,61	80,68	0.00	420.54	80.57	80.57	0.00	0.02	0.000	0.00	417.08			
•	•	•	•	•	×	•	•		•	Visual	Average	Change in		
DGM 1	DGM 1	DGM 1	Filter 1	DGM 2	DGM 2	DGM 2	Filter 2	Tunnel	Chimney	Smoke	Stove	Surface		Elapsed
Reading	Inlet T	Outlet T	Temp	Reading	Inlet T	Outlet T	Temp	Velocity	Draft	Observed	Temp	Temp.		Time
364,105	78.76	78.72		405.250	78,63	78 65		0.023			440.8	0		C
364.918	79.00	78.88		406,366	78,73	78,84		0,023			432.1	-8.6502		10
365,970	79.17	79.03		407,496	78,93	78,99		0,023			410.3	-30.544		20
367.022	79.19	79.17		408,435	79,06	79,09		0.023			415.3	-25.469		30
368 074	79.42	79 31		409,470	79,19	79,27		0,023			412.9	-27.9		40
369.117	79.60	79.51		410.598	79.43	79_54		0.023			429.2	-11.609		50
370.167	79.68	79.63		411,522	79,58	79.62		0.023			446.6	5.8003		60
371.210	79_97	79.85		412.571	79.79	79_89		0.023			456.0	15.188		70
372,260	80,18	80,05		413.846	79,97	80,08		0.023			459.7	18.915		80
373,315	80_45	80,31		414,698	80_21	80,29		0.023			461.0	20,245		90
374.368	80_47	80_46		415.761	80_33	80,43		0.023			456.8	16,044		100
375.424	80,63	80,62		416.813	80_41	80_49		0.023			460.8	20.009		110
376,477	80,84	80,75		417.894	80,59	80,69		0.023			473.4	32.58		120
377.531	80,91	80,90		418.940	80 72	80,81		0.023			463.0	22.234		130
378.585	81,01	81,03		419,956	80,90	80,94		0.023			451.3	10.471		140
379.645	81,07	81,16		421.024	80,99	80,99		0.023			447.1	6.348		150
380,705	81,14	81 24		422,191	81,06	81,10		0.023			441.4	0.5917		160
381.765	81,22	81,33		423,156	81_15	81,15		0.023				-5.0141		170
382.823	81.25	81.40		424.220	81.24	81.22		0.023				-8.8184		180
383.879	81,18	81 39		425.273	81 29	81.20		0.023	1-1-1		424.6	-16,168		190
384.944	81.18	81.43		426,347	81.31	81.24		0.023			415.4	-25.421	·	200
385.998	81_17	81.41		427.398	81_28	81.19		0.023			405.1	-35.645		210
387.061	81,22	81.45		428,458	81.33	81.24		0.023			397.5	-43.32		220
388_114	81.22	81.47		429.504	81_37	81.24		0.023			387.1	-53.689		230
389,174	81.33	81.56		430.568	81.45	81.37		0.023			373.7	-67.093		240
390.224	81,35	81,63		431.616	81.54	81,43		0.023			358.4	-82.432		250
391.285	81 36	81.63		432.678	81.55	81.47		0.023			346.8	-93.993		260
392 331	81 32	81.65		433.732	81.56	81,45		0.023	- N - N 3		334.7	-106.07		270
393.392 394.441	81_42 81_49	81.67 81.76		434.790 435,836	81_62 81_75	81,52 81,61		0.023			324.8 318.2	-116.03	100.50	280

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	Manu	facturer:		SBI				
		Model:		XTD 1.9				
		Date:		23-08-2011				
		Run:		2				
1	Project	#:		G100456088				
	Test Dura	ation:		290				
Total Gas V	olume (D	GM 1):		29,605	Pit	ot Factor	0.82	
Total Gas V	1000000000000000000	C401041030		29 735		(0	.99 standar	
Average Baro	1.000			29.915		0.84 or Ca	al. Factor fo	S-Type
		lar Weig	ht	28.56				
		orrection		0.9124				
Calibration Fa			1	1,0000				
Calibration Fa				0.9960				
			(1) VS:	0.0280				
			(2) VS:	0.0279			Filter	Filler
							Face	Face
DGM 1	DGM 1	DGM 1	DGM 2	DGM 2	DGM 2	Tunnel	Velocity	Velocity
Reading	Inlet T	Outlet T					DGM 1	DGM 2
364.105	78.8	78.7	a	78.629247	78,652	122.16		
364.918	79.0	78.9	406.366	78.725053	78.837	105.5	6,86	9,3
365,970	79.2	79.0		78.934498	78.987	102.08	8.88	9.5
367.022	79.2	79.2	408,435	79.061544	79.09	107.19	8.88	7.8
368,074	79.4	79.3		79,186059	79.274	112.16	8.87	8.7
369.117	79.6	79.5	410,598	79,432406	79,538	112.23	8.79	9,4
370,167	79.7	79.6		79.581358	79.624	117.37	8.85	7.7
371.210	80.0	79.8		79,791744	79.885	116.47	8,79	8.8
372,260	80.2	80.0		79.96844	80.081	115.1	8.84	9.0
373.315	80.4	80.3	1	80,208142	80.289	115.09	8,88	8.8
374.368	80.5	80.5	<u></u>	80.329168	80.434	111.82	8,86	8.9
375.424	80.6	80.6	416.813	80,412347	80,494	110.52	8.89	8.8
376.477	80.8:		417.894	80,591955	80.686	109.15	8,86	9.0
377.531	80.9	80.9	418.940	80.719212	80.815	106.67	8.86	8.7
378,585	81.0		419.956	80.90165	80.938	105.14	8,86	8.5
379,645	81.1		421.024	80,991852	80.995	104.71	8.91	8.9
380,705	81.1		422.191	81,06308	81.1	102.97	8.91	9.7
381,765	81.2		423,156	81,154143	81.148	103.28	8.91	8.0
382.823	81.2		424.220	81.240354	81.219	102.42	8,89	8.9
383,879	81.2		425.273	81.287122	81.198	98.871	8.87	8.8
384.944	81.2		425.273	81.309336	81.245	99.623	8.95	8.9
385,998	81.2		427.398	81.276636	81.191	99.191	8.86	8.8
385,998	81.2		428.458	81.330697	81.243	98.865	8,93	8.8
388.114	81.2		429.504	81.365372	81.243	97.227	8.85	8.7
· · · · · · · · · · · · · · · · · · ·	81.3		429.504	81.447432	81.37	96.566	8.91	8.9
389.174	81.3		430.568	81.543416	81.428	97.342	8,82	8.7
390.224			÷1	81,543416	81.472	97.342	8.91	o./ 8,8
391.285	81.4		432.678				8.79	8.8
392.331	81.3		433.732	81,556603	81.455	ちてんごうじゅードタンパン 第二	8.79	8.8
393.392	81.4	81.7		81.616452			8.81	
394.441	81.5	81.8	435,836	81.749149	81,608	93.474	0.01	8.7

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	Proportio	nal Rate	Calculatio	ons	(EPA Formu	ulas from F	PR5G)	
	Stack are	a (ft2)	0.3491		Mar	ufacturer:	SBI	
Mood	moisture (	and the second se	16.523		14101		XTD 1.9	
	Veight (lbs		13.9				23-08-20	11
	ate (Dry k	beauties and the second	1.089			Run:		
Dunn		griny.	1.000			T GIT.	-	
inal Ter	nperature	(DGM #1	Degree	e Renkin <sup>.</sup>	540,644			
	nperature	A Design of the Coldenser	Advert and an area		540.567			
	unnel Tem				564.923			
	unnel Velo	And the second of the second in	Children and the second of		7.802204			
	ndardized				146.54			
010		Turine T	1011 (400)					
		Average	Average					
		Inlet +	inlet +					
		Outlet	Outlet	99.94	99.94	#1	#2	
Tunnel	Tunnel	Temp.	Temp.			dDGM	dDGM	
Velocity	Velocity	Meter 1	Meter 2			Vol.Std.	Vol.Std.	
Delta-P	Ft/Sec	Deg. R	Deg. R	PR1	PR2	(ft3)	(ft3)	Time
0.023	7.921	538.7	538.6					0
0.023	7.806	538,9	538.8	78.02	106.23	0.796	1.089	10
0.023	7.783	539,1	539.0	100,61	107.20	1.030	1.102	20
0.023	7.818	539.2	539.1	101.06	89.47	1.030	0.916	30
0.023	7.852	539.4	539.2	101.46	99.01	1.029	1.009	40
0.023	7.853	539,6	539.5	100,56	107.87	1.020	1.099	50
0.023	7.888	539.7	539.6	101.67	88.74	1.027	0.900	60
0.023	7.882	539.9	539.8	100.87	100.62	1.019	1.021	70
0.023	7.872	540.1	540.0	101.39	102.95	1.026	1.046	80
0.023	7.872	540.4	540.2	101.82	100.71	1.030	1.023	90
0.023	7.850	540.5	540.4	101.32	101.45	1.028	1.034	100
0.023	7.841	540.6	540.5	101.46	100.27	1.031	1.023	110
0.023	7.832	540.8	540.6	101.02	102.87	1.028	1.051	120
0.023	7.814	540.9	540.8	100.88	99,30	1.028	1.017	130
0.023	7.804	541.0	540.9	100.72	96.30	1.028	0.987	140
0.023	7.801	541.1	541.0		101.17	1.034	1.038	150 160
0.023	7.789	541.2 541.3	541.1 541.2	101.07 101.08	110.36 91.27	1.034	1.134 0.937	170
0.023	7.791	541.3	541.2		100.55	1.033	1.033	180
0.023	7.760	541.3	541.2	100.80	99,19	1.031	1.033	190
0.023	7.766	541.3	541.2		101.23	1.023	1.023	200
0.023	7.763	541.3		100.14	99.03	1.028	1.043	210
0.023	7,760	541.3	541.3	100.96	99.84	1.036	1.029	220
0.023	7.749	541.3	541.3	99.86	98.37	1.026	1.016	230
0.023	7.744	541.4	541.4	100.44	99.99	1.033	1.033	240
0.023	7.750	541.5	541.5	99.56	98.54	1.023	1.017	250
0.023	7.744	541.5	541.5	100.52	99.77	1.034	1.031	260
0.023	7.734	541.5	541.5	98.98	98.90	1.019	1.023	270
0.023	7.719	541.5	541.6	100.19	99.07	1.034	1.027	280
0.023	7.723	541.6	541.7	99.09	97.97	1.022	1.015	290

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			Intertek Testing Service	S				
			SFBA EPA ADJUSTED	EMISSION	RESULTS			
Man	ufacturer		SBI			RESULT	s	
		Model	XTD 1.9			1.1.1.1.1.1.1.1		
	t -		23-08-2011		-	erage Adjusted Emis	elons Rate	4.07
	1 -	Run:				arage Unadjusted Em	CALLS CONTRACTOR STATE	2.84
	D		G100456088		AV		(Dry kg/hr):	1.09
Test		and a particular of				DUIN Rale	(Dry kg/m).	31105
	Duration (M	state of the second second	16.560		i			
Tes	st Duration (	nours).	4.83					
	I				5150			
	÷				BAROM	IETRIC PRESSU		00.04
					-		Average:	29.91
	TEMPERAT	JRE FAC					Start:	29.9
			DGM #1:	0.9766			End:	29.9
			DGM #2:	0.9768				
	as essention market				DRY GAS	METER VALUES		
	VOLUMES	SAMPI				DGM #1	Final:	394.44
			DGM #1:	29,622			Initial:	364.10
			DGM #2:	29,750				
	- mil 1					DGM #2	Final:	435.83
	TOTAL TU	NNEL V	/OLUME (scf):	42496			Initial:	405.2
	SAMPLE F	ATIOS			TEMPE	RATURES (DEG	RANKIN)	
		Sample	e Train 1:	1434.6	F E		DGM #1:	540.64
		Sample	e Train 2:	1428.4			DGM #2:	540.57
	TOTAL EN	ISSION	S		CALIBR	ATION FACTOR	s	
		e Train		12.34			DGM #1:	1.000
		e Train		13.14			DGM #2:	0.996
	Cumpi	e main	Ave:	12.74			D'OIII II Z.	0.000
	EMISSION	RATES		0.000	TUNNE	L FLOW RATE:		146.5
	Sample			2.55	TOININE	PARTICULATE	CATCH IN	
	Sample		17	2.33			e Train 1:	(9)
	Sample	mail 2		2.72		and the second sec	Filters	7.
		DEMO	Ave: SION RATES	2.04			Probe	
	post manufactor through the second	of the set of a rise Cr		3,96				0.9
	Sample				(]a	<b>D</b>	Total	8,
	Sample	main 2		4.17	i-	Sampl	e Train 2:	
		DE	Ave:	4.07	·		Filters	8,
		DEV	IATION:	2.62%			Probe	0,
							Total	9.2
			ter than 7.5% due to low		catch			
			rates shall not differ by 7.					
	of the weig	hted av	erage emission rate limit	(4.1 or 7.5)	(5g-3)			
	Use the fol	lowing:						
	Catalutie	aite		5.20%				
	Catalytic un			5.20%				
	7.5% of 4.1	g/hr						
		_		01/0201400				
	Non catalyt			2.84%				
	7.5% of 7.5	an Danim						



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	REPORT	DATA			No.			
	CEI OITI	Brint						
1 1 1 T		Client:	SBI				-	
		Run:	2					
		Date:	23-08-2011		1			
		Project:	G100456088		- w			
		Model:	XTD 1.9					
Fuel M	loisture (	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	19 79333333					
	Static (n		0.095					
oracia		meter:	29,915					
Aver	age Roor	1.1.2.2.2.112	81.53					
river	ige ribbl	n romp.	01.00		1			
					-			
Change	a in stove	e temp:	-122.582564		-			
onlang	5 11 51071	a comp.	122.002001					
	Bum F	tate:	1.089					
Adjusted	I Emissic		4.068					
· · · · · · · · · · · · · · · · · · ·		em 1:	3,962					
1		em 2:	4.175					
	Devia		2.62%		1			
	Filter	r 1:	0.00					
	Filter	12:	0.00		Ť.			
	Tur	nnel:	104.92					
		DGM 1:	80.64					
		DGM 2:	80.57					
	Water Co	ollected:						
					1			
	Room	Temp	Bar Pressure		Relative Hu	midity	Air Velo	city
	Before	After	Before	After	Before	After	Before	After
	87	87	29.91	29.92	22	22	0	0

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Flue	Room	Tunnel	Unit	Unit	Unit	Unit	Unit	Scale
Gas	Temp	Dry Bulb	Тор	Back	R.Side	L.Side	Bottom	weight
436.96	84.08	156.35	477.01	405.05	577.00	562.04	422.45	12.69
624.55	81.62	180.81	764.07	377.45	587.52	541.59	432.65	10.03
403.01	77.67	130.83	670.34	380.39	560.45	546.41	450.00	8.37
379.40	76.14	125.41	639.99	408.64	546.39	546.11	456.44	6.96
358.50	77.87	120.73	601.00	414.39	542.31	544.89	454.52	5.89
352.85	78.32	4170.00	600.28	516.58	528.07	550.43	449.09	4.82
380.09	88.48	126.33	606.60	505.74	526.66	554.50	439.75	3.77
310.65	85.91	113.21	568.36	534.91	508.50	553.92	428.14	3.38
275.85	86.85	108.41	485.65	497.23	479.31	530.34	420.71	3.17
257.11	84.35	103.86	437.27	493.99	457.76	507.45	414.97	2.99

100

	TUNNEL VELOCITY	TUNNEL	SQUARE ROOT
A CENTER	0.023	120	0.1500
<b>B</b> CENTER	0.023	118	0.1500
A1	0.018	118	0.1323
A2	0.020	117	0.1414
A3	0.020	118	0.1414
A4	0.018	113	0.1323
B1	0.018	117	0.1323
B2	0.020	118	0.1414
B3	0.020	118	0.1414
B4	0.018	116	0.1323
AVERAGE	0.0195	117.24	0.1369
unnel Diameter (	in):	8	1

- 64 ---

E&E Tunnel Traverse Worksheet

2.20

PITOT CONSTANT 0.9124

Static Pressure:

Tunnel Diameter (in): Tunnel Area (ft2) Tunnel Static Pressure

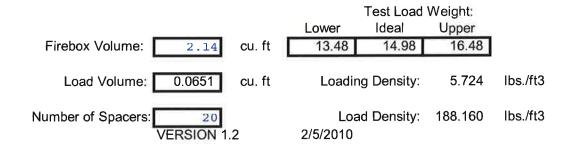
0.349066 -0.095

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### **E&E FUEL LOAD DATA SHEET**



		Piece S	Size:		Weight	М	eter Moistu	re Content
Thick	х	Wide	х	Length	lbs		Dry Unco	rrected %
	2		4	12	1	20.1	20.6	20.2
	2		4	12	1	20.2	20.3	20.4
	2		4	- 12	1	21	20.3	20.5
	2		4	12	1.1	20.5	19.8	18.9
	2		4	16	1.65	21.1	20.3	22
	2		4	16	1.85	20.30	19.90	20.40
	2		4	16	1.70	19.80	21.00	21.00
	2		4	16	1.65	20.90	19.90	21.10
	2		4	16	1.30	21.40	20.30	21.00

Test Load Weigh	12.25 lbs.	Dry Weigh	4.60	) kg.
Dry: 20.58	two pin: (dry)		wet:	17.29

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			Test Load Weight:			
		L	ower	Ideal	Upper	
Firebox Volume: 2.14	cu. ft		13.48	14.98	16.48	
Load Volume: 0.0651	cu. ft		Loadin	g Density:	6.495	lbs./ft3
Number of Spacers: 20			Loa	d Density:	213.504	lbs./ft3

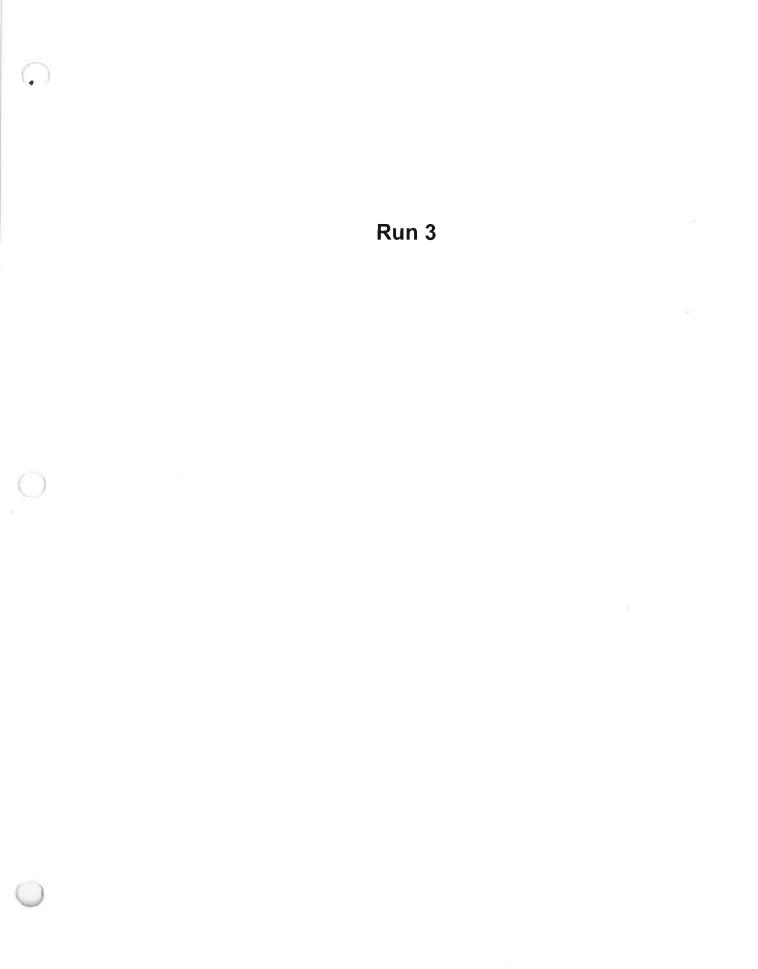
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	Piece Size:		Weight		Moisture C	
Thick x	Wide x	Length	lbs	Dry	Uncorrecte	d %
2	4	15.75	1.35	19.30	19.30	18.60
2	4	15.75	1.30	19.80	19.20	19.80
2	4	15.75	1.95	22.20	21.90	21.50
4	4	15.75	3.55	19.70	19.10	18.90
4	4	15.75	3.60	19.80	19.20	18.60
		Spacers	2.15			

Test Load Weigh 13.90 Ibs.	Dry Weigh	5.26 kg.
Average Moist	ture Content: %	Wet: 16.52
Pre-test moist	20.58	Wet: 17.07
Coal Bed Range: 2.8 lbs.		20% to 25% of test load

03/26/12

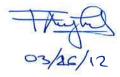




#### Run Notes EPA Methods 28 and 5G-3

PROJECT / TES	T INFORMATION		Appl	iance	Information
	and the second design of the s	K.V	Appliance Type:	2	1 - Catalytic 2 - Non - Catalytic 3 - Pellet 4 - Hydronic
Test Date:	24-Aug-11	RUN#3 24 /08/2011	Firebox Volume, ft <sup>3</sup> :	2.14	N/A for pellet type
Test Run Number: Date tunnel cleaned: Purpose of Test	3 8/18/2011 Cat 3		Convection Blower	2	1 - No Fan 2 - Fan Optional 3 - Fan Standard

		Test Settings
P	Primary Air:	Open at 3/4"
Sec	ondary Air:	Fixed
Con	ntrol Board:	N/A
В	Blower/Fan:	Off the first 30 minutes and turned On-Low after 30 minutes for the reminder of the test
		Pre- Burn Activities
Time	Activity	
(min.)	Closed the	primary air at 3/4" when the scale indicated 11.5 pounds
45	Stirred the	Coad Bed
100	Leveled the	e Coal Bed and activate ( door left ajar at 1/4 " open) for 30 seconds
	This manip	pulation lasted for 55 seconds
		Start-Up Procedure
Loading of	fuel, sec. :	Loaded by 45 seconds
Fuel-loa	ding door :	Left ajar (1/4") for 60 seconds
F	Primary air:	Fully open the first 5 minutes. Abruptly closed at 3/4" at 5 minutes.
Sec	ondary air:	Fixed
Con	ntrol board:	N/A
Bl	lower / fan:	Off the first 30 minutes and turned On-Low after 30 minutes for the reminder of the test
		Other Notes
Coal Bed ra	ange: 2.8-3	.4 lb



	1			VERSION 1	2	2/5/2010					1	
Manufacturer	SBI					1						
	XTD 1.9	· · · · · · · · · · · · · · · · · · ·									V	
Date	24-08-2011											
Run:	3											
Control #	G100456088											
Test Duration:	170											
		Start	End						- · · · · · · ·			
	Barometer (in.Hg):	29.95	29.95									
	Dry Bulb (F):	87	87									
	Humidity (%):	24	23				1					
	rianiany (70).		20									
*Blower turned on at 30 min-lov	and the platestic design of the second se									_		
Moisture content of	f wood (wet basis):	16.2666										
	Average	0.67	6.54	14.49	400,69	84.74	132.32	544.97	512.12	498.60	550.21	353,50
	•	*					•					
Elapsed	······································			:	Flue	Room	Tunnel	Unit	Unit	Unit	Unit	Unit
emiT	1	CO	CO2	02	Gas	Temp	Dry Bulb	Тор	Back	R.Side	L.Side	Bottom
0			9.22	13 27	411.36	79 92	140.87	459,32	545 92	457.42	501,75	355.4
10		0.35	12.02	9,09	428.60	86.01	134_97	502.97	520.06	429.67	482,87	367.9
20		0.25	11.24	9,51	519 39	88,59	145.22	648,93	344.21	448 44	486,08	363.7
30		0.23	9.82	11,58	523 57	83,76	150.61	721.59	382_50	481,50	515,53	356,74
40		0.25	9.31	11.84	486_62	84.40	143.78	695.04	451.44	484.42	548.25	346.9
50		0.28	9.26	12,39	471,68	83,90	144.26	674.20	579.88	481.15	566,31	342.6
60		0.31	9.07	12.3	455.04	84,87	141.52	642 64	508,43	487.35	576 32	339,14
70		0.33	8.65	12.27	443,62	85,90	140_46	625,04	520,19	506,93	594.70	337 5
80		0.44	6.71	14,48	446 82	87,57	141.54	626,91	574.44	539,29	609 75	338.30
90		0.62	5.17	15.57	409.73	87.68	136 35	598,55	498.75	555,60	618,37	341,97
100		0.71	4.68	16.07	378.42	84.80	132,65	552 16	609.09	553,59	609,16	346,88
110		0.88	4.24	16 66	356 21	89,61	126,80	505,55	470,40	549.92	589,89	351,59
120		0.84	4.39	16 54	339.80	86.98	120.67	471.17	519.61	526.07	570.29	354.9
130		1.02	3.82	17.06	330 15	85 73	118,15	450,10	570.17	513,49	554 18	358.0
140	0.49	1.29	2.77	17.65	320.03	82,93	118.71	434,81	555.03	504,46	541.87	361.90
150		1.38	2.69	17.84	310.06	81.65	117_44	418,62	540.63	496.79	529.77	
150 180 170	0.05	1.38 1.32 1.18	2.69 2,29 2.42	17.84 18,28 18,49	310.06 295.84 285.49	81.65 80.85 80.11	117_44 115 22 112 53	418.62 399.25 382.59	540.63 523.31 504.09	496.79 482.64 476.04	529.77 513.84 494.79	365 42 367 37 366 54

- Tagel 03/26/12

									1					
Manu	facturer	SBI							1					
		XTD 1.9												
-	Date:	24-08-20	11						i l					
	Run:													
C	Control #:	G100456	088											
403,26	83.75	83.75	85.51	444.75	83.54	83.54	86.99	0,02	0.000	0.00	491.88			
*	*	*	•	•	•		•	•	•	Visual	Average	Change in		
DGM 1	DGM 1	DGM 1	Filter 1	DGM 2	DGM 2	DGM 2	Filter 2	Tunnel	Chimney	Smoke	Stove	Surface		Elapsed
Reading	Inlet T	Outlet T	Temp	Reading	Inlet T	Outlet T	Temp	Velocity	Draft	Observed	Temp	Temp.		Time
394.453	81.79		82.20	435,849	81,67	81.62	81.84	0.020			464.0	0	_	C
395.485	82.15	82,01	86.65	436.941	81,94	81.93	87.71	0.020			460.7	-3.2684		10
398,540	82.33	82,24	88.95	437.999	82,10	82_12	89,96	0.020			458.3	-5.6832		20
397.558	82.72	82,53	86.31	439.017	82,39	82 47	88.02	0.020			491.6	27.599		30
398,589	83:10	82.89	84.53	440.055	82.67	82.79	86.56	0.020			505.2	41.236		40
399,631	83 27	83,11	84,15	441,122	82,88	82,99	85,60	0.020			528.8	64.861		50
400,669	83.57	83.42	84.51	442.185	83,17	83_30	85.84	0.020			510,8	46.802		60
401.710	83,80	83,67	84.17	443.210	83_44	83 54	86,16	0.020			516.9	52.904		70
402.744	84.00	83,90	84_14	444.243	83,71	83 76	86,17	0.020			537.7	73.765		80
403,774	84 12	84.10	83.98	445.271	83.87	83.91	86,54	0.020			522.6	58.673		90
404.805	84.20	84,23	83,67	446.305	84_01	83,98	86 12	0.020			534.2	70.203		100
405,847	84 35	84.41	87.52	447.345	84 14	84,10	89,05	0.020			493.5	29.5		110
406,882	84_35	84 49	83.47	448.387	84 18	84 11	85.29	0.020			488.4	24.439		120
407.925	84 51	84.65	86,31	449.423	84,36	84 28	87,66	0.020			489.2	25.215		130
408.961	84,70	84.82	88.05	450.483	84,58	84,50	89,33	0.020			479.6	15.64		140
410,002	84,80	84.97	84.87	451.500	84_77	84,69	86,23	0.020			470.2	6.2748		150
411.041	84,85	85.06	87.38	452,549	84,85	84.73	88,34	0.020			457.3	-6.6922		160
412.079	84.95	85.14	88.34	453.580	84.95	84.85	89,35	0.020	4		444.8	-19.163	-19.163	170

- Hayful 03/26/12

			(	E				
····	Manu	facturer:		SBI				
		Model:		XTD 1.9				
		Date:		24-08-2011				
		Run:		3				
Project #			G100456088					
1	Test Dura	ition:	1	170				
Total Gas Ve	olume (D	GM 1):		17.122	Pit	ot Factor	0.82	
Total Gas Ve	Total Gas Volume (DGM 2):					()	0 99 standar	d,
Average Barometric Pressure:			29.95		0.84 or C	al. Factor fo	r S-Type)	
Molecular Weight			ht	28.56				
	Pitot Co	orrection	2	0 9342				
Calibration Factor (DGM #1):				1.0000				
Calibration Factor (DGM #2):				0.9960				
			(1) VS:	0.0456				
			(2) VS:	0.0455			Filter	Filter
			and a concerned and				Face	Face
DGM 1	DGM 1	DGM 1	DGM 2	DGM 2	DGM 2	Tunnel	Velocity	Velocity
Reading	Inlet T.	Outlet T	a high constant provide a second				DGM 1	DGM 2
394.453	81.8	81.8		81,668899	81.618	140.87		
395.485	82.2	82.0	436.941	81.941464	81.932	134.97	8.67	9.14
396.540	82.3	82.2		82.095693	82.122		8.86	8.8
397.558	82.7	82.5	439.017	82.388255	82.469	150.61	8.54	8.5
398.589	83.1	82.9	440.055	82.670854	82.791	143.78	8.65	8.68
399,631	83.3	83.1	441.122	82.884323	82.987	144.26	8.74	8.91
400.669	83.6	83.4	442.165	83.167972	83,301	141.52	8.70	8.71
401.710	83.8	83.7	443.210	83.438783	83.54	140.46	8.72	8.72
402.744	84.0	83.9	444.243	83.705638	83.757	141.54	8.66	8.62
403.774	84.1	84.1	445.271	83.867129	83,913	136.35	8.62	8.57
404.805	84.2	84.2	446.305	84.006334	83.975	and the state of the	8.63	8.62
405.847	84.3	84.4	447.345	84.137122	84.099	126.8	8.72	8.6
406.882	84.4	84.5		84.184462	84.11	120.67	8,66	8.6
407.925	84.5	84.6	449.423	84.363675	84.283	118.15	8.72	8,6
408.961	84.7	84.8	450.463	84.576035	84.501	118.71	8.66	8,6
410.002	84.8	85.0	451.500	84.772274	84.687	117.44	8.70	8.6
411.041	84.8	85.1		84.85142	84.735	115.22	8.68	8.73
412.079	84.9	85.1	453.580	84,946482	84,853	112.53	8.67	8.58

Thypes 03/26/12

	Proportio	nal Rate	Calculatio	(EPA Formu	PR5G)			
	Charalt and	(110)	0.0404		Mar	for all use as	0.01	
Stack area (ft2): Wood moisture (% wet):		second and a second	0.3491		Mar	ufacturer:		
	and the south the second state of the	Construction of Construction	16.267				XTD 1.9	
	Veight (Ibs	ACCOMPANY 1	13.7				24-08-20	11
Burn R	ate (Dry k	g/hr):	1.837			Run:	3	
		(DGM #1	The lot of					
Final Ter	nperature	(DGM #2	) Degrees	s Rankin:	543.537			
Final Tu	un <mark>nel Tem</mark>	perature i	Degrees I	Rankin:	592.318			
Final Tu	unnel Velo	city (feet	per secon	id):	7.707459			
Sta	ndardized	I Tunnel F	low (dscf	m):	138.22			
		Average	Average					
		Inlet +	inlet +					
		Outlet	Outlet	99.95	99,95	#1	#2	
Tunnel	Tunnel	Temp.	Temp.			dDGM	dDGM	
Velocity	Velocity	Meter 1	Meter 2			Vol.Std.	Vol.Std.	
Delta-P	Ft/Sec	Deg. R	Deg. R	PR1	PR2	(ft3)	(ft3)	Time
0.020	7.763	541.8	541.6				· · · · ·	0
0.020	7.725	542.1	541.9	100.08	105.26	1.006	1.060	10
0.020	7.791	542.3	542.1	103.15	102.82	1.028	1.027	20
0.020	7.826	542.6	542.4	99.91	99.31	0.991	0.988	30
0.020	7.782	543,0	542.7	100.55	100.64	1.003	1.006	40
0.020	7.785	543.2	542.9	101.63	103.46	1.013	1.034	50
0.020	7.768	543,5	543.2	100.95	100.84	1.009	1.010	60
0.020	7.761	543.7	543.5	101.11	100.90	1.011	1.012	70
0.020	7.768	544.0	543.7	100.48	99.79	1.004	1.000	80
0.020	7.734	544.1	543.9	99.63	98.85	1.000	0.995	90
0.020	7.710	544.2	544.0	99.40	99.10	1.001	1.000	100
0.020	7.672	544.4	544.1	99,93	99.15	1.011	1.006	110
0.020	7.632	544.4	544.1	98.73	98.82	1.004	1.008	120
0.020	7.615	544.6	544.3	99,25	98.01	1.012	1.002	130
0.020	7.619	544.8	544.5	98,60	98,39	1.005	1.005 ;	140
0.020	7.610	544.9	544.7	98.94	97.97	1.009	1.002	150
0.020	7.596	545.0	544.8	98.55	98.90	1.007	1.013	160
0.020	7.578	545.0	544.9	98.21	96,95	1.006	0,996	170

- Thughl 03/26/12

		Intertek Testing Service:	5				
		SFBA EPA ADJUSTED	EMISSION F	RESULTS			
Manufacturer.		SBI			RESULT	s	
manara otor or .	Model	XTD 1.9			THE OFFICE		
		24-08-2011		Aaraa	Adjusted Emis	einne Rate:	3.15
	Run:	and the second se			Unadjusted Emis		1.93
D		G100456088		Average	Bum Rate		1.84
					Dunnate	(DIY KGHI)	
Test Duration (M Test Duration (		2.83					
Test Duration (	nours).	2.03		_			
				BAROMETE	RIC PRESSU	RE	
				Britterine II	Menter of the state of the second	Average:	29.9
TEMPERAT	IDE EAC	TOPS				Start:	29.9
TEIM EIGHT	DINETINO	DGM #1:	0.9710			End	29.9
		DGM #2:	0.9714				
		DOM NZ.	0.0111	DRY GAS MET	FR VALUES		
VOLUMES SAMP		LED			DGM #1	Final:	412.07
, of an or righting		DGM #1:	17,133		T. T. M. C. T.	Initial:	394.45
		DGM #2:	17,172				
					DGM #2	Final:	453.5
TOTAL TU	INNEL V	/OLUME (scf):	23498			Initial:	435.84
SAMPLE F	RATIOS			TEMPERAT	URES (DEG.	RANKIN)	
		e Train 1;	1371.5			DGM #1:	543.75
		e Train 2:	1368.4			DGM #2:	543.54
TOTAL EN	IISSION	IS		CALIBRATIO	ON FACTOR	3	
	e Train		5,62	1		DGM #1:	1.000
	e Train	1-1-1	5.34			DGM #2:	0.996
		Ave:	5.48				
EMISSION	RATES	3		TUNNEL FL	OW RATE:		138.2
Sample	Train 1	(g/hr):	1.98	PA	RTICULATE	CATCH (m	ng)
Sample			1.88	1		a Train 1:	
		Ave:	1,93		1	Filters	3.
ADJUSTE	DEMIS	SION RATES				Probe	0.
Sample			3.21			Total	4.
Sample			3.08		Sample	e Train 2:	
100000000000000000000000000000000000000	0.00200.0020	Ave:	3.15		8	Filters	3.
	DEV	ATION:	2.17%			Probe	0.
				n w - 1		Total	3.
If deviation	is grea	ter than 7.5% due to low	particulate ca	atch			
		rates shall not differ by 7.		1			
of the weig	hted av	erage emission rate limit	(4.1 or 7.5) (	5g-3)			
Use the fol	lowing:						
Catalytic u	nits		3.33%				
7.5% of 4.1			0.0074				
New ontobu	tic units		1.82%				



	diama l						
REPOR	RT DATA					1	
	0111	0.01		1			
	Client:	SBI					
	Run:	3					
	Date:	24-08-2011				-	
	Project:	G100456088					
tana Kanasa	Model:	XTD 1.9					
Fuel Moisture		19.42666667					
Stack Static		0.0925				f	
	rometer:	29.95					
Average Ro	om Temp:	84.74					
					i		
Change in sto	ve temp:	-19.1629032					
	+						
Bun	Rate:	1.837					
Adjusted Emiss	sion Rate:	3.146					
Sy	stem 1:	3.215					
Sy	stem 2:	3.078				1	
De	viation:	2.17%					
Fil	ter 1:	85.51					
Fil	ler 2:	86.99					
Т	unnel:	132.32					
	DGM 1:	83,75		1			
	DGM 2:	83.54		8			
Water	Collected:						
	Tomp	Bar Pressure		Relative H	umidity	Air Velo	ocity
Roo							
Roo Before		Before	After	Before	After	Before	After

Hughs ) 03/26/12

Flue	Room	Tunnel	Unit	Unit	Unit	Unit	Unit	Scale
Gas	Temp	Dry Bulb	Тор	Back	R.Side	L.Side	Bottom	weight
567.07	76.35	273.15	307.58	143.34	166.31	131.18	99.32	13.26
475.66	74.22	139.84	444.71	228.98	239.26	215.69	118. <b>71</b>	11.41
414.66	74.90	126.85	508.05	307.54	279.23	285.27	154.91	9.77
460.30	76.73	132.23	571.50	383.73	345.65	347.66	193.50	8.12
456.26	79.04	134.34	608.37	447.02	382.60	412.68	229.95	6.65
449.39	80.44	135.37	609.73	495.01	425.45	462.86	266.06	5.32
425.93	82.33	132.80	595.63	536.00	463.81	509.88	309.39	4.16
365.27	81.41	123.79	524.79	556.51	453.37	520.86	338.29	3.65
339.69	81.00	120.99	474.50	550.58	452.38	508.48	351.85	3.18

- Thypel 03/26/12

### E&E Tunnel Traverse Worksheet

TUNNEL TUNNEL SQUARE **VELOCITY TEMP** ROOT 132 A CENTER 0.020 0.1414 0.020 133 **B CENTER** 0.1414 **A**1 0.018 131 0.1323 0.020 131 A2 0.1414 0.018 130 0.1323 A3 128 0.015 A4 0.1225 133 **B1** 0.018 0.1323 134 **B**2 0.020 0.1414 134 **B**3 0.018 0.1323 128 0.015 0.1225 **B4 AVERAGE** 0.018 131.46 0.1321

Static Pressure:

PITOT CONSTANT

0.9342

Tunnel Diameter (in): Tunnel Area (ft2) Tunnel Static Pressure

8
0.349066
-0.0925

03/26/2

## **E&E FUEL LOAD DATA SHEET**

			Test Load	Weight:	
		Lower	Ideal	Upper	
Firebox Volume: 2.14 cu	i.ft 🛛	13.48	14.98	16.48	
Load Volume: 0.0000 cu	ı. ft	Loadin	g Density:	5.958	lbs./ft3
Number of Spacers: VERSION 1.2		Loa 2/5/2010	d Density:	#DIV/0!	lbs./ft3

		Piece Si	ze:		Weight	Meter Moisture Content				
Thick	х	Wide	х	Length	lbs		rrected %			
	2		4	12	1.2	19.5	20.9	20.8		
	2		4	12	1.15	21.2	21.1	21		
	2		4	12	1.25	20.3	20.4	20.9		
	2		4	12	1.15	20.5	21.6	21.7		
	2		4	16	1.55	20.5	20.8	21.4		
	2		4	16	1.65	20.80	19.70	20.30		
	2		4	16	1.60	21.50	20.10	20.10		
	2		4	16	1.60	21.00	20.80	20.90		
	2		4	16	1.60	21.00	19.20	20.20		

Test Load Weigh 12.75 lbs.

Dry Weigh

Dry 20.47

Average Pretest Moisture Content: % two pin: (dry) 20.90

Wet:

17.29

kg.

4.78

03/26/12

0

			Test Load	Weight:	
		Lower	Ideal	Upper	
Firebox Volume: 2.14	cu. ft	13.48	14.98	16.48	
Load Volume: 0.0651	cu. ft	Loading	g Density:	6.402	lbs./ft3
Number of Spacers: 20		Load	d Density:	210.432	lbs./ft3

	Piece Size: Wide x	Length	Weight Ibs	Meter Moisture Content Dry Uncorrected %			
2	4	15.75	1.50	19.50	19.50	19.50	
2	4	15.75	1.55	19.30	19.50	19.90	
2	4	15.75	1.45	19.20	19.10	19.10	
4	4	15.75	3.70	19.80	18.80	19.20	
4	4	15.75	3.35	19.50	19.50	20.00	
		Spacers	2.15				

Test Load Weigh 13.70 Ibs.	Dry Wei	<b>gh</b> 5.20 kg.
Dry: 19.43	ure Content: %	Wet: 16.27
Pre-test moistu	ure content: %	Wet: 16.99
Coal Bed Range: 2.8 Ibs.	to <u>3.4</u> lbs.	20% to 25% of test load
	The	£S

03/26/12

Run 4

 $\bigcirc$ 



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### Run Notes EPA Methods 28 and 5G-3

PROJECT / TES	T INFORMATION	Apr	liance	Information
Manufacturer: Model:	G100456088 SBI XTD 1.9 MTL1108221414-001	Appliance Type:	2	1 - Catalytic 2 - Non - Catalytic 3 - Pellet 4 - Hydronic
Test Date:	25-Aug-11	SBT FINCEL XTD14 FINCEL XTD14 F	2.14	N/A for pellet type
Test Run Number: Date tunnel cleaned:	4 8/18/2011 Fan Confirmation	Convection	2	1 - No Fan 2 - Fan Optional 3 - Fan Standard

The second second second

Test Settings	
Primary Air: Opened at 3/16"	
Secondary Air: Fixed	
Control Board: N/A	
Blower/Fan: Off at all times	
Pre- Burn Activities	
Time Activity	
(min.)	
45 Stirred the Coad Bed	
90 Leveled the Coal Bed and activate (door was left ajar 1/4" open) for 30 seconds.	
The whole manipulation lasted 55 seconds	
	_
	_
Start-Up Procedure	_
Loading of fuel, sec. : Loaded by 50 seconds	
Fuel-loading door : Left ajar at 1/4" for 90 seconds	
Primary air: Fully open the first 5 minutes. Abruptly closed (3/16") at 5 minutes.	_
Secondary air: Fixed	_
Control board: N/A	_
Blower / fan: Off at all times	_
Other Notes	_
Coal Bed range: 2.8-3.4 lb	
	_
	_
	_
	_

+ FFF 03/26/12

		1		VERSION	1.2	2/5/2010	1					
Manufacturer:												
Model:	XTD 1.9	ī.										
Date:	25-08-2011											
Run:	4-Fan Confirmatio	n										
Control #:	G100456088											
Test Duration:	290							-				
1		Start	End		10 C							
E	Barometer (in.Hg):	29.7	29.7	21								
	N/////99//											
	Dry Bulb (F):	87	87									
	Humidity (%):	25	24									
							ieuw					
Blower turned on at 30 min-low	position.							1				
Moisture content of	124242622200	16.6528										
	Average	0.95	4.69	16.12	257.38	86.11	99.11	422.13	396.21	433.76	454.48	311.3
•	*	*	4.69	*	*	*	*	+22.10	*	*	*	
Elapsed	Weight				Flue	Room	Tunnel	Unit	Unit	Unit	Unit	Unit
Time	Remaining	CO	CO2	02	Gas	Temp	Dry Bulb	Тор	Back	R.Side	L.Side	Bottom
0	13.85	0.46	2.28	19.46	289.68	79.77	116 74	408.57	517.87	463.82	489.75	374.
10	13.10	0.61	4	17.2	255 60	83.78	101.53	405.06	481,22	411.58	459.55	369
20	12,43	0.45	9.54	11.74	245.91	82.25	99.08	382,21	436,64	369,30	424_36	358
30	11,23	0.69	10.85	10.02	318.87	82.34	104.43	445.74	413.16	370,93	410.54	341
40	9.69	0.44	9,93	11.13	368,49	85.06	108,76	572.88	271.88	408,67	429.58	327
50	8.31	0.43	7,58	13.35	374.70	87.95	111.01	620.78	292.25	436,46	460.54	315
60	7.28	0.6	6,37	14 58	343.53	87.33	108,79	604.16	306.98	445,41	485.36	310
70	6.56	0.6	6,79	14 35	315.82	85.88	105.88	553.58	320.16	437.79	400 00	306
80	5 84	0.59	7.5	13 73	303 31	87.59	104 17	520.16	340.48	437.98	494.15	301
90	5.15	0.66	6.19	14,57	303.76	88.64	103.37	508.04	343.64	444.96	501.14	298
100	4.52	0.84	5.31	15.58	288.50	87.74	103.37	495.71	377.03	451.48	507.12	293
110	4.52	0.7	5.84	15.58	270.85	88,17	100.22	495.71	512.47	454.96	499.90	295
110												
	3.62 3.16	0.37	7.4	14.24	263.47	88.92	99.56	446.90	323_63	462,80	493,73	293.
130		0.53	6 44	14.83	268 72	85.29	98.96	448.48	343 94	477.18	491.56	291.
140	2.61	0.42	6.04	14.91	269.92	87,30	98.74	459.77	365 79	492,52	498,57	293
150	2.15	0.82	4.55	16,19	267.17	84,69	98.59	459.08	373 78	507,07	503.07	293
160	1.91	1.08	4.2	16.32	253,94	84,62	97,15	440.60	353 75	498,90	501.28	297,
170	1.68	1.26	3.89	16.53	243 37	85,62	96.14	418.68	361.67	487.46	492.05	297.
180	1.44	1,42	3.62	16.67	235,93	84,19	95,38	400,47	417 32	479.87	480,74	299
190	1.25	1.42	3.46	16.83	231.51	84.55	95.07	385,71	491.74	471.92	469,84	303.1
200	1.07	1.22	3.25	17.2	224.36	84.54	94.34	371.30	481.49	463.72	459.15	303.
210	0,90	1,33	3,03	17 39	221.20	86,11	94,49	362,48	471.27	452 19	449.93	304
220	0.76	1,5	2.17	18.2	217.40	86,81	93,91	353 78	459.54	435 19	440,76	307.0
230	0.63	1.56	2.02	18.3	209.30	86.88	93,32	341,32	446.51	418_60	429.46	310
240	0,50	1.65	1.81	18.54	203.72	87.01	92,78	327,19	432.03	402 54	414.08	310
250	0.38	1.36	1.45	19_12	197.46	87.82	92 15	315 10	418.42	389 62	400,16	310
260	0.26	1.34	1.28	19 31	192.06	88.40	92 13	304 02	405 12	378 24	385.80	308
270	0.17	1.5	1.01	19.42	185.68	87,95	91.77	292 16	390,12	364,65	371.31	308
280	0.10	1.38	1.46	19.3	180,98	87.77	91.65	281.80	375.38	352 17	356 52	305 6
290	0.00	1.23	1.53	19.38	178 24	88 23	91.29	272.00	361.03	344,79	342.24	304

1													
Manu	facturer:	SRI											
IVIAITU		XTD 1.9				_							
		25-08-20	11										
		4-Fan Co											
-		G100456		-					1				
U		G100450	000										
							1						
427.21	82.50	82.51	85.35	468.71	82.36	82.32	85.63	0.02	0.000	0.00	403.55		
4 1.2 1			*	*		*	*		*	Visual		Change in	
DGM 1	DGM 1	DGM 1	Filter 1	DGM 2	DGM 2	DGM 2	Filter 2	Tunnel	Chimney	Smoke	Stove	Surface	Elaps
Reading	Inlet T	Outlet T	Temp	Reading	Inlet T	Outlet T	Temp	Velocity	Draft	Observed	Temp	Temp.	Tin
412,092	81.92	81.89	81.88	453.582	81.78	81.76	81.98	0.023			450,9	0	
413 145	82.10	82.01	84.89	454.640	81.93	81.91	84.84	0.023	·		425.4	-25.547	
414.185	82.18	82.09	85.38	<ul> <li>Annotation</li> </ul>	81.97	81.97	85.60	0.023			394.1	-56,766	1
415.202	82.25	82.17	85.60	458.708	82.04	82.05	85,92	0.023			396.4	-54.467	3
416 219	82.28	82.21	86.04	457.726	82.10	82.06	86.29	0.023			402.0	-48.885	4
417.264	82.41	82.33	86.58		82.20	82.22	86.74	0.023			425.0	-25.889	ŧ
418.302	82,40	82.35	86.76	459,804	82.18	82.18	87.04	0.023			430,5	-20.38	6
419.372	82.52	82,45	86 67		82 32	82 27	87.02	0.023			421.9	-29.016	-
420,418	82.56	82.49	86,54	461,905	82.35	82.29	86.85	0.023			418.8	-32.059	
421,460	82.52	82.54	86.42	462.955	82.39	82 32	86,70	0.023			419.3	-31.56	(
422.508	82.43	82.51	86.25	464.016	82.35	82.24	86.56	0.023			425.0	-25.859	10
423.545	82.40	82.46	86.04	465.052	82.29	82.22	86 22	0.023			445.7	-5.2	11
423.545	82.42	82.48	85.73	466.113	82.32	82.25	86.08	0.023			404.0	-46.876	12
425.642	82.47	82.51	85.65	467,133	82.32	82.37	85.93	0.023			410.5	-40.378	13
426.685	82.42	82.51	85,65	468,187	82.37	82.28	85.79	0.023			422.0	-28.914	14
427.735	82.42	82.49	85.53	469.222	82.34	82.31	85.72	0.023			427.4	-23.518	15
	62.49	82.49	85.55		82.34	82.34	85.68	0.023	2		418.3	-32,563	10
428,775	82.57	82.57	85.55	470.280 471.327	82.43	82.34	85.61	0.023			410.5	-39.349	17
						82.38	85.39	0.023			411.6	-35.351	18
430.870	82,54	82.62	85.28	472.363	82,44	7.6			2		415.6	-26.296	19
431,912	82,56 82,65	82 58 82 63	85.02	473.427	82,47	82 35 82 41	85.28 85.22	0.023			424.0	-35.137	20
		82,63	84.94 84.96	474.478	82,46	82.41 82.39	85.22	0.023			415.8	-35.137 -42.79	21
434.007	82,66			475.510	82,49	7.0					399.4	-42.79	22
435.055	82,67	82,65	84.92	476.551	82,54	82,46	85.19	0.023			399.4	-51.52	23
436.098	82.65	82.63	84.85	477.604	82.51	82.42	85.17	0.023			377.3	-73,602	24
437.137	82,66	82.72	84.79	478.652	82,60	82.56	85.14	0.023	6		366.8	-73.602 -84.139	25
438 180	82,67	82,72	84.76	479,683	82,58	82.51	85,15	0.023				-84.139 -94.585	
439.217	82.76	82,77	84.75	480.707	82,63	82.60	85.22	0.023			356.3		20
440 265	82.77	82,77	84.59	481.783	82,61	82.58	85.19	0.023	li		345.3	-105.63	27
441.314	82.75 82.88	82.83 82.90	84.48 84.39	482.818 483.854	82.70 82.79	82 69 82 78	85.03 85.01	0.023			334.3 324.9	-116.59 -126	28

- Hoghel 03/26/12

	Manu	facturer:		SBI				
		Model:		XTD 1.9				
		Date:		25-08-2011				
		Run:		4-Fan Confirma	ation			
	Project		£	G100456088				
	Test Dura			290				
Total Gas Vo	and the state of the second			29.227	Dit	ot Factor	0.82	
Total Gas Vo	the set of second se			29 125	C A	Contraction of the second second second	99 standar	d
Average Baron	· ·			29.7			al. Factor for	
Average baro			ht	28.56		0.04 01 02	I. Factor to	S-Type
		lar Weig		0,915		_		
Calibration Fa			1.2					
Calibration Fa	INTERNAL DISCOURSES.	Charles in the second second		1.0000				
Calibration Fa	ctor (DGI	vi #2):	(4) 1/0.	0.9960				
			(1) VS:	0.0287				
			(2) VS:	0.0288			Filter	Filler
					DOW		Face	Face
DGM 1	DGM 1	DGM 1	DGM 2		DGM 2	Tunnel	Velocity	Velocity
Reading	Inlet T 81.9	Outlet T	Reading 453,582	Inlet T 81.781248	Outlet T 81.758	Dry Bulb 116.74	DGM 1	DGM 2
412.092		82.0	·		81,909	101.53	8.77	8.78
413.145	82.1			81.929632			8.66	8.6
414.185	82.2	82.1		81.971338		99,079		17. m .
415.202	82.2		456.708	82.03575	82.045		8.47	8.5
416.219	82.3		457.726	82.099349	82.058		8.47	8.4
417.264	82.4	82.3		82.195643	82.221	111.01	8.70	8,6
418.302	82.4		459.804	82.180898	82.178		8,64	8.6
419.372	82.5		460.898	82.321816	82.27	105.88	8.91	
420.418	82.6		461.905	82.348315	82.286	104.17	8.71	
421.460	82.5		462.955	82.390194	82.316	103.37	8.67	8.7
422.508	82.4		464.016	82.351067	82.236	101.97	8.73	8.80
423.545	82.4		465.052	82.289862	82.223	100.22	8.63	8.59
424.596	82.4		466.113	82.321002	82.246	99,561	8.75	8.80
425.642	82.5		467.133	82.374472	82.37	98.964	8.71	8.46
426.685	82.4		468.187	82.327256	82.284	98.739	8.68	8.74
427.735	82.5		469.222	82.344883	82.306	98.59	8.74	8.58
428.775	82.5		470.280	82.362811	82.345		8.66	8.78
429.824	82.6		471.327	82.433036	82.414	96.144	8.73	8,68
430.870	82.5		472.363	82.43575	82.377		8.71	8.59
431.912	82.6	82.6	473.427	82.471214	82.353	95.075	8.67	8.82
432.959	82.6	82.6	474.478	82.461684	82,405	94.343	8.71	8.72
434.007	82.7	82.6	475.510	82.486717	82.391	94.489	8.72	8.56
435,055	82.7	82.6	476,551	82.536783	82.463	93,907	8.72	8.63
436.098	82.6	82.6	477.604	82.512443	82.42	93,321	8.68	8.73
437.137	82.7	82.7	478.652	82.604884	82.565	92.778	8.65	8,69
438.180	82.7	82.7	479.683	82.584228	82.508	92.153	8.68	8.5
439.217	82.8	82.8	480.707	82.628727	82.598	92.134	8.63	8.49
440.265	82.8	82.8	481.783	82.613875	82.576	91.769	8.72	8.92
441.314	82.8	82.8	482.818	82.701504	82.687	91.648	8.73	8.58
442.357	82.9		483,854	82,790418	82.782	91.293	8.68	8.5

- + Kypes 03/26/12

	Proportio	nal Rate	Calculatio	ns	(EPA Formu	las from P	R5G)	
	Stack are	ea (ff2)	0.3491		Man	ufacturer:	SBI	
Wood	moisture (		16.653				XTD 1.9	
	Veight (Ibs		13.9				25-08-20	11
	ate (Dry k		1.087				4-Fan Co	
Burn K	ale (DIY K	g/m).	1.007			Kuli.	4-ran 60	minado
inal Ter	nperature	(DGM #1	) Degrees	Rankin:	542.503			
	nperature							
	innel Tem	An Annual State ( 1998) When	A second s		559.113			
	innel Velo	and the state of the state of the	the state of the local designs of the		7.812183			
	ndardized		the state of the second second	1 T/,	-147.18			
		Average						
		Inlet +	Inlet +		1000	102		
		Outlet	Outlet	99.94	99.94	#1	#2	
Tunnel	Tunnel	Temp.	Temp.			dDGM	dDGM	
Velocity	Velocity	Meter 1	Meter 2	0.04	000	Vol.Std.	Vol.Std.	Time
Delta-P 0.023	Ft/Sec 7,934	Deg. R 541.9	Deg. R 541.8	PR1	PR2	(ft3)	(ft3)	Time O
0.023	7.834	541.9		101.20	101.65	1.018	1.019	10
		542.1	542.0		99.89	1.005	1.003	20
0.023	7.812 7.849	542.1	542.0	99.72	99.89	0.983	0.988	30
0.023	7.849	542.2	542.0		98.41	0.983	0.980	40
		542.2	542.1	98.33	100.42	1.009	0.980	50
0.023	7.895	542.4		101.22	100.42	1.009	1.002	60
0.023	7.880	542.4 542.5		100.34	100.62	1.003	1.053	70
0.023	7.859	542.5 542.5		103,15	96,91	1.033	0.969	80
0.023	7.848	542.5	542.3	100.88	100.97	1.006	1.010	90
0.023	7.832	542.5	542.4	100.22	100.97	1.000	1.010	100
0.023	7.820	542.5	542.3	99,48	99,36	1.002	0.997	110
0.023	7.820	542.4	542.3	100,76	101.70	1.002	1.021	120
0.023	7.815	542.5	542.5	100.78	97.70	1.015	0.981	130
0.023	7.810	542.5	542.4	99.92	100.95	1.007	1.014	140
0.023	7.809	542.5	542.3	100.57	99.11	1.014	0.996	150
0.023	7.799	542.5	542.5	99.48	101.18	1.004	1.018	160
0.023	7.792	542.6	542.4	100.23	100.02	1.013	1.007	170
0.023	7.786	542.6	542.4	99.88	98.91	1.010	0.997	180
0.023	7.784	542.6	542.4	99.47	101.55	1.006	1.024	190
0.023	7.779	542.6	542.4	99.87	100.24	1.011	1.011	200
0.023	7.780	542.6	542.4	99.98	98.44	1.012	0,993	210
0.023	7.776	542.0	542.5	99,92	99.23	1.012	1.001	220
0.023	7.772	542.6	542.5	99.40	100.33	1.007	1.013	230
0.023	7.768	542.7	542.6	98,96	99.78	1.003	1.008	240
0.023	7,764	542.7	542.5	99.28	98.12	1.007	0.992	250
0.023	7.763	542.8	542.6	98.70	97.44	1.001	0.985	260
0.023	7.761	542.8	542.6	99.71	102.35	1.012	1.035	270
0.023	7.760	542.8	542.6		98.42	1.012	0,995	280
U.VEU	11100	542.9	542.8	99.17	98.47	1.007	0.996	290

- Thighel 03/26/12

		Intertek Testing Service	5				
		SFBA EPA ADJUSTED	EMISSION	RESULT	3	ļ	
Manufacturer		SBI			RESUL	rs	
the second s		XTD 1.9				·····	
		25-08-2011			Aerage Adjusted Emin	asions Rate:	4,56
		4-Fan Confirmation		A	verage Unadjusted En		3.03
Proi		G100456088				(Dry kg/hr):	1.05
Test Duration (Min		290				1-11-0-11	1.000.000
Test Duration (He		4.83					
rest boralish (n	ouroy.					1	
				BARO	METRIC PRESSU	RE	
				0/11/0		Average	29
TEMPERATUR	E FAC	TORS				Start:	29
TERR ERVIOR	L L L M	DGM #1:	0.9733			End:	29
		DGM #2:	0.9736			ter rist.	
		DOM #2.	0.0700	DRY GA	S METER VALUES		
VOLUMES S	AMPL	ED		Price OF	DGM #1	Final:	442.38
i c some o c		DGM #1:	29,239		0.01111	Initial:	412.09
		DGM #2:	29,138			1000000	
					DGM #2	Final:	483.85
TOTAL TUN	NEL V	OLUME (scf):	42683			Initial:	453.58
SAMPLE RA	TIOO			TEMP		DANKINI	
and the system is the year of the	A further with	Tenin 4	4450.0	TEMP	ERATURES (DEG	DGM #1:	542.50
	10000002	Train 1:	1459.8			and the state of a state of the	542.50
5	ample	Train 2:	1464.9			DGM #2:	542.34
TOTAL EMIS	SION	s		CALIB	RATION FACTOR	s	
Sample	2-1110-011	The second	14.31	OF THE P		DGM #1:	1.000
Sample			14.94			DGM #2:	0.996
797404 0455	1	Ave:	14.62				
EMISSION R	ATES		1.	TUNN	EL FLOW RATE:		147.2
Sample Tr			2.96	+ ((*-))+* (+ 1)*	PARTICULATE	CATCH (n	
Sample Tr			3.09			le Train 1:	S.
		Ave:	3.03			Filters	9.
ADJUSTED	EMISS					Probe	0.
Sample Tr	ain 1 (	a/hr):	4.48		1	Total	9.
Sample Tr			4.64		Samp	e Train 2:	
		Ave:	4.56			Filters	9.
	DEV	IATION:	1.80%			Probe	0.
						Total	10.
If deviation is	great	er than 7.5% due to low	particulate	catch		-	
	(1) The (1 - 1) is (1) is (1)	ates shall not differ by 7.	NGUL0034424687233 124	and an			
		erage emission rate limit		(5g-3)			
Use the follow	wing:						
Cotoballa			4.000				
Catalytic unit			4.02%				
7.5% of 4.1 g	Inc						
Non catalytic	units		2.19%				
7.5% of 7.5 g							

03/26/12

Before 87	After 87	29.70	29.70	25	24	0	0
	0.61	Before	After	Before	After	Before	After
		Bar Pressure			umidity		
						1	
Water C							
	DGM 2:	82.34		-			
	DGM 1:	82.50					
				-			
				-			
ge in stov	e temp.	0					
an in etou	o tomo:	0					
rage Koo	m temp:	80,11					
All second second second							
	**************************************						
		the second secon					
Į	and the second se			· · · · · · · · · · · · · · · · · · ·			
				-			
REPORT	IDATA					1	
	Moisture ck Static (r Barc ge in stov ge in stov Bum d Emissi Sys Sys Devi Filte Filte Tu Water C	Date: Project: Model: Moisture (Dry): ck Static (neg): Barometer: erage Room Temp: ge in stove temp: ge in stove temp: Bum Rate: ed Ernission Rate: System 1: System 2: Deviation: Filter 1: Filter 2: Tunnel: DGM 1;	Client:         SBI           Run: 4-Fan Confirmation         Date:         25-08-2011           Project:         G100456088         Model:         XTD 1.9           Moisture (Dry):         19.98         Static (neg):         0.085           Barometer:         29.7         29.7           prage Room Temp:         86.11         Static (neg):         0           ge in stove temp:         0         0         Static (neg):         0           Burn Rate:         1.087         4.562         System 1:         4.479           System 1:         4.479         System 2:         4.644         Deviation:         1.80%           Filter 1:         85.35         Filter 1:         85.35         Filter 2:         85.63           Tunnel:         99.11         DGM 1:         82.50         DGM 2:         82.34           Water Collected:	Client:         SBI           Run: 4-Fan Confirmation         Date:         25-08-2011           Project:         G100456088         Model:         XTD 1.9           Moisture (Dry):         19.98         Static (neg):         0.085           Barometer:         29.7         29.7           prage Room Temp:         86.11         0           ge in stove temp:         0         0           Burn Rate:         1.087         0           ed Emission Rate:         4.562         System 1:         4.479           System 1:         4.479         System 2:         4.644           Deviation:         1.80%         Filter 1:         85.35           Filter 1:         85.35         5           Junnel:         99.11         DGM 1:         82.50           DGM 1:         82.50         DGM 2:         82.34           Water Collected:	Client:         SBI           Run: 4-Fan Confirmation         Date:         25-08-2011           Project:         G100456088         Model:         XTD 1.9           Moisture (Dry):         19.98         Static (neg):         0.085           Barometer:         29.7         29.7           prage Room Temp:         86.11         86.11           ge in stove temp:         0         0           Burn Rate:         1.087         9           ed Emission Rate:         4.562         System 1:         4.479           System 1:         4.479         System 2:         4.644           Deviation:         1.80%         Filter 1:         85.35           Filter 1:         85.35         5           JogM 1:         82.50         DGM 1:         82.50           DGM 2:         82.34         Water Collected:         82.34	Client:       SBI         Run: 4-Fan Confirmation       Date:       25-08-2011         Project:       G100456088       Model:       XTD 1.9         Moisture (Dry):       19.98       Static (neg):       0.085         Barometer:       29.7       Static (neg):       0         ge in stove temp:       0       0         Bum Rate:       1.087       System 1:       4.479         System 1:       4.479       System 2:       4.644         Deviation:       1.80%       Filter 1:       85.35         Filter 1:       85.35       Filter 2:       85.63         Tunnel:       99.11       DGM 1:       82.50         DGM 1:       82.50       DGM 2:       82.34         Water Collected:	Client:       SBI         Run: 4-Fan Confirmation         Date:       25-08-2011         Project:       G100456088         Model:       XTD 1.9         Moisture (Dry):       19.98         ck Static (neg):       0.085         Barometer:       29.7         prage Room Temp:       86.11         ge in stove temp:       0         Burn Rate:       1.087         ed Emission Rate:       4.562         System 1:       4.479         System 2:       4.644         Deviation:       1.80%         Filter 1:       85.35         Filter 2:       85.63         Tunnel:       99.11         DGM 1:       82.50         DGM 2:       82.34         Water Collected:       82.34

1/25/12

Flue	Room	Tunnel	Unit	Unit	Unit	Unit	Unit	Scale
Gas	Temp	Dry Bulb	Тор	Back	R.Side	L.Side	Bottom	weight
529.73	83.96	153.14	454.65	470.50	434.27	453.61	390.06	12.27
474.43	88.47	131.29	726.59	321.31	502.54	489.77	374.24	9.28
391.57	89.78	117.30	649.66	340.56	517.24	514.42	376.12	7.82
403.34	92.11	117.89	671.78	495.58	530.29	534.92	380.38	6.33
405.40	90.90	117.93	697.25	550.07	538.19	553.88	381.67	4.85
354.64	89.77	111.55	654.29	518.49	546.37	565.62	379.22	3.97
340.81	88.98	110.66	608.90	474.93	546.45	564.71	381.71	3.30
293.24	90.46	105.10	529.82	575.42	519.39	546.12	382.80	3.09
269.81	85.41	102.23	464.51	545.69	493.36	519.83	376.96	3.01
253.08	84.32	99.38	424.35	525.82	470.31	496.75	372.55	2.82

03/25/12

	TUNNEL	TUNNEL	SQUARE	Static Pressure:
	VELOCITY	TEMP	ROOT	
A CENTER	0.028	124	0.1658	
<b>B</b> CENTER	0.028	121	0.1658	
A1	0.025	122	0.1581	PITOT
A2	0.028	122	0.1658	CONSTANT
A3	0.025	122	0.1581	<u>N</u>
A4	0.018	118	0.1323	
B1	0.023	120	0.1500	
B2	0.025	121	0.1581	
B3	0.023	122	0.1500	
B4	0.020	118	0.1414	
AVERAGE	0.024	121.08	0.1517	
unnel Diameter (	(in) <sup>.</sup>	8	1	

E&E Tunnel Traverse Worksheet

PITOT CONSTANT 0.9150

Tunnel Diameter (in): Tunnel Area (ft2) **Tunnel Static Pressure** 

- 1/1gh J 03/26/12

### **E&E FUEL LOAD DATA SHEET**

		Test Load Weight:				
			Lower	Ideal	Upper	
Firebox Volume: 2.14	cu. ft	L	13.48	14.98	16.48	
Load Volume: 0.0000	cu. ft		Loadinę	g Density:	5.771	lbs./ft3
Number of Spacers: VERSION 1.	2		Load 2/5/2010	d Density:	#DIV/0!	lbs./ft3

Piece Size:					Weight	М	eter Moistu	re Content
Thick	x	Wide	х	Length	lbs		rrected %	
	2		4	12	1.15	21.3	19.5	22.5
	2		4	12	1.15	21.7	19	21.7
	2		4	12	1.15	21.3	19.2	21.1
	2		4	12	1.15	21	19.8	21.9
	2		4	16	1.35	21.6	18.9	22.1
	2		4	16	1.30	20.00	17.90	19.90
	2		4	16	1.70	21.60	19.40	21.50
	2		4	16	1.70	22.40	17.90	23.60
	2		4	16	1.70	24.30	21.20	23.90

two pin: (dry)

Test Load Weigh 12.35 lbs.

Dry Weigh

20.90

4.63 kg.

17.29

Average Pretest Moisture Content: % Wet:

Dry: 21.13

1/mg/26/12

		Lower	Ideal	Upper	
Firebox Volume: 2.14	cu. ft	13.48	14.98	16.48	
Load Volume: 0.0651	cu. ft	Loadin	g Density:	6.495	lbs./ft3
Number of Spacers: 20		Loa	d Density:	213.504	lbs./ft3
			,		

	Piece Size:		Weight		Moisture C	
Thick x	Wide x	Length	lbs	Dry Uncorrected %		
2	4	15.75	1.60	20.00	19.80	19.40
2	4	15.75	1.60	19.20	20.00	18.90
2	4	15.75	1.75	21.90	21.10	23.60
4	4	15.75	3.65	19.20	19.50	18.70
4	4	15.75	3.20	19.70	19.50	19.20
		Spacers	2.10			
·						

Test Load Wei	<b>gh</b> 13.90 lbs.	Dry Weigh	5.25	kg.
Dry: 19.98	Average Moisture	<b>Content: %</b> 19.98	Wet:	16.65
21.13	Pre-test moisture	<b>content: %</b> 21.13	Wet:	17.45
Coal Bed Rang	<b>je:</b> 2.8 lbs. to	o 3.4 Ibs.	20% to 25	% of test load

03/26/12 -

Run 5

 $\bigcirc$ 



#### Run Notes EPA Methods 28 and 5G-3

PROJECT / TES	T INFORMATION		Appl	iance	Information
Project Number:	G100456088				1 - Catalytic
Manufacturer:	SBI		Appliance	2	2 - Non - Catalytic
Model:	XTD 1.9		Type:	4	3 - Pellet
Sample ID Number:	MTL1108221414-001	SBL			4 - Hydronic
Test Date:	26-Aug-11	100EL XTD 19 CAT 4 26/08/2011	Firebox Volume, ft <sup>3</sup> :	2.14	N/A for pellet type
Test Run Number:	5		Convection		1 - No Fan
Date tunnel cleaned:	8/18/2011			2	2 - Fan Optional
Purpose of Test	Cat 4		Blower		3 - Fan Standard
		10000 TO 10000			

Primary Air: Fully open
Secondary Air: Fixed
Control Board: N/A
Blower/Fan: Off the first 30 minutes and turned On-Low after 30 minutes for the reminder of the test
Pre- Burn Activities
Time Activity
(min.) Closed the primary air when the scale indicated 8.00 pounds
45 Stirred the Coad Bed
70 Added 1.6 lb of fuel consisting of 2x4 pieces of 4" of length
90 Leveled the Coal Bed and activated - the door was left ajar at 1/4" for 30 seconds.
This manipulation lasted 55 seconds.
Start-Up Procedure
_oading of fuel, sec. : Loaded by 40 seconds
Fuel-loading door : Left ajar at 1/4" for 60 seconds
Primary air: Fully open.
Secondary air: Fixed
Control board: <u>N/A</u>
Blower / fan: Off the first 30 minutes and turned On-Low after 30 minutes for the reminder of the test
Other Notes
Coal Bed range: 2.9-3.5 lb

- Hayta J 03/26/12

				VERSION	1.2	2/5/2010	1					
Manufacturer.	SBI											
Model	XTD 1.9											
Date:	26-08-2011											
Run:	5						8					
Control #:	G100456088						1					
Test Duration:	120						S					
		Start	End									
	Barometer (in.Hg):	29.97	29.7									
	Dry Bulb (F):	87	87				-					
	Humidity (%):	23	23									
*Blower turned on at 30 min-lov	w position											
Moisture content of		16,2479										
	Average	0.55	6.10	13.67	507.56	84,79	144.16	637.50	644.73	571.39	606.49	415.93
•	•			*	*	*		*			*	
Elapsed	Weight				Flue	Room	Tunnel	Unit	Unit	Unit	Unit	Unit
Time		CO	CO2	02	Gas	Temp	Dry Bulb	Тор	Back	R.Side	L.Side	Bottom
0	14.05	0,31	13,14	6,93	656.4	78.8	174.0	715.3	562.1	514.0	546.0	453.6
10	11.28	0.21	9,41	10,47	659.3	81.3	175,7	814.0	604.5	537,1	570,4	446,9
20	8.64	0.23	9.59	10,78	600_8	84.5	162 <sub>.</sub> B	793.6	635.8	544,2	598,0	433,3
30	6.81	0,18	9.63	10,15	595 5	85.4	161,9	744.5	660.7	535,2	624,8	423.6
40	5.25	0,19	8,32	11,58	580,5	84 1	157 B	777.3	681.1	578.7	647.5	414.2
50	3.68	0.24	5.49	14,38	548.9	86.1	151.8	740.1	700_4	802.7	652,4	407.8
60	2.37	0,3	5,82	14 3	493.9	85.0	141_1	664.8	705.3	628,8	650,5	
70	1.49	0.62	4.16	15.49	459.3	87.7	133.2	583_0	692.1	618,1	639.2	403 5
80	8	0.75	3,81	15,77	437.9	89_4	130_0	546_5	674.5	606.7	627.1	406.0
90	a	0,92	3,15	16,35		86.7	125.3	511.1	648 1	579,8	606,0	405 0
100		1	2.88	16.57		84.7	121.B	481_3	620.3	569,0	586,4	403,9
110	· · · · · · · · · · · · · · · · · · ·	1.05	2,26	17,12		84.7	119.4	458 2	598 4	557,0	568,1	401,7
120	0.00	1.1	1,59	17.77	378.6	83.9	119.0	457.8	598.2	556.9	567,9	401.9

- Hughel 03/26/12

						1							
Manu	facturer.	SBI											
	Model:	XTD 1.9											
	Date:	26-08-20	11										
	Run:	5											
(	Control #	G100456	088										
						S							
448.55	81.12		85.41	490.06	80.82	80.76	85.87	0.02	0.000	0,00		1000	
•	•	1. M.C. 19			*		*	•	•	Visual		Change in	
DGM 1	DGM 1	DGM 1	Filter 1	DGM 2	DGM 2	DGM 2	Filter 2		Chimney	Smoke	Stove	Surface	Elapse
Reading	Inlet T	Outlet T	Temp	Reading	Inlet T	Outlet T	Temp	Velocity	Draft	Observed	Temp	Temp.	Tin
442.376	80.0	79.7	88.9	483,865	79.7	79.7	89.5	0.023			558.2	0	
443.410	80.3	79.9	88,1	484.911	79.9	79.9	88,9	0,023			594.6	36,368	1
444.398	80.6	80.2	86.2	485.908	80,1	80.2	80.6	0.023			601.0	42.784	2
445.395	80,9	80.5	85.3	486.905	80,4	80_4	82.2	0.023			597.7	39.528	3
446.440	80,9	80,6	84.5	487.941	80.5	80_6	86,6	0.023			619.7	61,533	4
447.505	81.0	80.8	83.5	489,010	80.6	80_6	88.4	0.023			620.7	62.472	5
448.545	81.2	B1_0	82.4	490.048	81.0	80.9	86.1	0.023			611.0	52.806	e
449.555	81.4	81,2	81.5	491.061	81.2	81.0	83.7	0.023			587.2	28.949	7
450.603	81,5	81.3	85.4	492.093	81,3	81.1	85.6	0.023			572.2	13,953	8
451.652	81,6	81,4	86.3	493,153	81,4	81.3	86.4	0.023			550.0	-8.2094	9
452.710	81.7	81.5	86.1	494.209	81.4	81.3	86.3	0.023			532.2	-26.031	10
453.775	81.7	81.7	86.1	495.270	81,6	81,4	86.0	0.023			516.7	-41.506	11
454.850	81.7	81.6	86.1	496,350	81.6	81.4	86.0	0.023			516.5	-41.678	12

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	Manu	facturer:		SBI					
	wante	Model:		XTD 1.9					
		Date:		26-08-2011					
		Run		5					
Project #			G100456088						
	Test Dura			120					
Total Gas Vo		22.0.75-CA		12,133	Pit	ot Factor	0.82		
Total Gas Vo				12.099			99 standar	d	
Average Baron	about the second second	a service a state of the		29.835			84 or Cal. Factor for S-Typ		
riverage baro			ht	28.56		0.010100		S ()pol	
	Molecular Weigh Pitot Correction			0.9616					
Calibration Fa	and a start way	Sec. 6 (1997)	1	1,0000					
Calibration Fa				0.9960					
oundration i u	0.01 (0.0.		(1) VS:	0.0697		· · · · · · · · · · · · · · · · · · ·			
			(2) VS:	0.0699			Filter	Filter	
			(-/ •••				Face	Face	
DGM 1	DGM 1	DGM 1	DGM 2	DGM 2	DGM 2	Tunnel	Velocity	Velocity	
Reading	Inlet T	Outlet T	Reading	Infet T	Outlet T	Dry Bulb	DGM 1	DGM 2	
442.376	80.0	79.7	483,865	79.664485	79.691	174.04			
443.410	80,3	79.9	484.911	79.891642	79.912	175.7	8.69	8.75	
444.398	80.6	80.2	485.908	80.119421	80.202	162.81	8.29	8,34	
445.395	80.9	80.5	486,905	80.373522	80.448	161,93	8.37	8.34	
446.440	80.9	80.6	487.941	80.522855	80.561	157.8	8.77	8,66	
447.505	81.0	80.8	489.010	80.64603	80.605	151.82.	8.93	8,94	
448.545	81.2	81.0	490.048	80.963026	80,879	141.13	8.72	8.67	
449.555	81.4	81.2	491.061	81.18308	81.011	133.24	8.47	8.46	
450,603	81.5	81.3	492.093	81,259849	81.104	129.96	8.78	8.6	
451.652	81.6	81.4	493.153	81.408024	81.255	125.33	8.79	8.8	
452.710	81.7	81.5	494.209	81.442825	81.323	121.84	8.86	8.8	
453.775	81.7	81.7	495.270	81,596558	81.45	119.4	8.92	8.85	
454,850	81.7	81.6	496.350	81,565239	81.42	119.03	9.00	9.01	

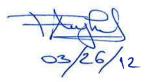
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	Proportio	nal Rate	Calculatio	ons	(EPA Form	ulas from F	PR5G)	
	Stack are	ea (ft2):	0.3491		Mar	SBI		
Wood	moisture (	% wet):	16.248			Model:	XTD 1.9	
	Veight (lbs		14.05				26-08-20	11
	ate (Dry k		2.669			Run:		
							-	
Final Ter	nperature	(DGM #1	) Dearee	s Rankin:	541.000			
	nperature							
	unnel Terr				604,156			
Final Tunnel Velocity (feet per second):					8.513885			
	indardized				149.12			
	201220222222222222222222222222222222222				and the second s			
		Average	Average					
		Inlet +	inlet +					
		Outlet	Outlet	99.75	99.75	#1	#2	
Tunnel	Tunnel	Temp.	Temp.			dDGM	dDGM	
Velocity	Velocity	Meter 1	Meter 2			Vol.Std.	Vol.Std.	
Delta-P	Ft/Sec	Deg. R	Deg. R	PR1	PR2	(ft3)	(ft3)	Time
0.023	8.723	539.9	539,7					0
0.023	8.735	540.1	539.9	102.21	103.30	1.008	1.016	10
0.023	8,645	540.4	540.2	96.61	97.41	0.962	0.968	20
0.023	8.639	540.7	540.4	97.37	97.30	0.970	0.967	30
0.023	8,611	540.8	540.5	101.70	100.74	1.017	1.005	40
0.023	8.569	540.9	540.6	103.12	103.43	1.036	1,036	50
0.023	8.494	541.1	540,9	99.78	99,50	1,012	1.006	60
0.023	8,438	541.3	541.1	96.23	96.43	0.982	0.981	70
0.023	8.414	541.4	541.2	99,56	97.95	1.019	1.000	80
0.023	8.381	541.5	541.3	99.24	100.19	1.019	1.026	90
0.023	8.356	541.6	541.4	99.77	99.50	1.028	1.022	100
0.023	8.339	541.7	541.5	100.21	99.74	1.035	1.027 :	110
0.023	8.336	541.7	541.5	101.13	101.50	1.045	1.045	120

03/26/12



		Intertek Testing Services	5				
		SFBA EPA ADJUSTED	EMISSION F	RESULTS			
Manufacturer.		SBI			RESULT	S	
Manuacturer.		XTD 1.9			RECOLI	Č	
		26-08-2011	i	Ave	rage Adjusted Emis	sions Rate	2.87
	Run:	Construction and Construction of Construction			age Unadjusted Em		1.73
		G100456088		Avoid	Burn Rate		2.67
Test Duration (	A CONTRACTOR OF A CONTRACTOR O	an and a			Burrrate	(21) (gran)	
Test Duration	Contract Contractor						
1 OUT D'UTURIO							
		,		BAROME	TRIC PRESSU	26	
1				BAROME		Average:	29.83
TEMPERA	TURE FAC	TORC		-		Start:	29.9
I EIVIPERA	TUREFAU	DGM #1:	0.9760			End:	29.
		DGM #1:	0.9764			LIG.	20.
		DGIVI#2.	0.9704	DPV CASA	METER VALUES		
VOLUME	ES SAMP	ED		DRT GAS I	DGM #1	Final:	454.8
VOLOWIE	LO O/NIF	DGM #1:	12.140		50M #1	Initial:	442.37
		DGM #2:	12.107	0		These.	
		DOM NE.	12.101		DGM #2	Final:	496.3
TOTAL T	UNNEL	VOLUME (scf):	17894			Initial:	483.86
CAMPLE	RATIOS			TEMPER	ATURES (DEG.		
SAMPLE		e Train 1:	1474.0	TEMPER		DGM #1:	541.00
		e Train 2:	1474.0			DGM #1:	540.79
	Sample	a frain 2:	14/0.1			DGIVI #2.	540.78
TOTAL E	MISSION	IS		CALIBRA	TION FACTORS	S	
Sam	ple Train	1 (g);	3.54			DGM #1:	1.000
	ple Train		3.40	111		DGM #2:	0.996
	Alcologie Instant	Ave:	3.47				
EMISSIC	N RATES	3		TUNNEL	FLOW RATE:		149.1
Sampl	e Train 1	(g/hr):	1.77		PARTICULATE	CATCH (n	ng)
Sampl	e Train 2	(g/hr):	1.70		Sample	e Train 1:	
		Ave:	1.73			Filters	1.
ADJUST	ED EMIS	SION RATES				Probe	0.
Sampl	e Train 1	(g/hr):	2.92			Total	2.
Sampl	e Train 2	(g/hr):	2.83		Sample	e Train 2:	
		Ave:	2.87			Filters	1.
-	DE\	/IATION:	1.65%			Probe	0.
						Total	2.
If deviation	on is grea	ter than 7.5% due to low	particulate c	atch			
		rates shall not differ by 7.					
of the we	ighted av	erage emission rate limit	(4.1 or 7.5)	(5g-3)			
Use the f	following:						
Catalytic	unite		2.32%				
7.5% of 4			2.3270				
and the second s	lytic units		1.27%				
7.5% of 7	1.5 g/hr	1					



					-			
	REPORT	DATA						
					1			
		Client:	SBI					
		Run:	5					
		Date:	26-08-2011					
	-	Project:	G100456088					
		Model:	XTD 1.9					
Fuel	Moisture (	Dry)	19.4					
Stac	k Static (n	eg):	0.075					
	Baro	meter:	29.835			1		
Ave	rage Roor	m Temp:	84.79				1	
		= 10						
					1		1	
Chan	ge in stove	e temp:	0		1			
0.0241240							1	
	Burn F	tate:	2.669					
Adjuste	ed Emissio	on Rate:	2.874					
		em 1:	2.922		-			
		em 2:	2.827					
	Devia		1.65%		1			
	Filter	r 1:	85.41		1			
	Filte	12:	85.87					
	Tur	nnel:	144.16					
		DGM 1:	81.00		1			
		DGM 2:	80.79		1			
	Mator C	ollected:						
	vvale u				1			
	vvalei G							
		Temp	Bar Pressure		Relative H	umidity	Air Velo	city
	Room	Temp	Bar Pressure Before	After	Relative Hi Before	umidity After	Air Velo Before	city After

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Flue	Room	Tunnel	Unit	Unit	Unit	Unit	Unit	Scale
Gas	Temp	Dry Bulb	Тор	Back	R.Side	L.Side	Bottom	weight
512.93	73.55	183.08	320.54	124.12	147.54	119.78	70.18	14.56
664.48	74.46	176.21	671.06	219.64	221.18	204.59	108.24	11.38
694.47	82.97	182.70	819.07	184.36	350.31	316.80	181.11	8.23
602.06	88.56	160.17	769.42	322.71	497.90	424.33	278.21	5.98
541.43	89.48	147.53	701.57	480.67	568.46	497.13	355.82	4.53
532.83	87.49	145.68	686.40	534.40	600.31	547.82	413.36	3.18
445.13	88.34	188.96	590.11	586.29	576.50	563.51	439.80	4.77
457.34	79.43	133.83	564.30	589.27	556.16	551.67	444.24	3.76
439.63	81.31	128.86	538.24	584.95	540.92	543.57	447.41	2.98

03/26/12

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VERSION 1.2

#### 2/5/2010

TUNNEL TUNNEL SQUARE

### E&E Tunnel Traverse Worksheet

	VELOCITY	TEMP	ROOT
A CENTER	0.022	161	0.1483
B CENTER	0.023	162	0.1500
A1	0.020	160	0.1414
A2	0.023	160	0.1500
A3	0.023	160	0.1500
A4	0.018	157	0.1323
B1	0.020	160	0.1414
B2	0.023	160	0.1500
B3	0.023	160	0.1500
B4	0.018	157	0.1323
AVERAGE	0.02095	159.94	0.1434

Static Pressure:

#### PITOT CONSTANT 0.9616

Tunnel Diameter (in): Tunnel Area (ft2) **Tunnel Static Pressure** 

8
0.349066
-0.075

26/12

# **E&E FUEL LOAD DATA SHEET**

	Test Load Weight:				
	Lower Ideal Upper				
Firebox Volume: 2.14 cu. ft	13.48 14.98 16.48				
Load Volume: 0.0651 cu. ft	Loading Density: 6.145	lbs./ft3			
Number of Spacers: 20 VERSION 1.2	Load Density: 201.984 1 2/5/2010	lbs./ft3			

	Piece Size:		Weight	Meter I	Meter Moisture Content			
Thick x	Wide x	Length	lbs	Dry	Dry Uncorrected %			
2	4	12	1.2	20.2	20	20.3		
2	4	12	1.25	21.2	20.8	21.3		
2	4	12	1.25	21.1	19.7	21.4		
2	4	12	1.3	21.4	20.3	21.2		
2	4	16	1.65	21.3	19.8	21.6		
2	4	16	1.65	20.30	19.50	21.30		
2	4	16	1.65	22.00	21.20	20.00		
2	4	16	1.60	22.10	19.90	21.40		
2	4	16	1.60	22.00	19.30	21.20		

Test Load Weigh 13.15 lbs.

Dry Weigh 4.93

Dry: 20.85

Average Pretest Moisture Content: %

20.90

two pin: (dry)

Wet:

17.29

kg.

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VERSION 1.2

2/5/2010

### **E&E FUEL LOAD DATA SHEET**

			Test Load Weight:		
		Lower	Ideal	Upper	
Firebox Volume: 2.13	cu. ft	13.42	14.91	16.40	
Load Volume: 0.0000	cu. ft	Loadir	ng Density:	6.596	lbs./ft3
Number of Spacers:		Loa	ad Density:	#DIV/0!	lbs./ft3

Piece Size:		Weight	Meter Moisture Content			
Thick x	Wide x	Length	lbs	Dry Uncorrected %		
2	4	15.75	1.45	19.20	19.90	19.00
2	4	15.75	1.55	19.30	19.50	19.00
2	4	15.75	1.65	19.10	19.20	19.20
4	4	15.75	3.65	19.50	21.10	18.60
4	4	<b>15.75</b>	3.35	19.70	19.50	19.20
		Spacers	2.40			

Test Load Weigh 14.05 Ibs.	Dry Weig	<b>h</b> 5.34 kg.
Average Moist	ture Content: %	Wet: 16.25
Pre-test moist	20.85	Wet: 17.25
Coal Bed Range: 2.9 lbs.	to 3.5 lbs.	20% to 25% of test load
	1/4/2 03/26/12	